

AD A061400

APRPL TR-78-53

LEVEL II

Acurex-UM-78-86 (72)

20000726127

**MOMENTUM/ENERGY INTEGRAL
TECHNIQUE (MEIT) USER'S MANUAL**

10 K/Kwong, K. / Suchsland, H. / Tong
Acurex Corporation / Aerotherm Division
~~Aerospace Systems Division~~
485 Clyde Avenue
Mountain View, California 94042

9 Rept. for Aug-31 Dec 77,

11 Jul 1978

12 102 p.

Approved for public release; distribution unlimited.

DDC FILE COPY

Prepared for
Air Force Rocket Propulsion Laboratory
Director of Science and Technology
Air Force Systems Command, USAF
Edwards Air Force Base
California 93523

15 Contract F04611-76-C-0075

16 3059 17 09

Reproduced From
Best Available Copy

DDC
RECEIVED
NOV 21 1978
D

78 11 13 10

410 834

NOTICES

When Government drawings, specifications, or other data are used for any purpose other than in connection with a definitely related Government procurement operation, the United States Government thereby incurs no responsibility nor any obligation whatsoever; and the fact that the Government may have formulated, furnished, or in any way supplied the said drawings, specifications, or other data, is not to be regarded by implication or otherwise or in any manner licensing the holder or any other person or corporation, or conveying any rights or permission to manufacture, use, or sell any patented invention that may in any way be related thereto.

FOREWORD

This report was submitted by Acurex Corporation/Aerotherm Division, 485 Clyde Avenue, Mountain View California 94042, under Contract F04611-76-C-0075, Job Order No. 305909HM with the Air Force Rocket Propulsion Laboratory, Edwards AFB, California 93523.


51 2027
2027 2912
303028044
The work documented in this report was performed as a result of a recommendation made in Volume II, Applicability of Reentry Technology to Rocket Nozzle Design, AFRPL-TR-77-78, which is an interim report of work performed under the above mentioned contract. The Aerotherm work was managed by Mr. Duane L. Baker, Program Manager, Aerospace Systems, and the Air Force Project Manager was Mr. William F. Payne.

This report has been reviewed by the Information Office/XOJ and is releasable to the National Technical Information Service (NTIS). At NTIS it will be available to the general public, including foreign nations. This technical report has been reviewed and is approved for publication; it is unclassified and suitable for general public release.


WILLIAM F. PAYNE, Project Manager

FOR THE COMMANDER


CHARLES R. COOKE, Director
Solid Rocket Division


Dr. Clark Hawk
Acting Chief
Ballistic and Space Propulsion
Branch

UNCLASSIFIED

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

REPORT DOCUMENTATION PAGE		READ INSTRUCTIONS BEFORE COMPLETING FORM
1. REPORT NUMBER AFRPL-TR-78-53✓	2. GOVT ACCESSION NO.	3. RECIPIENT'S CATALOG NUMBER
4. TITLE (and Subtitle) Momentum/Energy Integral Technique (MEIT) User's Manual		5. TYPE OF REPORT & PERIOD COVERED August 1977 to 31 December 1977
7. AUTHOR(s) K. Kwong, K. Suchsland, H. Tong		6. PERFORMING ORG. REPORT NUMBER UM-78-86 (7257)✓
9. PERFORMING ORGANIZATION NAME AND ADDRESS Acurex Corporation/Aerospace Systems Division 485 Clyde Avenue Mountain View, California 94042		8. CONTRACT OR GRANT NUMBER(s) F04611-76-C-0075
11. CONTROLLING OFFICE NAME AND ADDRESS Air Force Rocket Propulsion Laboratory/AFSC Edwards Air Force Base, California 93523		10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS JON 305909HM
14. MONITORING AGENCY NAME & ADDRESS (if different from Controlling Office)		12. REPORT DATE July 1978
		13. NUMBER OF PAGES 129
		15. SECURITY CLASS. (of this report) Unclassified
		16a. DECLASSIFICATION/DOWNGRADING SCHEDULE
10. DISTRIBUTION STATEMENT (of this Report) Approved for public release; distribution unlimited		
17. DISTRIBUTION STATEMENT (of the abstract entered in Block 20, if different from Report) Approved for public release; distribution unlimited		
18. SUPPLEMENTARY NOTES		
19. KEY WORDS (Continue on reverse side if necessary and identify by block number) Rocket Nozzle Numerical Solution Boundary Layer Roughness Heating Heat Transfer Coefficient Integral Methods		
20. ABSTRACT (Continue on reverse side if necessary and identify by block number) This document presents a user's manual for the Momentum/Energy Integral Technique (MEIT) Computer Program, including a general description of the theory and solution procedure, the verification of the approach, as well as a detailed set of input instructions. MEIT is a boundary layer integral code which solves both the integral momentum and energy equations to predict the heat transfer coefficient for		

DD FORM 1 JAN 73 1473 EDITION OF 1 NOV 68 IS OBSOLETE

UNCLASSIFIED

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

UNCLASSIFIED

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

rocket nozzle environments.

A significant difference between MEIT and previous boundary layer codes is its ability to account for the effects of surface roughness.



UNCLASSIFIED

SECURITY CLASSIFICATION OF THIS PAGE (When Data Entered)

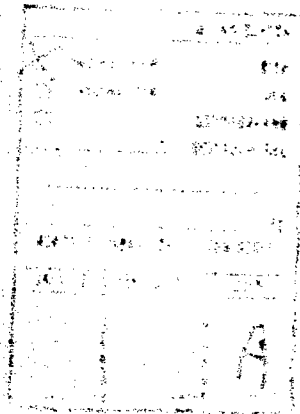
TABLE OF CONTENTS

<u>Section</u>	<u>Page</u>
1 INTRODUCTION	5
2 MEIT METHODOLOGY	7
2.1 Basic Equations	7
2.2 Shape Factor, Recovery Factor, Stanton Number and Friction Coefficient	9
2.3 Solutions of Boundary Layer Integral Equations	15
3 VERIFICATION OF MEIT	18
3.1 Aerojet MX Upper Stage Nozzle	18
3.2 C/CAN Nozzle	30
3.3 Conclusions and Recommendations	30
4 DESCRIPTION OF INPUT AND OUTPUT	38
4.1 Input Instructions	38
4.2 Output Description	41
5 SAMPLE PROBLEMS	48
6 PROGRAM LISTING	84

ADDRESSING BY	
DTIC	Whole Section <input checked="" type="checkbox"/>
DDC	Full Section <input type="checkbox"/>
UNCLASSIFIED	<input type="checkbox"/>
JUSTIFICATION	
BY	
DISTRIBUTION/AVAILABILITY CODE	
Dist.	AVAIL. and/or SPECIAL
A	

LIST OF ILLUSTRATIONS

<u>Figure</u>		<u>Page</u>
1	Geometry of the Aerojet MX upper stage nozzle	20
2	Edge conditions of the Aerojet MX upper stage nozzle	23
3	Nozzle radius vs. stream length for the Aerojet MX upper stage nozzle	24
4	Heat transfer coefficient of the Aerojet MX upper stage nozzle	25
5	Modified heat transfer coefficient for the Aerojet MX upper stage nozzle	26
6	Heat transfer coefficient for the Aerojet MX upper stage nozzle	28
7	Predicted heat transfer augmentation factor for Aerojet MX upper stage nozzle	29
8	Geometry of the C/CAN nozzle	31
9	Edge conditions of the C/CAN nozzle	34
10	Nozzle radius vs. stream length for the C/CAN nozzle	35
11	Heat transfer coefficient for the C/CAN nozzle	36



LIST OF SYMBOLS

B'	blowing parameters, $\rho_w v_x / \rho_e u_e C_M$
c_p	specific heat at constant pressure
$C_f/2$	friction coefficient, $\tau_w / \rho_e u_e^2$
C_h	Stanton number, $\dot{q}_w / \rho_e u_e (h_r - h_w)$
f	transitional intermittency factor
F	recovery factor
h	enthalpy
h_r	recovery enthalpy
h_t	total enthalpy = $h + u^2/2$
H	shape factor, δ^*/θ
$I_{x,y,z}$	influence coefficient (Equation (20))
k	roughness height
p	pressure
Pr	Prandtl number
\dot{q}_w	wall heat flux
r	radial coordinate
R	Reynolds analogy factor $\equiv C_h / C_f/2$
s	stream length
T	temperature
u	streamwise velocity component
v	body normal velocity component
y	distance in surface normal direction, radial coordinate
γ	isentropic exponent, ratio of specific heats, c_p/c_v
δ^*	boundary layer displacement thickness

LIST OF SYMBOLS (concluded)

θ	boundary layer momentum thickness
$\lambda_{x,y}$	blowing reduction parameter
μ	viscosity
ν	kinematic viscosity, μ/ρ
ρ	density
ϕ	boundary layer energy thickness
τ	skin friction

Subscripts

e	boundary layer edge
∞	freestream
l	laminar flow
t	turbulent flow
tr	transitional flow
w	wall

Superscripts

$'$	reference properties
-----	----------------------

SECTION 1

INTRODUCTION

In predicting rocket nozzle performance and analyzing Arc Plasma Generator (APG) data, the heat and mass transfer coefficient must be defined. In the past, the heat transfer coefficient has been calculated within Aerotherm by some boundary layer integral codes such as ARGEIBL (Reference 1) or BLIMP (Reference 2). Both of these computer codes assume that the boundary layer develops on a smooth wall. It has been shown (see Reference 3) that surface roughness developed in rocket nozzle and APG environments can cause substantial heat transfer augmentation. To account for this and other boundary layer effects, the Momentum/Energy Integral Technique (MEIT) computer program has been developed.

The MEIT methodology was originally developed to predict nosetip ablation on reentry vehicles. This methodology has been validated for reentry environment and is currently an important part of the ASC code (Reference 4). The methodology employed by MEIT solves both the integral momentum and energy equations. In addition, it utilizes heat transfer and skin friction laws based on the most recent roughness heating and friction data.

MEIT was developed from ASC by extracting all the subroutines that are related to the boundary layer calculation. Any nonapplicable subroutines, unnecessary variables and common block variables were deleted and a driver routine was written to read in all the required input. To tailor it for rocket nozzle applications, the input and output formats were modified so that they are compatible with the usage requirements of rocket nozzle designers.

MEIT was verified by comparing solutions to solutions generated by ARGEIBL and BLIMP. Solutions from the TBL code (Reference 5) which is developed by Pratt and Whitney Aircraft Company, were also used. Both smooth and rough wall solutions were considered in the MEIT checkout. Like ARGEIBL and other integral techniques, the heat transfer coefficient generated by MEIT must be decreased by 25 percent.

In Section 2, a brief description of the MEIT methodology is presented. This is followed by the verification of MEIT in Section 3. Section 4 provides the input and output formats and Section 5 presents two sample problems. A listing of the program is given in Section 6.

SECTION 2

MEIT METHODOLOGY

The MEIT methodology was originally developed to predict nosetip ablation in reentry vehicles. A detailed description of the methodology is given in Reference 6. Only the essential information will be presented in Section 2.

The MEIT methodology solves both the boundary layer integral momentum and energy equations. The required input are surface shape, boundary layer edge conditions, boundary layer gas properties and wall conditions (see Section 4). To solve these two equations, the local shape factor, recovery factor, Stanton number and friction coefficient must be defined. The effects of surface roughness, transpiration, acceleration, and boundary layer properties are taken into account in terms of influence coefficients. These influence coefficients are included in the formulation of both the local Stanton number and friction coefficient. The solution procedure is carried out by an implicit finite difference scheme. Although MEIT is designed primarily for rocket nozzle environment, which consists of turbulent flow; both laminar and transitional flow situations are also included.

In Section 2.1, the basic equations are presented. This is followed by the formulation of local shape factor, recovery factor, Stanton number, and friction coefficient in Section 2.2. The solution procedure is described in Section 2.3.

2.1 BASIC EQUATIONS

The two boundary layer integral equations solved by MEIT are:

Integral momentum equation

$$\frac{1}{r\rho_e u_e^2} \frac{d}{ds} (r\rho_e u_e \theta) = \frac{C_f}{2} + \frac{(\rho v)_w u_e}{\rho_e u_e^2} + \frac{H\theta}{\rho_e u_e^2} \frac{dp}{ds} \quad (1)$$

Integral energy equation

$$\frac{1}{r\rho_e u_e (h_{t,e} - h_w)} \frac{d}{ds} (r\rho_e u_e (h_{t,e} - h_w) \phi) = C_h \left(\frac{h_r - h_w}{h_{t,e} - h_w} \right) + \frac{(\rho v)_w (h_{t,e} - h_w)}{\rho_e u_e (h_{t,e} - h_w)} \quad (2)$$

where the momentum and energy thicknesses are respectively:

$$\theta \equiv \int_0^\infty \frac{\rho u}{\rho_e u_e} \left(\frac{u_e - u}{u_e} \right) dy \quad (3)$$

$$\phi \equiv \int_0^\infty \frac{\rho u}{\rho_e u_e} \left(\frac{h_{t,e} - h_t}{h_{t,e} - h_w} \right) dy \quad (4)$$

The boundary layer shape factor, H , is defined as:

$$H = \frac{\delta^*}{\theta} \quad (5)$$

where δ^* , the displacement thickness is given by:

$$\delta^* = \int_0^\infty \left(1 - \frac{\rho u}{\rho_e u_e} \right) dy \quad (6)$$

The total enthalpy at the boundary layer edge is defined by

$$h_{t,e} = h_e + \frac{u_e^2}{2} \quad (7)$$

while the recovery enthalpy is given by

$$h_r = h_e + F \frac{u_e^2}{2} \quad (8)$$

where F is the recovery factor.

The heat transfer rate and skin friction are related to the Stanton number and friction coefficient respectively by:

$$\tau_w = \rho_e u_e^2 \frac{C_f}{2} \quad (9)$$

$$\dot{q}_w = \rho_e u_e C_H (h_r - h_w) \quad (10)$$

In order to facilitate the solutions of equations (1) and (2), besides the required input of surface shape, boundary layer edge conditions, boundary layer gas properties, and wall conditions, the local shape factor, recovery factor, Stanton number and friction coefficient have to be formulated.

2.2 SHAPE FACTOR, RECOVERY FACTOR, STANTON NUMBER AND FRICTION COEFFICIENT

The shape and recovery factors are evaluated in MEIT by the following relations.

For laminar flow:

$$H_\ell = 3.029 \frac{T_w}{T_e} - 0.614 \quad (11)$$

$$F_\ell = Pr^{1/2} \quad (12)$$

For turbulent flow:

$$H_t = 2.285 (1 + 3.2e^{-n}) \frac{T_w}{T_e} - 0.96 \quad (13)$$

$$F_t = Pr^{1/3} \quad (14)$$

where n, the turbulent velocity profile exponent, is given by:

$$n = \frac{0.37 + \ln Re_0}{2.79 - 0.14 \ln Re_0} \quad (15)$$

The friction coefficient and the Stanton number are evaluated by the basic wall shear and heat flux laws respectively. Both of these laws are based on incompressible flow along a smooth, isothermal, impervious, flat plate. The friction coefficient and Stanton number are:

for laminar flow

$$\frac{C_{f,l,o}}{2} = \frac{0.245}{Re_\theta} \quad (16)$$

$$C_{h,l,o} = \frac{0.22}{Pr^{1/3} Re_\phi} \quad (17)$$

And for turbulent flow

$$\frac{C_{f,t,o}}{2} = \frac{0.245}{Re_\theta} + \frac{0.0123 Re_\theta}{100 + Re_\theta} (\log_{10} Re_\theta)^{-1.6} \quad (18)$$

$$C_{h,t,o} = \frac{0.22}{Pr^{1/3} Re_\phi} + \frac{0.0123 Re_\phi}{Pr^{1/3} (100 + Re_\phi)} (\log_{10} Re_\phi)^{-1.6} \quad (19)$$

In order to account for the various boundary layer effects, the Stanton number and friction coefficient given above are modified by the corresponding influence coefficients:

$$C_{x,y} = C_{x,y,o} \prod_z I_{x,y,z} \quad \begin{matrix} \text{for } x = h, f \\ y = l, t \end{matrix} \quad (20)$$

The influence coefficients are shown by $I_{x,y,z}$ where the subscripts x and y indicate whether the influence coefficient pertains to heat or momentum transfer ($x = h$ or f) and laminar or turbulent flow ($y = l$ or t), respectively. The subscript z indicates the type of phenomenon for which the basic laws are being modified.

Four phenomena are considered by MEIT. These phenomena and their corresponding z -subscripts are given in Table 1. The influence coefficients corresponding to each of these effects are formulated below.

TABLE 1

Phenomena	z-subscript of influence coefficient
acceleration	β
transpiration	B'
boundary layer properties	p
roughness	r

Acceleration

In laminar flow,

$$I_{f,l,\beta} = (1 + 3\beta)^{1/3}, \quad \beta > 0$$

$$I_{f,l,\beta} = 1.0, \quad \beta < 0$$

$$I_{h,l,\beta} = (1 + 4\beta)^{1/6}, \quad \beta > 0$$

$$I_{h,l,\beta} = 1.0, \quad \beta < 0$$

$$\text{where: } \beta \equiv \frac{2\xi}{u_e} \frac{du_e}{d\xi}$$

$$\xi \equiv \int_0^s \rho_e \nu_e u_e r^2 ds$$

In turbulent flow, only the first terms of the appropriate basic turbulent laws are modified by the above influence coefficients.

Transpiration

Blowing effects are modeled with adaptations to film theory (Reference 7).

$$I_{h,y,B'} = \frac{\ln(1 + 2\lambda_{h,y} R' B')}{2\lambda_{h,y} R' B'}, \quad y = l, t$$

$$I_{f,y,B'} = \frac{\ln(1 + 2\lambda_{f,y} R' B')}{2\lambda_{f,y} R' B'}, \quad y = l, t$$

where: $R \equiv C_h/C_{f/2}$ = Reynolds Analogy Factor

R' = Mass to heat transfer coefficient ratio

$\lambda_{x,y}$ = Blowing reduction parameter.

R is a dependent variable which is evaluated during the solution process. Both R' and $\lambda_{x,y}$ are input (see Section 4). MEIT, however, does provide build-in default values for $\lambda_{x,y}$. These default values are:

$$\lambda_{h,l} = \lambda_{f,l} = 0.5$$

$$\lambda_{h,t} = \lambda_{f,t} = 0.35$$

Boundary Layer Properties

Boundary layer properties of density, viscosity, and Prandtl number are evaluated at the reference enthalpy h'

$$h' = ah_e + bh_r + ch_w$$

The property influence coefficients are:

$$I_{x,y,p} = \left(\frac{\rho'}{\rho_e}\right)^d \left(\frac{\mu'}{\mu_e}\right)^e, \quad x = f, h; \quad y = l, t$$

where the constants a , b , c , d , and e for all combinations of x and y are given in Table 2.

TABLE 2

Constants Used to Evaluate Property Influence Coefficients

Property influence coefficients	Constant				
	a	b	c	d	e
$I_{f,l,p}$	0.23	0.19	0.58	0	0
$I_{h,l,p}$	0.23	0.19	0.58	1	1
$I_{f,t,p}$	0.36	0.19	0.45	1	0.25
$I_{h,t,p}$	0.36	0.19	0.45	1	0.25

Surface Roughness

In laminal flow,

$$I_{h,l,r} = I_{f,l,r} = 1$$

In turbulent flow, the influence coefficient due to surface roughness is based on correlations from PANT and Stanford heat transfer data (Reference 8 and 9), as well as Stanford and NSWC friction data (Reference 9 and 10). The turbulent influence coefficients due to roughness are:

$$I_{f,t,r} = 1 + 0.5 f(k/\theta) g(X)$$

$$I_{h,t,r} = 1 + 0.3 f(k/\theta) g(X)$$

where: $f(k/\theta) = 1 + 0.09 (k/\theta) + 0.53 (1 - e^{-k/\theta})$

$$g(X) = X + 1.5 (1 - e^{-X}) \quad \text{for } X > 0$$

$$= 0 \quad \text{for } X \leq 0$$

$$X = \log \frac{k^+}{15.5}$$

$$K^+ = \frac{\rho_e u_e k}{\mu_e} \frac{\mu_e}{\mu_w} \left(\frac{\rho_w}{\rho_e} \right)^{1/2} \sqrt{\frac{C_{f,t,s}}{2}}$$

$C_{f,t,s}$ = smooth wall friction coefficient given by equation (19)

k = surface roughness

k is input either as function of material or location (see Section 4).

The above formulations for H , F , C_h , $C_{f/2}$ are only for laminar and turbulent flows. To evaluate these four parameters for transitional flow the following relation is used:

$$P = (1 - f) P_l + f P_t \quad (21)$$

where P is one of the four parameters above and f is the transitional intermittency factor.

The transitional intermittency employed in MEIT is based on the work of Persh (Reference 11), and according to the interpretation of Dahm (Reference 12).

$$f = 1 - \frac{\alpha}{Re_\theta^2 (C_{f,t} - C_{f,l})}$$

where

$$\alpha = Re_{\theta,tr}^2 (C_{f,t} - C_{f,l})_{tr}$$

and the subscript tr refers to conditions at the transition point.

f is set to zero in laminar flow, unity in turbulent flow, and varies between 0 and 1 in transitional flow.

—This completes the formulation of the four required parameters used in the solutions of equations (1) and (2).

2.3 SOLUTIONS OF BOUNDARY LAYER INTEGRAL EQUATIONS

As mentioned above, the required input to MEIT are surface shape, boundary layer edge conditions, boundary layer gas properties, and wall conditions. These quantities are input in terms of body points. A finer grid in terms of integration points, which include all the body points, is generated by the program to ensure adequate solution accuracy of the integral equations. The boundary layer edge conditions, gas properties and wall conditions at each integration point are obtained by linear interpolation from the input. The solution procedures of the boundary layer integral equations (1) and (2) consist of:

- start-up series solutions at the first three integration points
- finite difference numerical solutions for the rest of the integration points

The solutions at the first integration point are given by:

$$\theta_1 = \sqrt{\frac{0.245 \nu_1 (1 + R_1 B_1')}{(3 + H) \left. \frac{du_e}{ds} \right|_1}} \frac{z}{\pi C_{f,l,z}}$$

$$\phi_1 = \sqrt{\frac{0.22 \nu_1 (1 + B_1')}{2 Pr \left. \frac{du_e}{ds} \right|_1}} \frac{z}{\pi C_{h,l,z}}$$

The solutions at the second and third integration point are related to the first integration point by:

$$\theta = \theta_1 (1 + a\psi^2)$$

$$\phi = \phi_1 (1 + b\psi^2)$$

$$\text{where: } a = \frac{\frac{13 + H_1}{4} \frac{\alpha}{\gamma} + \frac{1}{3} - \frac{0.659 (3 + H_1) \alpha (\gamma-1)}{\gamma} - \frac{(H_1 - 0.614) \alpha (\gamma-1)}{\gamma}}{8 + 2H_1}$$

$$b = \frac{1}{6} \left[\frac{3\alpha}{\gamma} + \frac{1}{3} - \frac{2 \times 0.659 \alpha (\gamma-1)}{\gamma} - \frac{2(1-F_2)(1+B') \alpha (\gamma-1)}{(1 - T_w/T_1)\gamma} \right]$$

$$\psi = s/R_{\text{ref}}$$

$$\text{and } \alpha = \frac{1 - (p_3/p_1)}{\psi_3^2}$$

In the above formulation, R_{ref} is an arbitrary constant radius and γ is the isentropic exponent. The subscripts 1 and 3 denote the first and third integration point condition respectively.

The solutions of the first three integration points were originally derived for reentry nosetip ablation prediction, and consider the first integration point to be a stagnation point. In MEIT, these solutions serve only as the start up procedure and should be ignored in the output.

For the rest of the integration points, the following implicit finite difference scheme is used:

$$F_{x,I} = F_{x,I-1} + 0.5(F'_{x,I-1} + F'_{x,I})(s_I - s_{I-1}) \quad x = f, h$$

$$\text{where: } F_f = r \rho_e u_e^2 \theta \quad (\text{see Equation (1)})$$

$$F_h = r \rho_e u_e (h_{t,e} - h_w) \phi \quad (\text{see Equation (2)})$$

$$F'_f = \frac{dF_f}{ds}$$

$$F'_h = \frac{dF_h}{ds}$$

I is the integration point index and F'_f and F'_h are both evaluated from equation (1) and (2) respectively.

Since the values of $F_{x,I}$ depend on $F'_{x,I}$, the solution is obtained by iteration. This iteration is local because closure is obtained at each integration point before proceeding down the body to the next integration point. Convergence is based on changes of less than 0.1 percent in both the heat and momentum transfer coefficients between successive iterations. If the iteration fails to converge in 30 tries, a local explicit solution is obtained by setting $F'_{x,I} = F'_{x,I-1}$, and subsequently reevaluating $F'_{x,I}$ based on the resulting value of $F_{x,I}$, before proceeding to the next integration point.

SECTION 3

VERIFICATION OF MEIT

Three computer programs were used in the check out of MEIT. These three codes are:

- ARGEIBL
- BLIMP
- TBL

Both ARGEIBL and BLIMP have no provisions to account for surface roughness. ARGEIBL solves only the energy integral equation and the heat transfer coefficients it calculates are routinely multiplied by 0.75 to improve their accuracy. BLIMP uses an exact implicit technique to solve the boundary layer differential conservation equations. The solution from BLIMP is believed to be the most accurate of these codes and was used as the primary criterion to determine the validity of MEIT in the check out. TBL is developed by Pratt and Whitney Aircraft Company and, like MEIT, it uses both the momentum and energy integral equations to calculate the Stanton number. It also has build-in routines to account for surface roughness.

The check out is performed by generating and comparing heat transfer coefficients for two typical rocket nozzle environments using these four computer codes. The selected rocket nozzle environments are the Aerojet MX upper stage and the C/CAN nozzle. The results of the check out and the conclusions and recommendations are summarized below.

3.1 AEROJET MX UPPER STAGE NOZZLE

An analysis of the Aerojet MX upper stage nozzle by BLIMP, ARGEIBL, and MEIT as used to validate MEIT. The geometry of the nozzle is shown

in Figure 1. A listing of the nozzle wall coordinates is given in Table 3. The nozzle has a 3.146-inch radius throat and it uses a PEG/FEFO propellant. The elemental composition of the propellant and the associated chamber conditions are given in Table 4. All this information was obtained from Reference 13. The edge conditions were calculated by the ACE code (Reference 14), and the results in terms of edge pressure, temperature, enthalpy, and velocity are presented in Figure 2. The nozzle radius is plotted as a function of stream length in Figure 3. A wall temperature of 5500°R was used in all the following calculations.

Smooth wall solutions were obtained using MEIT, ARGEIBL, and BLIMP, and the heat transfer coefficients from these solutions are compared in Figure 4. The MEIT and ARGEIBL solutions are very close to each other for regions downstream of the throat. Both of these solutions are high compared to BLIMP results. As mentioned above, the ARGEIBL solution must be reduced by a 0.75 factor to accurately predict the heat transfer coefficient. Using 0.75 as the modifier, the modified MEIT and ARGEIBL solutions are again compared to the BLIMP solution in Figure 5. From this figure, it can be seen that both the reduced MEIT and ARGEIBL solutions compare much better with the BLIMP solution. This shows that MEIT, like ARGEIBL, requires a modifier of 0.75.

For the unblown, smooth wall and turbulent flow calculations (as in the above case) it can be shown from Section 1 and Reference 1 that MEIT is solving the same Energy Integral Equation as in ARGEIBL (i.e., for this case the Momentum Integral Equation does not enter into the solution process). It is therefore of interest to find out the reasons for the difference in the MEIT and ARGEIBL heat transfer coefficient solutions. The chief reason is the different formulation for the local Stanton number in the two codes. In MEIT, the local Stanton number is given by equation (19)

$$C_{h,t,o} = \left[\frac{0.22}{Pr^{1/3} Re_\phi} + \frac{0.0123 Re_\phi}{Pr^{1/2} (100 + Re_\phi)} (\log Re_\phi)^{-1.6} \right]$$

and modified by the influence coefficients due to acceleration and boundary layer properties. In ARGEIBL, the Stanton number is defined by:

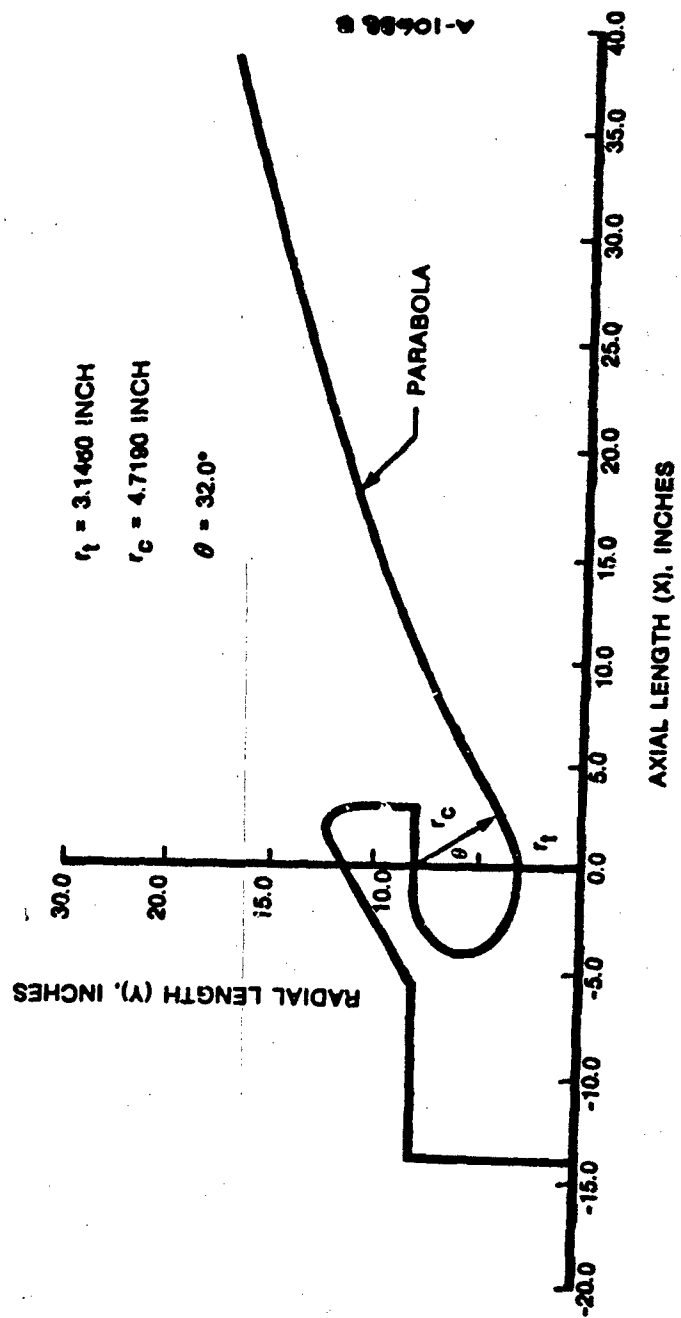


Figure 1. Geometry of the Aerojet MX upper stage nozzle.

TABLE 3. WALL COORDINATES OF THE AEROJET MX UPPER STAGE NOZZLE

X, IN.	Y, IN.	
-4.00	5.40	NOSE CAP
-3.89	4.96	
-3.72	4.67	
-3.54	4.44	
-3.30	4.25	
-3.04	4.02	
-2.76	3.83	
02.38	3.65	
02.08	3.52	
-1.70	3.39	
-1.32	3.30	
-0.94	3.22	
-0.58	3.19	
-0.20	3.147	
0	3.146	THROAT
0.165	3.149	
0.411	3.164	
0.657	3.19	
1.06	3.27	
1.45	3.38	
1.99	3.588	
2.36	3.78	
3.62	4.54	
7.53	6.64	
10.32	7.95	
14.89	9.87	
20.43	11.93	
25.20	13.5	
30.60	15.2	
38.60	17.5	EXIT

TABLE 4. PEG/FEFO PROPELLANT DATA

$P_{\text{CHAMBER}} = 102. \text{ ATM}$

$T_{\text{CHAMBER}} = 6912. \text{ }^{\circ}\text{R}$

ELEMENTAL COMPOSITION

ELEMENT	GM ATOMS 100 GRAMS
H	2.39527
C	1.13509
N	1.79248
O	2.27887
F	0.07275
Al	0.68563
Cl	0.07071

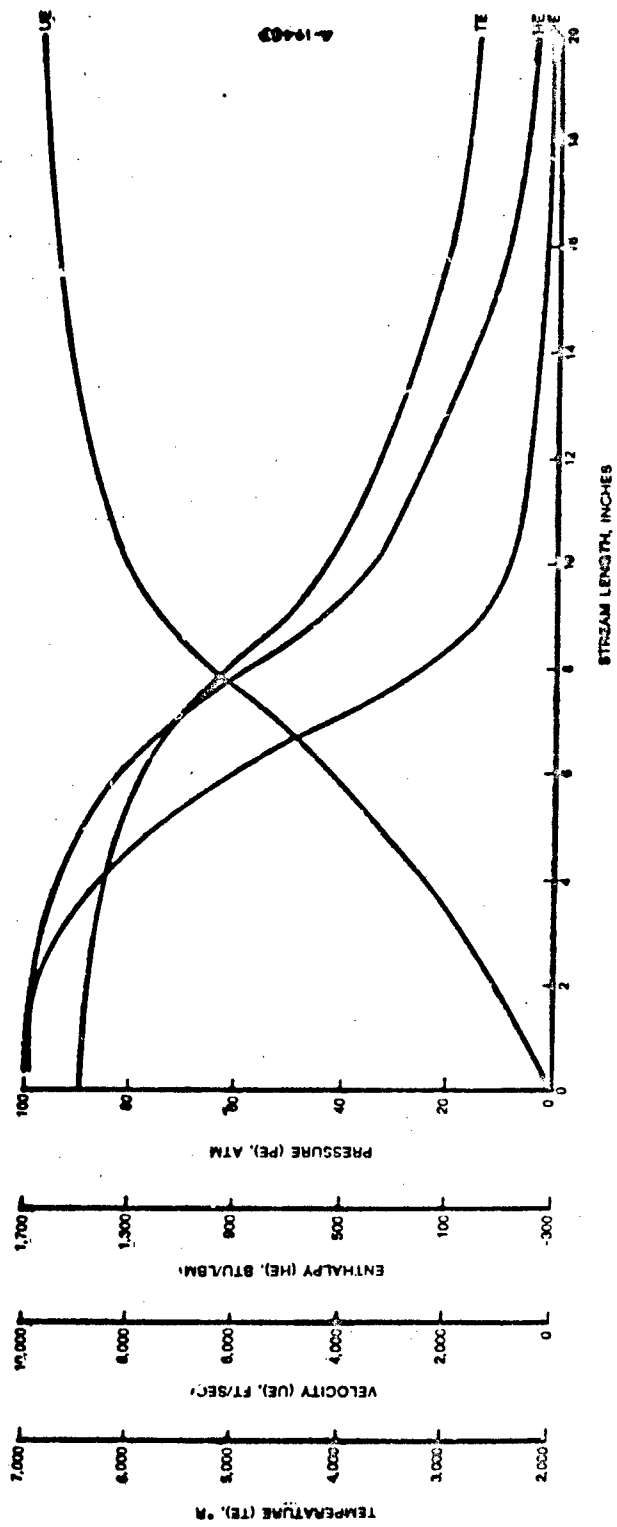


Figure 2. Edge conditions of the Aerojet MX upper stage nozzle.

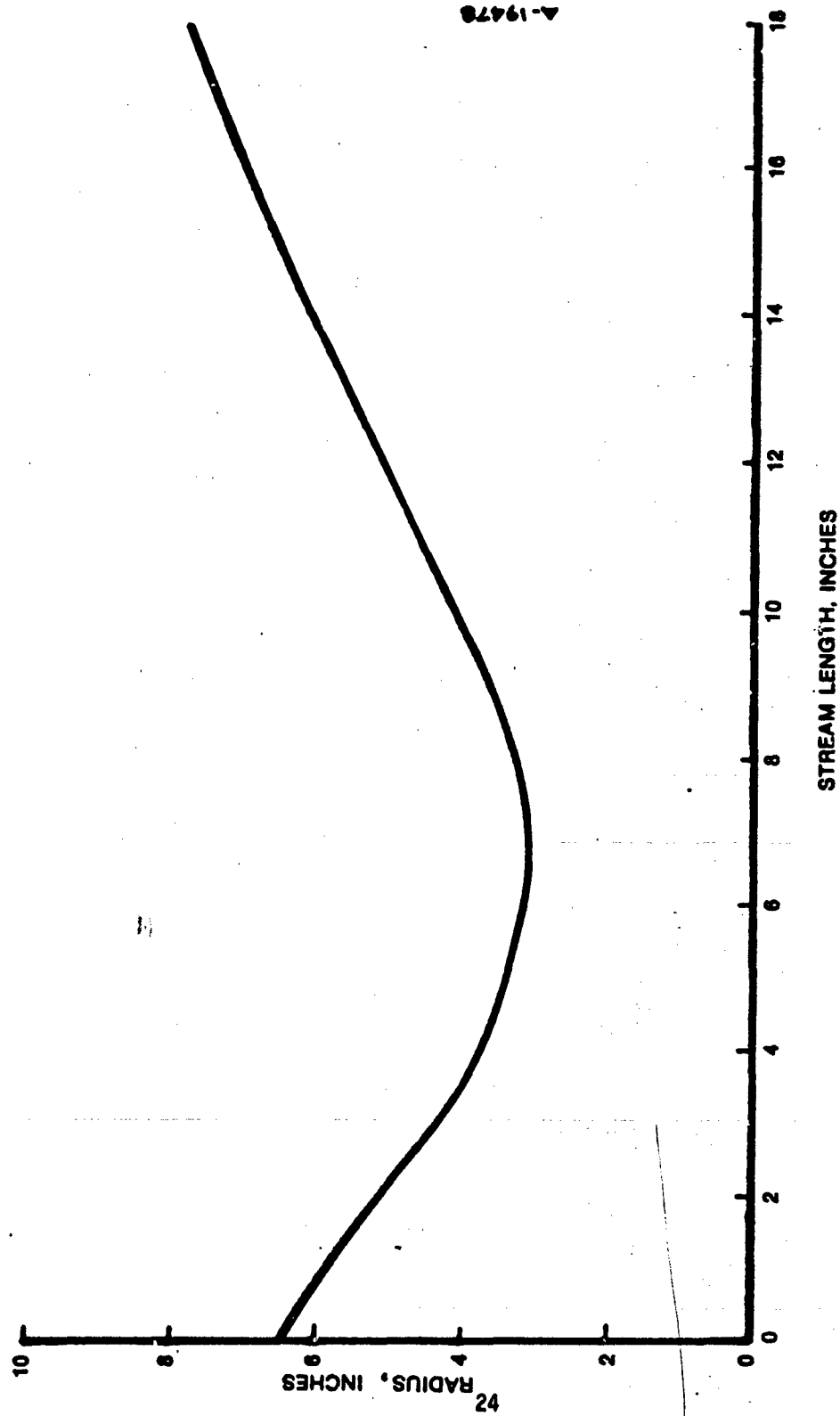


Figure 3. Nozzle radius vs. stream length for the Aerojet MX upper stage nozzle.

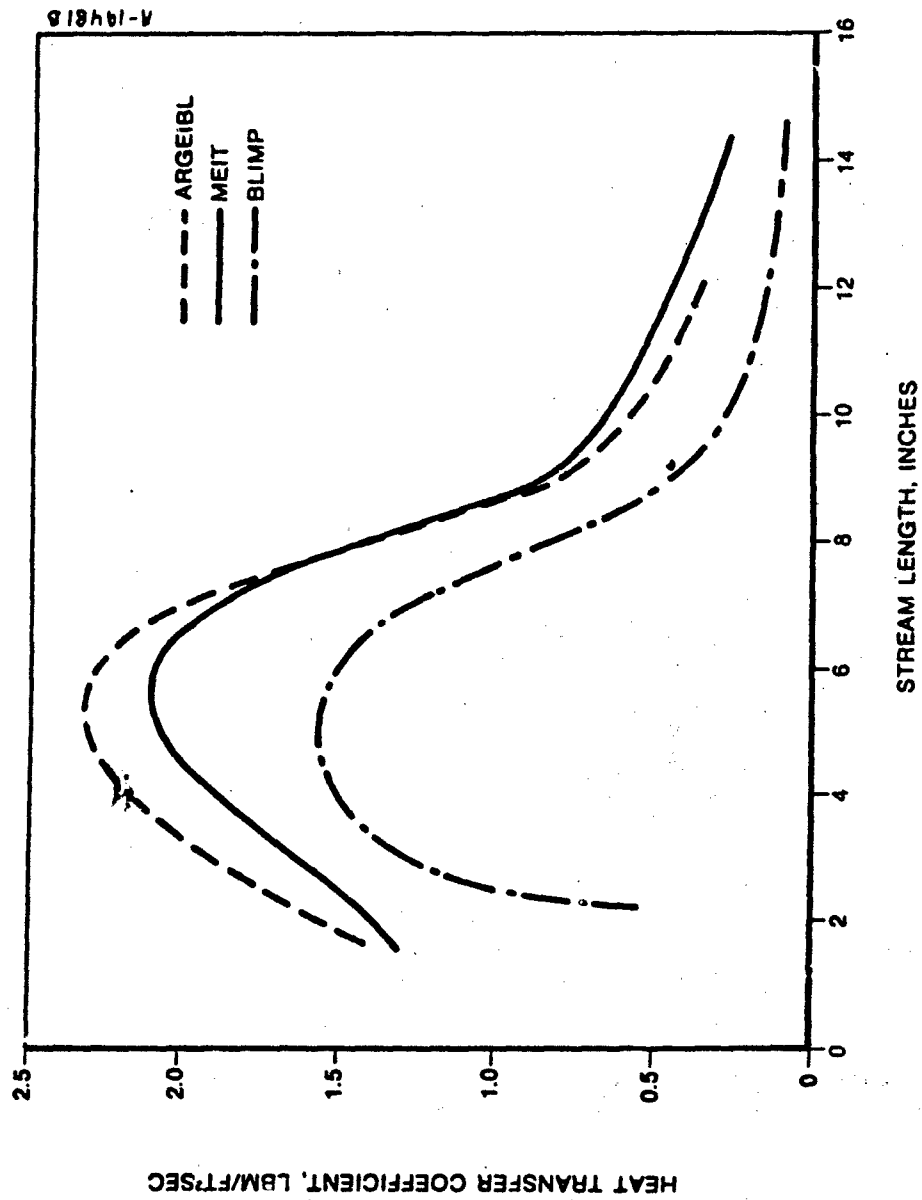


Figure 4. Heat transfer coefficient for the Aerojet MX upper stage nozzle.

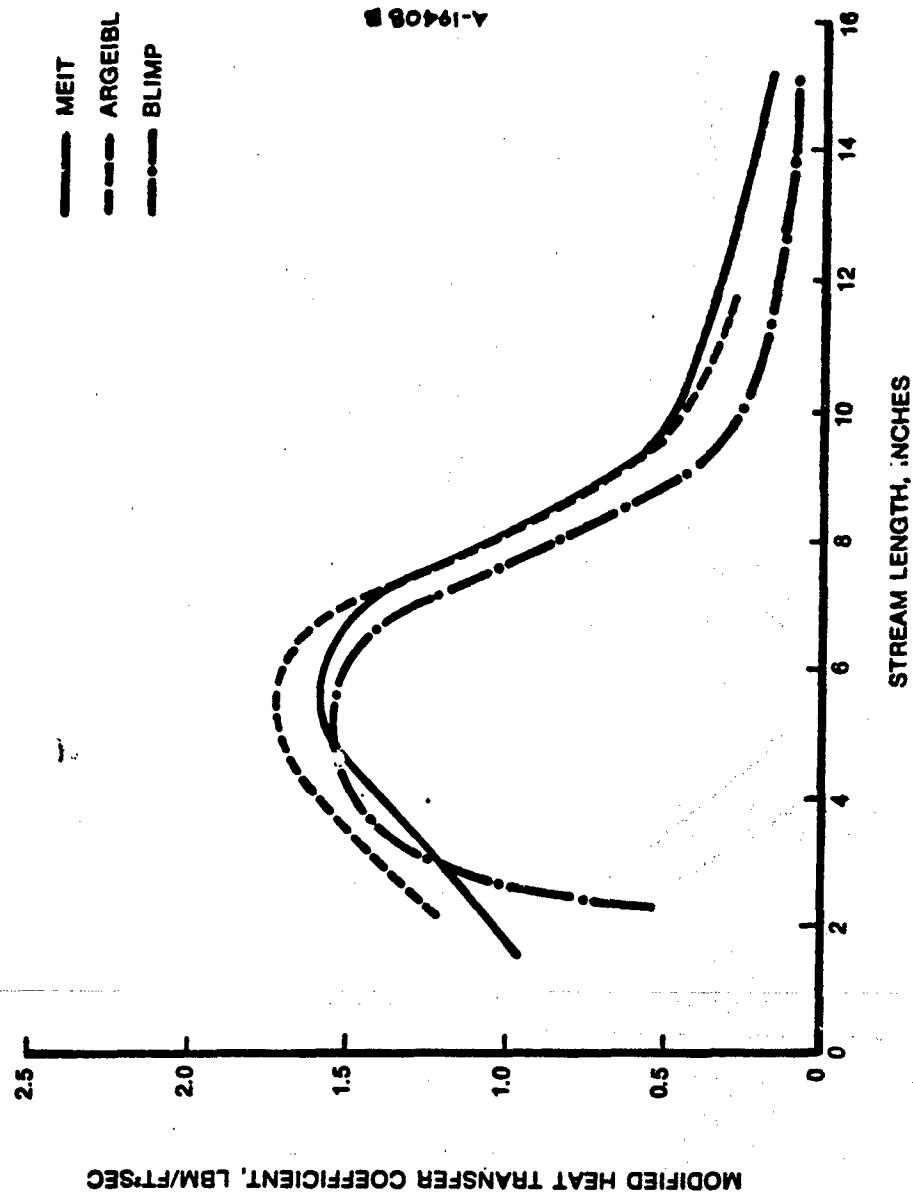


Figure 5. Modified heat transfer coefficient for the Aerojet MX upper stage nozzle.

$$C_h = \frac{0.0130 \left(\frac{\rho'}{\rho}\right)^{1/4}}{(Pr')^{1/6} Re^{1/4}}$$

where the subscript ' denotes properties evaluated at the reference enthalpy.

Other reasons are differences in the subroutines built in each code. These are the following:

- ARGEIBL uses the trapezoidal rule to calculate the numerical integration whereas MEIT uses an averaging technique.
- ARGEIBL uses a cubic curve fit to interpolate the required properties whereas MEIT uses a linear interpolation.

To check if MEIT is indeed solving the same energy integral equation as in ARGEIBL for the unblown, smooth wall and turbulent flow calculation, the Stanton number formulation in MEIT was replaced by the ARGEIBL formulation, and a solution was obtained using this new 'ARGEIBL-MEIT' code. The heat transfer coefficients from this calculation are again compared to those given by ARGEIBL in Figure 6. The two solutions compare very well in the nose cap region and the differences in other locations are basically due to the different inherent routines mentioned above.

In order to check the surface roughness formulation, a rough wall solution was generated by MEIT. A roughness height of 2 mil was used throughout the nozzle. The roughness augmentation from this calculation is compared to those given in Reference 15 in Figure 7. The results from Reference 15 are based on local energy thickness and conditions given by the smooth wall BLIMP solution and were hand-calculated using the MEIT surface roughness formulation. Figure 7 shows that these two solutions compare very well with each other. The higher values given by Reference 15 are mainly due to the use of smooth wall momentum thicknesses in the hand calculation.

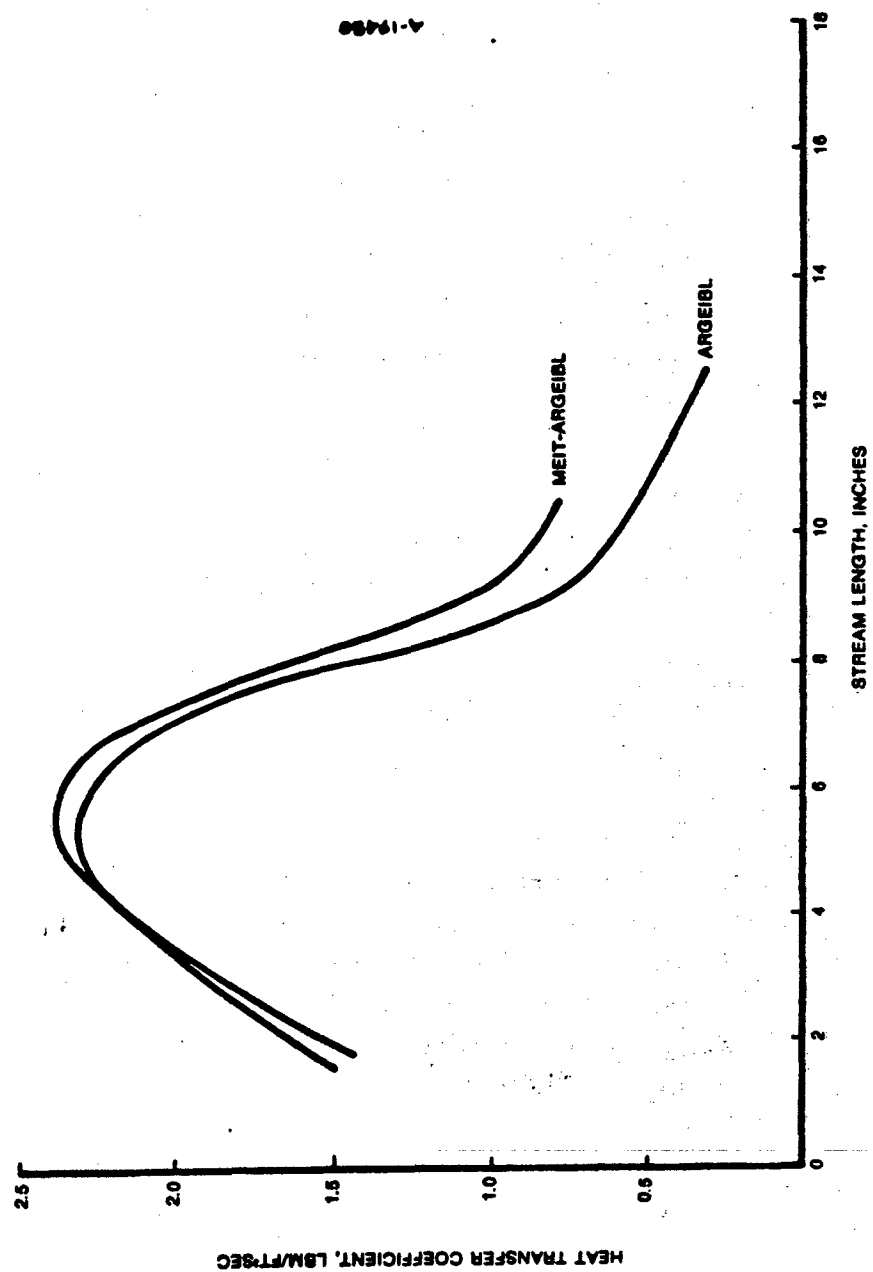


Figure 6. Heat transfer coefficient for the Aerojet MX upper stage nozzle.

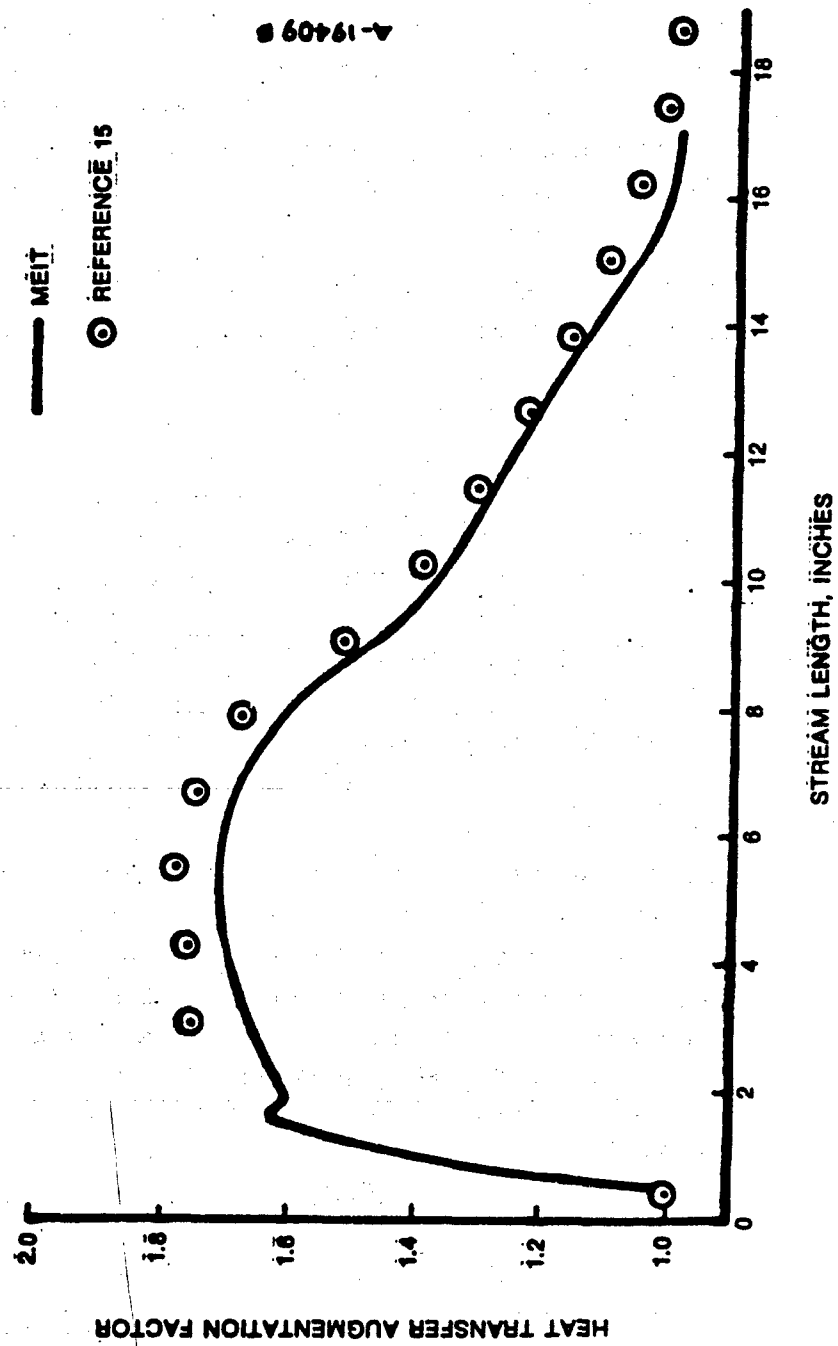


Figure 7. Predicted heat transfer augmentation factor for the Aerojet MX upper stage nozzle.

3.2 C/CAN NOZZLE

The C/CAN nozzle is used primarily to compare the rough wall solutions generated by MEIT and TBL. The geometry of the nozzle is shown in Figure 8. A listing of the wall coordinates of the nozzle is given in Table 5. The nozzle has a throat radius of 0.960 inch and uses a HT 90/18 propellant. The elemental composition of the propellant and the chamber conditions are given in Table 6. The above information was obtained from Reference 16. The edge conditions were again calculated by ACE and are presented in Figure 9. The nozzle radius vs. stream length plot is given in Figure 10 and the wall temperature is assumed to be 4939°R.

Both smooth and rough wall calculations were performed by MEIT. Smooth and rough wall solutions generated by TBL were furnished to Aero-therm by Atlantic Research Corporation (Reference 16). The rough wall calculations were based on a roughness height of 2 mil. The solutions are compared in Figure 11. For the smooth wall case, the MEIT and TBL solutions are almost identical. For the rough wall case, MEIT predicts lower heat transfer coefficients than TBL except for locations just downstream of the combustion chamber. According to Reference 16, the TBL solutions, like those generated by ARGEIBL, are normally modified by modifying factors to make them compatible with measured values. These modifying factors are developed from actual motor firing data. However, since there were no firing data available at the time of the check out, the question of whether MEIT or TBL is more accurate in rough wall prediction cannot be answered at this time.

Reference 16 also indicates that the roughness modelling in TBL would not approach the smooth wall modelling when the surface roughness is reduced. To make sure that this is not the case for MEIT, an additional MEIT calculation was performed using a roughness height of 0.01 mil. The results are exactly the same as the smooth wall solutions shown in Figure 11. This indicates that MEIT is self-consistent.

3.3 CONCLUSIONS AND RECOMMENDATIONS

The findings and conclusions based on the above discussion are summarized below:

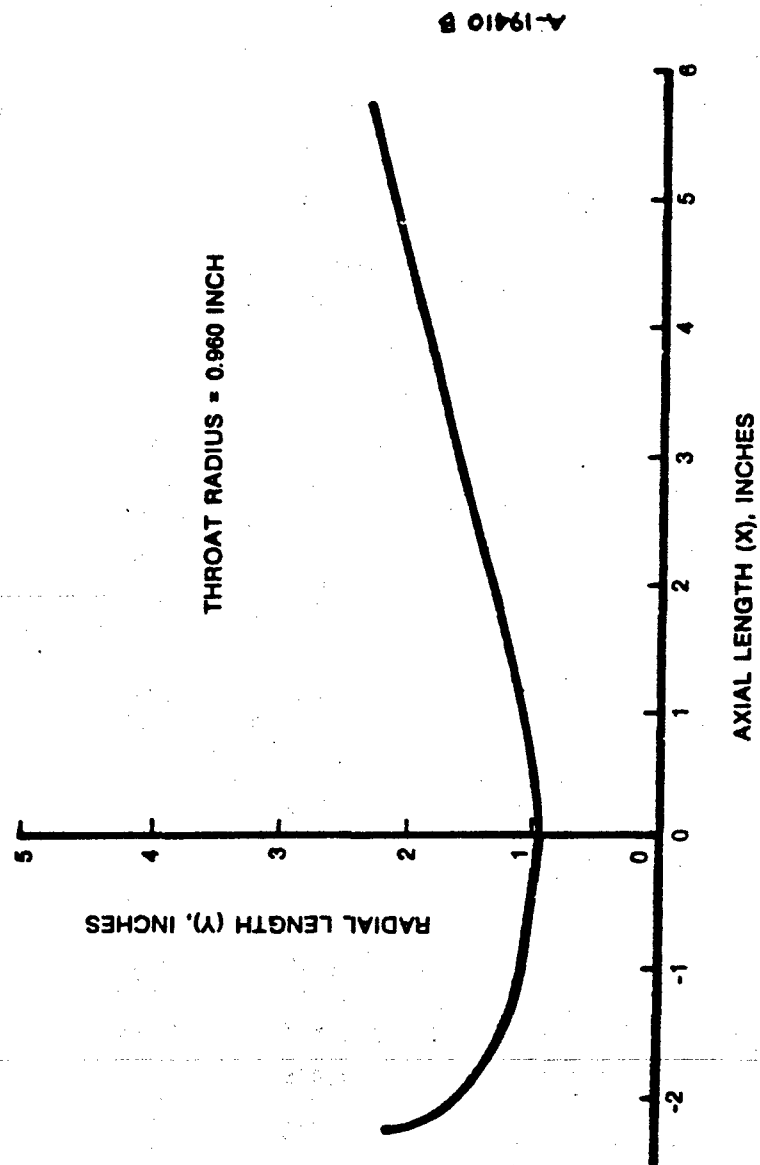


Figure 8. Geometry of the C/CAN nozzle.

TABLE 5. WALL COORDINATES OF THE C/CAN NOZZLE


X, IN.	Y, IN.	
-2.25	2.12	
-2.20	1.836	
-2.0	1.526	
-1.85	1.410	
-1.50	1.252	
-1.10	1.114	
-0.80	1.041	
-0.54	0.991	
-0.30	0.971	
-0.10	0.961	
0.0	0.960	
0.10	0.961	
0.20	0.965	
0.40	0.980	
0.60	1.005	
0.80	1.041	
1.20	1.141	
1.70	1.275	
2.45	1.475	
3.45	1.743	
4.45	2.011	
5.70	2.346	

TABLE 6. HT 90/18 PROPELLANT DATA

$P_{\text{Chamber}} = 68.027 \text{ atm}$

$T_{\text{Chamber}} = 6627.6 \text{ }^{\circ}\text{R}$

$H_{\text{Chamber}} = - 812.70 \text{ Btu/lbm}$

ELEMENTAL COMPOSITION:

Element	<u>Gm Atoms</u> <u>100 gram</u>
H	3.4976
C	.6936
N	.6177
O	2.4857
Al	.6671
Cl	.6128

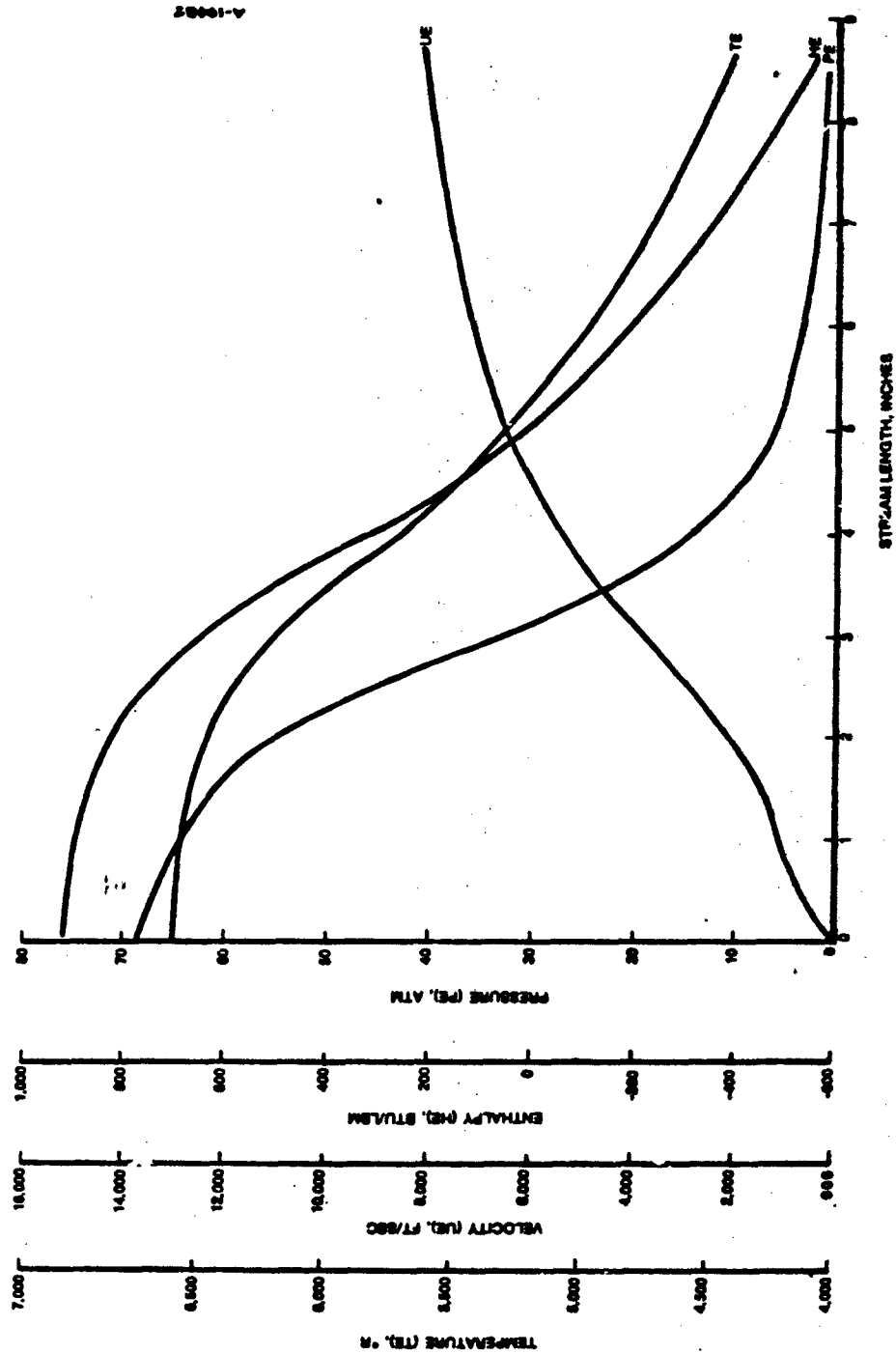


Figure 9. Edge conditions of the C/CAN nozzle.

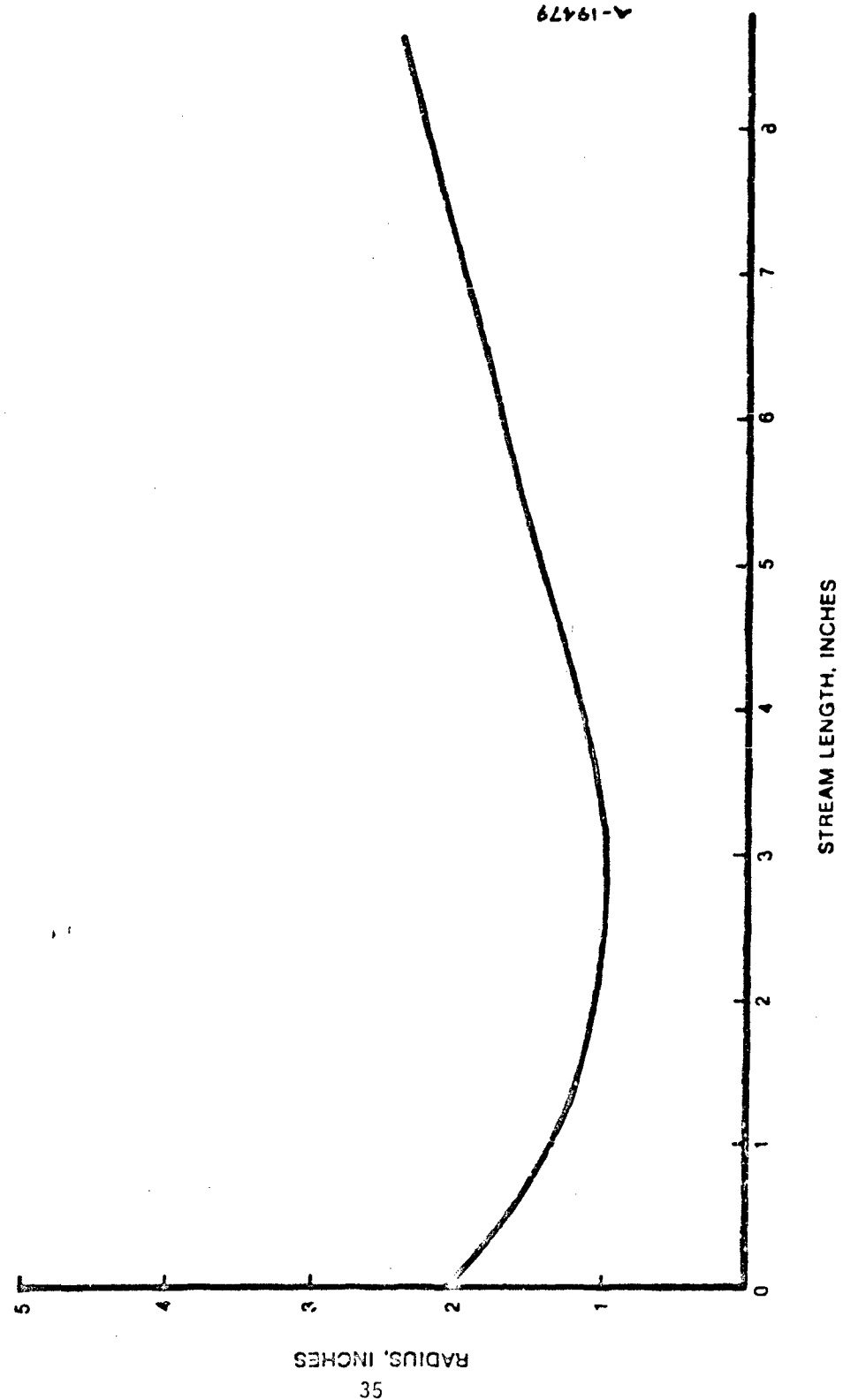


Figure 10. Nozzle radius vs. stream length for the C/CAN nozzle.

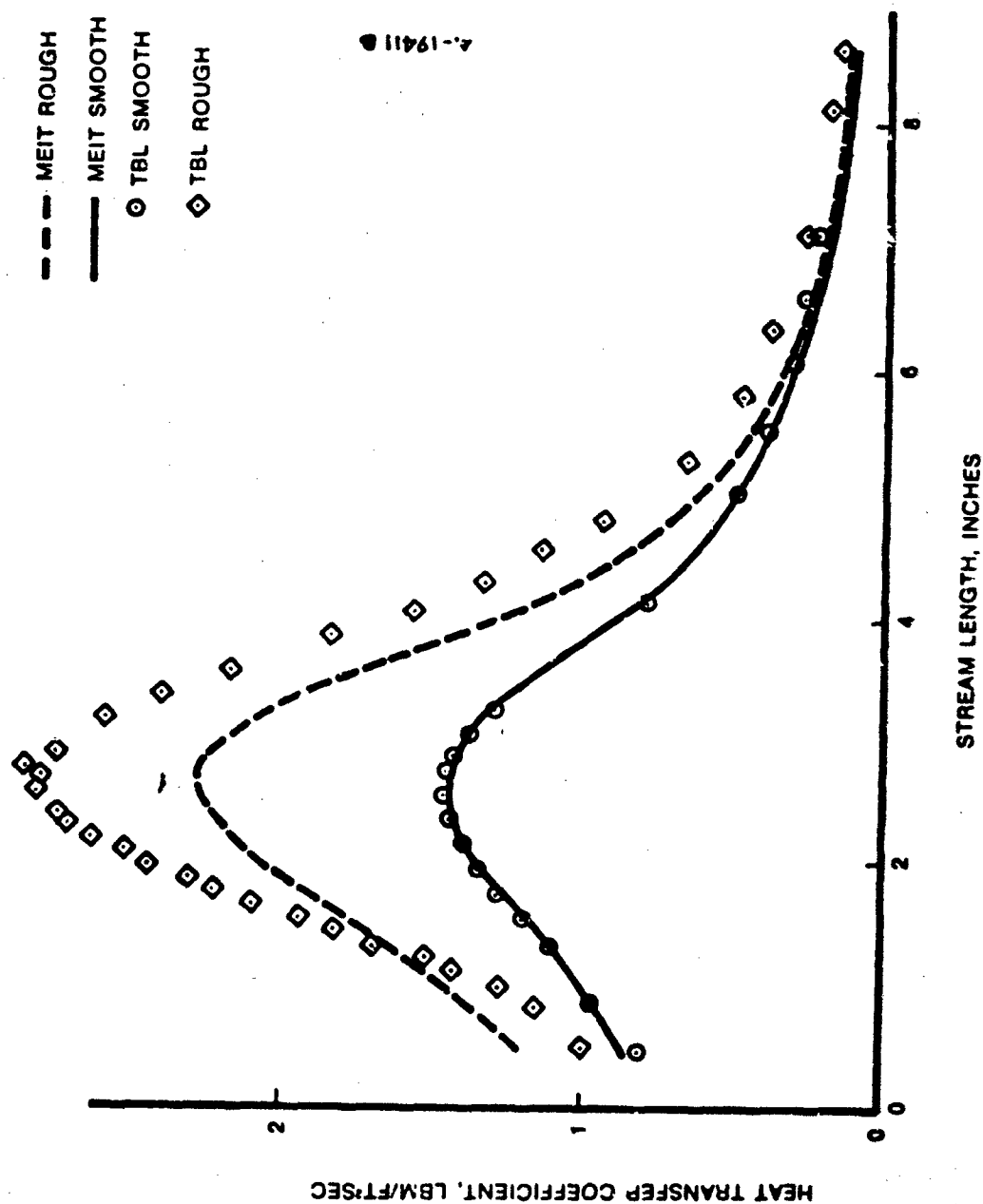


Figure 11. Heat transfer coefficients for the C/CAN nozzle.

- For nonblown, smooth wall and turbulent flow, both MEIT and ARGEIBL solve the same energy integral equation.
- Using the BLIMP solution as the criterion and a modifying factor of 0.75, the modified MEIT solution is better than the modified ARGEIBL solution.
- MEIT and TBL predict essentially the same heat transfer coefficient for smooth wall calculation.
- For rough wall calculation, MEIT predicts a lower heat transfer coefficient than TBL except in regions immediately downstream of the combustion chamber.
- MEIT is self-consistent in its roughness modelling.

The recommendations are:

- For both smooth and rough wall calculations, a factor of 0.75 should be used to modify the heat transfer coefficient generated by MEIT.
- Experiments or analyses should be conducted to deduce the heat transfer coefficient from actual motor firing data to check the validity of the surface roughness modelling in MEIT.
- A technique needs to be devised to evaluate nozzle material roughnesses for input into MEIT.
- When there is no firing data to modify the TBL heat transfer coefficient, the MEIT solution modified by a 0.75 factor should be used for rough wall predictions.

SECTION 4

DESCRIPTIONS OF INPUT AND OUTPUT

This section provides detailed user oriented input instructions and a description of the output. The input instructions are presented in Section 4.1 and the output features are covered in Section 4.2.

4.1 INPUT INSTRUCTIONS

The program input consists of three card sets:

1. General program constants and transition information
2. Surface shape, boundary layer edge and wall conditions
3. Boundary layer gas properties

The description of these three card sets is given below.

Card Set 1 - Control Cards

This card set is made up of three cards which provide general program constants and transition information. The four blowing reduction parameters, $\lambda_{x,y}$, which are used to calculate the blowing influence coefficients (see Section 2.2), are also included in this card set

Card No.	Column	Format	Data	Unit
1	1	I1	NSM - No. of material, up to 3 allowed	-
	2	I1	IROUGH - Roughness height input flag 0 - Input as function of material (see below) 1 - Input as function of location (see Card Set 2)	-

Card No.	Column	Format	Data	Unit
2	3-10	F8.5	CMH - Mass to heat transfer coefficient ratio, default value = 1.0	-
	11-20	F10.5	GAM2 - Isentropic exponent, default value = 1.2	-
	1-10	F10.5	BTS - $\lambda_{f,t}$, default value = 0.5	-
	11-20	F10.5	BTH - $\lambda_{h,t}$, default value = 0.5	-
	21-30	F10.5	BLS - $\lambda_{f,1}$, default value = 0.35	-
	31-40	F10.5	BLH - $\lambda_{h,1}$, default value = 0.35	-
	41-50	F10.5	RUFL - Surface roughness height as function of material, input only if IROUGH = 0	mil

Repeat card 2 for each material (number of cards equals NSM).

2 + NSM	1-2	I2	NS - No. of body points (maximum 60)	-
	2-4	I2	IBRUPT - Abrupt transition flag 0 - laminar and transitional flow 1 - fully turbulent flow.	-
	8-6	I2	NREYCR - Transition flag 0,7 - all turbulent 1 - all laminar 4 - transitional	-
	7-8	I2	IPRNT - Output print flag 1 - Detailed output at body point 2 - Detailed output at integration point	-
	9-12		Blank	
	13-22		DLTRAN - Axial location at which transition takes place, input only if NREYCR = 4	in

Card Set 2 - Body Point Data

This card set is made up of nine subsets and they provide the surface sharp, edge and wall condition information to the program. The nine subsets are:

- IMAT - Material index, default value = 1
- ZSP - Axial wall coordinates (in.)

- RSP - radial wall coordinates (in)
- PE - Edge pressure (atm)
- HE - Edge enthalpy (Btu/lbm)
- UE - Edge velocity (ft/sec)
- TSP - Wall temperature (°R)
- BPSP - Blowing parameter $\equiv (\rho v)_w / \rho_e u_e C_M$
- RUF2 - Surface roughness height (mil)
RUF2 is input only if IROUGH = 1 (see Card Set 2).

The nine subsets are input in the above order. Each of these subsets has NS entries and each entry corresponds to a point on the heated surface of the body. The input format of all the subsets are F10.3 except IMAT which uses an input format of I10. The values of each subset are entered eight to a card. Since the solution for the first body point is based on stagnation conditions (see Section 2), it is recommended that the first entry in the velocity subset (UE) be zero.

Card Set 3 - Gas Property Tables

The gas property table provides the thermodynamic and transport properties of the boundary layer gas. This table is divided into subtables based on pressure. Within each pressure subtable, they are ordered either on temperature or enthalpy. If they are ordered on temperature, the same temperature array must be used for all other pressure subtables. The same is true for the enthalpy entries if the properties are input as functions of enthalpy and pressure.

Card No.	Column	Format	Data	Unit
1	1-3	I3	IPMAX - No. of pressure entries (maximum 21)	
	4-6	I3	IHMAX - No. of temperature or enthalpy entries (maximum 35)	
	7-12	I3	LTB - Temperature enthalpy flag 0- Properties input as functions of pressure and enthalpy 1- Properties input as functions of pressure and temperature	

Card No.	Column	Format	Data		Unit
2	1-10	F10.3	PT	- Pressure	atm
3 to IPMAX + 2					
	1-12	E12.4	HT	- Enthalpy	Btu/lbm
	13-24	E12.4	TEMP	- Temperature	°R
	25-36	E12.4	EMT	- Molecular weight	
	37-60		Blank		
	61-72	E12.4	ET	- Viscosity	lbm/ft-sec
	73-80	F8.4	GT	- Prandtl No.	

Cards 3 to IPMAX + 2 are repeated until the total number of pressures is equal to IPMAX. Note the pressure, enthalpy, and temperature entries must be input in ascending order.

4.2 OUTPUT DESCRIPTION

MEIT output can be divided into three categories. These are:

- Output of Input
- Output of Calculation Results
- Debug Output

The descriptions of each of these output are given below.

Output of Input

The program output begins with the output of the input. This output is made up of three parts:

- General program information
- Thermodynamic table
- General input information table

The general program information prints out the program constants contained in the first three input cards. These include mass to heat transfer coefficient ratio, isentropic exponent, the four blowing reduction parameters, and transition information. The FORTRAN names corresponding to

these variables are given in Section 4.1. The thermodynamic table tabulates the thermodynamic and transient properties of the boundary layer gas as functions of pressure. This table is self-explanatory. The general input information table gives the surface shape, boundary layer edge conditions and wall conditions. The variables printed in this table, their FORTRAN names and definitions are listed below:

- BODY PT NO (J)
Index of the body points
- INTEG PT NO (I)
Index of the integration point for which the computed parameters are printed
- MATL NO (MATL)
Material index.
- STREAM LENGTH, inch (S)
Stream length along the heated surface from the initial point to the integration points
- AXIAL LENGTH, inch (Z)
Axial coordinate of the integration points with respect to the initial point
- RADIAL LENGTH, inch (R)
Radial coordinate of the integration points with respect to the centerline
- BODY ANGLE, degrees (THETB)
Angle which the tangent to the surface makes with respect to the centerline
- NORMALIZED ABLATION RATE (BPSP)
Normalized ablation rate B' at the wall

$$B' \equiv \frac{(\rho v)_w}{\rho_e u_e C_M}$$
- WALL TEMP, °R (TW)
Temperature of the wall

- SURFACE ROUGHNESS, mil (RUFMIL)
Surface roughness height of the wall material
- PRESSURE, atm (PE)
Edge pressure of the boundary layer
- ENTHALPY, Stu/lbm (HE)
Edge enthalpy of the boundary layer
- VELOCITY, ft/sec (UE)
Edge velocity of the boundary layer

Output of Calculation Results

The results of the code calculations are printed out in three tables.
These three tables are:

1. Viscous Flow - Edge Properties
2. Viscous Flow - Wall and B. L. Recovery Properties
3. Viscous Flow - Boundary Layer Solution

The variables printed in each table, their FORTRAN names and definitions are listed below.

1. Viscous Flow - Edge Properties Table

- BODY PT NO (J)
Index of the body points
- INTEG PT NO (I)
Index of the integration point for which the computed parameters are printed
- STREAM LENGTH, inch (S)
Stream length along the heated surface from the initial point to the integration points
- VELOCITY, ft/sec (UE)
Velocity at the edge of the boundary layer
- MACH NO (HCAM)
Mach number at the edge of the boundary layer

- ENTHALPY, Btu/lbm (HE)
Enthalpy at the edge of the boundary layer
- TEMPERATURE, °R (TE)
Temperature at the edge of the boundary layer
- DENSITY, lbm/ft³ (ROE)
Density at the edge of the boundary layer
- VISCOSITY, lbm/ft-sec (VISE)
Viscosity at the edge of the boundary layer
- UNIT RE NO, 1/ft (URE)
Unit Reynolds number at the edge of the boundary layer

Note that the Mach number given in this table is valid only if there are no condensed species in the freestream.

2. Viscous Flow - Wall and B.L. Recovery Properties Table

- BODY PT NO (J)
Index of the body points
- INTEG PT NO (L)
Index of the integration point for which the computer parameters are printed
- STREAM LENGTH, inch (S)
Stream length along the heated surface from the initial point to the integration points
- WALL TEMPERATURE, °R (TW)
Temperature at the wall
- WALL ENTHALPY, Btu/lbm (HW)
Enthalpy of gas at wall temperature and pressure
- WALL DENSITY, lbm/ft³ (ROW)
Density of gas at wall temperature and pressure
- WALL VISCOSITY, lbm/ft-sec (VISW)
Viscosity of gas at wall temperature and pressure

- RECOVERY ENTHALPY, Btu/lbm (HR)
Recovery enthalpy defined by $h_r \equiv h_e + F (h_t - h_e)$
- RECOVERY FACTOR (RECOV)
Recovery Factor defined by $F = Pr^n$, $n = \begin{cases} 1/2 & \text{for laminar flow} \\ 1/3 & \text{for turbulent flow} \end{cases}$
- SENSBLE CONV HEAT FLUX, Btu/ft² sec
Sensible convective heat flux defined by $\dot{q}_w = \rho_e u_e C_H (h_r - h_w)$
- CF/2
Function coefficient $C_f/2 \equiv \tau_w / (\rho_e u_e^2)$

3. Viscous Flow - Boundary Layer Solution Table

- BODY PT NO (J)
Index of the body points
- INTEG PT NO (I)
Index of the integration point for which the computed parameters are printed
- STREAM LENGTH, inch (S)
Stream length along the heated surface from the stagnation point to the integration points
- MOMENTUM THICKNESS, mil (THE)
Momentum thickness θ of the boundary layer
- ENERGY THICKNESS, mil (PHI)
Energy thickness ϕ of the boundary layer
- SHAPE FACTOR (HSF)
Boundary layer shape factor, $H \equiv \delta^*/\theta$

where $\delta^* \equiv \int_0^\delta \left(1 - \frac{\rho u}{\rho_e u_e}\right) dy$ is the boundary layer displacement thickness.

- MOM THICK RE NO (RETH)
Reynolds number based on the momentum thickness, $Re_\theta = \frac{\rho_e u_e \theta}{\mu_e}$

- ENERGY THICK RE NO (REPH)
Reynolds number based on the energy thickness, $Re_\phi = \frac{\rho_e u_e \phi}{\mu_e}$
- HEAT TRANS COEFFICIENT, lbm/ft²sec (RUCH)
Heat transfer coefficient, $\rho_e u_e C_h \equiv \dot{q}_w / (h_r - h_w)$
where C_h is the Stanton number and \dot{q}_w is the wall heat flux
- REYNOLDS ANAL FAC (RAF)
Reynolds analogy factor $C_h / (C_f/2)$
- INTERMITTENCY (ADML)
Boundary layer intermittency factor f , where $0 \leq f \leq 1$ for flow ranging from fully laminar to fully turbulent regime
- HEAT TRANS AUGMENT (RUFST)
Heat transfer augmentation due to surface roughness, this quantity is equivalent to the roughness influence coefficient

As mentioned in Section 2, the solutions for the first three integration points are only for start up purpose. These solutions should be ignored in the output.

Debug Output

There are four error messages output by MEIT. The error messages and their meanings are given below.

- ***** Wrong Pressure Input Ordering
The pressure entries in the boundary layer gas properties table are not in ascending order.
- ***** Wrong Temperature/Enthalpy Input Ordering
The temperature or enthalpy entries in the boundary layer gas properties table are not in ascending order.
- ***** Input Temperature/Enthalpy Error
The corresponding temperature or enthalpy entries in the boundary layer gas properties table are not the same for different pressure entries.

- Computation of MEIT equations did not converge at Point I. The MEIT calculations at Integration Point I did not converge after 30 tries.

There are also other debug output built in MEIT. However, since these output are only useful to the very sophisticated users who are intimately familiar with the program logic, they are not described here.

SECTION 5

SAMPLE PROBLEMS

Presented in this section are two sample problems which were run on a Univac 1108 Digital Computer. For each sample problem, the following is presented:

- A brief description of the nature of the problem and solution.
- A listing of the input data deck.
- A listing of the output.

Sample Problem 1

This is a smooth wall calculation for the Aerojet MX upper stage nozzle with a PEG/FEFO propellant. The details of this system were described in Section 3. A total of 21 body points were input. The wall temperature was assumed to be 5500°R. A IPRNT = 1 option was used which printed out only the body point solutions.

INPUT LISTING OF SAMPLE PROBLEM NO. 1

1 .7089 1.2704

21 1 7 1

0. 1.65361 2.01637 2.81659 3.17910 3.85984 4.23981 4.61979
 9.97964 5.36262 5.96134 5.72631 5.97230 6.21041 6.62102 7.00631
 7.91796 13.08933 20.08066 30.76366 44.16533 58.20000 3.20000 3.20000
 0.00000 4.93904 6.44088 4.02000 3.63004 3.39000 3.27000 3.30000
 3.18996 3.17004 3.16804 3.16904 3.16404 3.18996 3.27000 3.30000
 3.780006.63996 9.87 13.5 17.4996
 180.00000 97.23560 94.37290 90.00630 83.27080 74.44780 69.87120 63.15230
 59.24808 54.85899 47.74930 44.58640 40.00090 35.78010 29.09960 22.65110
 11.333322.6765 1.2638 .6355 .3356
 1692.200001650.700001637.690001605.200001522.100011477.100011431.660001370.14999
 1331.200001304.300001197.360001156.240011094.199991028.10001 915.30000 763.88000
 456.29003-31.62 -296.84 -443.52 -594.98
 .000001295.1000111648.000002056.000002648.299993261.500003611.399994015.20001
 9281.099984465.599984977.099985179.799995371.599985765.799996286.299996743.20001
 7845.700019423.2 9976.5 10388. 10700.
 5500. 5500. 5500. 5500. 5500. 5500. 5500. 5500.
 5500. 5500. 5500. 5500. 5500. 5500. 5500. 5500.

6 16

1. 1.65361 2.01637 2.81659 3.17910 3.85984 4.23981 4.61979
 9.97964 5.36262 5.96134 5.72631 5.97230 6.21041 6.62102 7.00631
 7.91796 13.08933 20.08066 30.76366 44.16533 58.20000 3.20000 3.20000
 0.00000 4.93904 6.44088 4.02000 3.63004 3.39000 3.27000 3.30000
 3.18996 3.17004 3.16804 3.16904 3.16404 3.18996 3.27000 3.30000
 3.780006.63996 9.87 13.5 17.4996
 180.00000 97.23560 94.37290 90.00630 83.27080 74.44780 69.87120 63.15230
 59.24808 54.85899 47.74930 44.58640 40.00090 35.78010 29.09960 22.65110
 11.333322.6765 1.2638 .6355 .3356
 1692.200001650.700001637.690001605.200001522.100011477.100011431.660001370.14999
 1331.200001304.300001197.360001156.240011094.199991028.10001 915.30000 763.88000
 456.29003-31.62 -296.84 -443.52 -594.98
 .000001295.1000111648.000002056.000002648.299993261.500003611.399994015.20001
 9281.099984465.599984977.099985179.799995371.599985765.799996286.299996743.20001
 7845.700019423.2 9976.5 10388. 10700.
 5500. 5500. 5500. 5500. 5500. 5500. 5500. 5500.
 5500. 5500. 5500. 5500. 5500. 5500. 5500. 5500.

54000000	19236+02	58760+00	-53917-01	39785-00	9378
72000000	19140+02	65175+00	-10135+00	4157-00	9555
90000000	19010+02	81595+00	-16219+00	28338-00	9827
108000000	18667+02	95318+00	-23180+00	43977-00	9996
126000000	18625+02	10625+01	-38625+00	49327-00	9963
144000000	18505+02	12809+01	-58233+00	45757-00	9929
162000000	18315+02	15833+01	-93818+00	46471-00	9393
171000000	18216+02	19839+01	-99534+00	46795-00	9376
28.					
63000000	20655+02	12487+01	-70183+00	25462-00	9953
81000000	20203+02	18486+01	-54271+00	26022-00	9841
99000000	19551+02	64332+00	-18723+00	27561-00	9672
118000000	19351+02	49922+00	-19093+01	30888-00	9621
136000000	19356+02	49883+00	-58833+02	31480-00	9616
154000000	19329+02	49545+00	-16095+02	39281-00	9611
180000000	19327+02	49884+00	-19408+02	35503-00	9608
198000000	19321+02	46657+00	-51994+02	37982-00	9600
216000000	19386+02	49156+00	-13233+01	48278-00	9589
234000000	19276+02	52575+00	-28214+01	42376-00	9575
252000000	19274+02	52268+00	-51711+01	48267-00	9558
270000000	19183+02	63227+00	-83863+01	45997-00	9538
288000000	19855+02	78170+00	-12357+00	47284-00	9516
306000000	18941+02	77845+00	-21891+00	48731-00	9492
324000000	18808+02	85909+00	-21845+00	49883-00	9466
342000000	18734+02	90018+00	-24035+00	50410-00	9452
360000000	20957+02	12480+01	-73885+00	26150-00	8899
378000000	20951+02	10662+01	-68399+00	26473-00	8929
396000000	19755+02	73388+00	-89757+00	28046-00	8733
414000000	19403+02	49758+00	-59957+01	30198-00	8636
432000000	19336+02	3337+00	-8628+01	31522-00	8623
450000000	19335+02	4642+00	-85728+02	34218-00	8613
468000000	19331+02	45031+00	-25150+02	35512-00	8609
486000000	19325+02	46313+00	-8655+02	38000-00	8601
504000000	19315+02	48316+00	-96855+02	48278-00	8591
522000000	19292+02	50933+00	-20713+01	48473-00	8577
540000000	19253+02	54561+00	-38624+01	48442-00	8562
558000000	19195+02	59281+00	-64883+01	46220-00	8544
576000000	19111+02	64936+00	-96885+01	47818-00	8525
594000000	19017+02	71295+00	-13487+00	49227-00	8508
612000000	18921+02	78182+00	-17748+00	50491-00	8479
630000000	18837+02	81644+00	-28029+00	51873-00	8467
78.					
68000000	21181+02	12249+01	-73888+00	26372-00	8189
86000000	20670+02	10947+01	-63889+00	27090-00	8066
104000000	19908+02	73710+00	-35735+00	28397-00	7778
122000000	19446+02	82672+00	-18822+00	30339-00	7655
140000000	19341+02	49863+00	-6379+02	31882-00	7631
158000000	19335+02	48882+00	-36518+02	38222-00	7615
176000000	19328+02	48177+00	-38598+02	35319-00	7610
194000000	19319+02	47942+00	-81884+02	38809-00	7602
212000000	19308+02	50178+00	-17285+01	42168-00	7579
230000000	19267+02	53285+00	-34221+01	44325-00	7564
248000000	19217+02	57373+00	-54313+01	46355-00	7548
266000000	19187+02	62386+00	-82828+01	48805-00	7529
284000000	19058+02	67990+00	-11712+00	49687-00	7509

.14200+04	.68943+04	.18932+02	.74131+00	-.15596+00	.50017-04	.4407
.17100+04	.64102+04	.18093+02	.77323+00	-.17671+00	.51030-04	.4475
100.						
-.63000+03	.23513+04	.21295+02	.12100+01	-.74121+00	.26079-04	.5154
-.50000+03	.24720+04	.20018+02	.10954+01	-.64426+00	.27397-04	.5030
-.34000+03	.26100+04	.20023+02	.08075+00	-.59572+00	.28664-04	.4314
-.18000+03	.26033+04	.19527+02	.56084+00	-.14160+00	.30401-04	.4674
-.90000+02	.30503+04	.19418+02	.48972+00	-.63285+01	.31654-04	.4641
.90000+02	.34468+04	.19349+02	.45175+00	-.11190+01	.34237-04	.4617
.18000+03	.36462+04	.19340+02	.45190+00	-.57561+02	.35527-04	.4612
.34000+03	.40410+04	.19331+02	.46114+00	-.40264+02	.38016-04	.4603
.54000+03	.44252+04	.19322+02	.47722+00	-.73947+02	.40359-04	.4593
.72000+03	.47949+04	.19305+02	.49721+00	-.15242+01	.42547-04	.4580
.90000+03	.51477+04	.19276+02	.52499+00	-.28595+01	.44378-04	.4565
.10000+04	.54798+04	.19231+02	.56100+00	-.08193+01	.46440-04	.4550
.12600+04	.57801+04	.19167+02	.60608+00	-.70058+01	.48131-04	.4532
.14400+04	.60729+04	.19086+02	.65871+00	-.10555+00	.49637-04	.4513
.16200+04	.63352+04	.18987+02	.71543+00	-.14164+00	.51033-04	.4492
.17100+04	.64588+04	.18932+02	.74509+00	-.16103+00	.51609-04	.4481

SAMPLE PROBLEM 1 OUTPUT

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

NUMBER OF MATERIALS = 1
 CR/CH = .78398
 ISENTROPIC EXPONENT = 1.27000

MATL	STS	BYM	BLS	BLM
1	.35000	.35000	.35000	.35000

NS = 21
 ISRUPT = 1
 METER = 7
 IPANT = 1
 OLTRAN = .00000 INCHES

ABRUPT TRANSITION

FLOW IS TURBULENT

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

THERMODYNAMIC TABLE *****

PRESSURE = .300ATM				PRANDTL NUMBER
ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	
-530.0000	1801.7000	19.4270	.000022	.4589
-348.0000	1984.2000	19.3350	.000024	.4584
-360.0000	2405.5000	19.3270	.000027	.4606
-180.0000	2824.8000	19.3270	.000030	.4613
-90.0000	3031.2000	19.3260	.000031	.4613
90.0000	3432.6000	19.3190	.000034	.4609
180.0000	3628.5000	19.3090	.000035	.4604
360.0000	3975.5000	19.2670	.000038	.4591
548.0000	4274.5000	19.1850	.000039	.4570
720.0000	4520.8000	19.0650	.000041	.4543
900.0000	4724.7000	18.9080	.000042	.4511
1080.0000	4896.5000	18.7500	.000043	.4476
1260.0000	5043.7000	18.5370	.000044	.4440
1440.0000	5172.5000	18.3300	.000044	.4402
1620.0000	5286.2000	18.1270	.000045	.4364
1710.0000	5341.6000	18.0210	.000045	.4345

PRESSURE = 1.000ATM				PRANDTL NUMBER
ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	
-530.0000	1869.0000	19.6330	.000023	.4648
-348.0000	2002.0000	19.5890	.000024	.4600
-360.0000	2406.2000	19.5260	.000027	.4606
-180.0000	2825.1000	19.5270	.000030	.4613
-90.0000	3031.5000	19.5260	.000031	.4613
90.0000	3437.0000	19.5220	.000034	.4610
180.0000	3635.0000	19.5170	.000035	.4606
360.0000	4003.5000	19.2910	.000038	.4593
540.0000	4332.5000	19.2360	.000040	.4578
720.0000	4615.6000	19.1440	.000041	.4555
900.0000	4855.5000	19.0190	.000043	.4527
1080.0000	5059.6000	18.6670	.000044	.4496
1260.0000	5235.6000	18.6950	.000045	.4463
1440.0000	5389.8000	18.5090	.000046	.4429
1620.0000	5527.1000	18.3150	.000046	.4393
1710.0000	5555.5000	18.2160	.000047	.4376

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

PRESSURE = 25.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-630.0000	2176.0000	20.6530	.000025	.4955
-540.0000	2254.7000	20.2030	.000026	.4841
-360.0000	2475.9000	19.5510	.000028	.4672
-180.0000	2832.0000	19.3510	.000030	.4621
-90.0000	3034.8000	19.3360	.000031	.4616
90.0000	3441.9000	19.3290	.000034	.4611
180.0000	3482.8000	19.3270	.000036	.4603
360.0000	4035.8000	19.3210	.000038	.4600
540.0000	4412.3000	19.3060	.000040	.4589
720.0000	4766.0000	19.2760	.000042	.4575
900.0000	5095.4000	19.2260	.000044	.4558
1080.0000	5394.9000	19.1530	.000046	.4538
1260.0000	5645.3000	19.0580	.000047	.4516
1440.0000	5908.9000	18.9410	.000049	.4492
1620.0000	6128.9000	18.8080	.000050	.4466
1710.0000	6231.3000	18.7360	.000050	.4452

PRESSURE = 50.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-630.0000	2260.9000	20.9570	.000026	.5049
-540.0000	2442.3000	20.4910	.000027	.4929
-360.0000	2838.3000	19.7540	.000028	.4733
-180.0000	3047.7000	19.4030	.000030	.4636
-90.0000	3048.5000	19.3560	.000032	.4623
90.0000	3443.2000	19.3340	.000034	.4613
180.0000	3644.0000	19.3310	.000036	.4609
360.0000	4038.6000	19.3250	.000038	.4601
540.0000	4412.6000	19.3140	.000040	.4591
720.0000	4782.6000	19.2920	.000042	.4577
900.0000	5124.6000	19.2530	.000044	.4562
1080.0000	5441.7000	19.1950	.000046	.4544
1260.0000	5732.0000	19.1160	.000048	.4528
1440.0000	5996.7000	19.0170	.000049	.4503
1620.0000	6237.9000	18.9010	.000050	.4479
1710.0000	6350.6000	18.8370	.000051	.4467

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

PRESSURE = 75.000ATM				
ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-630.0000	2313.1000	21.1510	.000027	.5109
-350.0000	2390.6000	20.6780	.000027	.4986
-360.0000	2583.1000	19.9040	.000028	.4778
-180.0000	2866.5000	19.4660	.000030	.4655
-90.0000	3048.6000	19.3650	.000032	.4631
90.0000	3444.8000	19.3410	.000034	.4615
180.0000	3645.0000	19.3350	.000036	.4610
360.0000	4048.0000	19.3280	.000038	.4602
540.0000	4423.1000	19.3190	.000040	.4592
720.0000	4790.3000	19.3000	.000043	.4579
900.0000	5138.5000	19.2670	.000045	.4564
1080.0000	5464.5000	19.2170	.000046	.4548
1260.0000	5766.1000	19.1470	.000048	.4529
1440.0000	6042.7000	19.0580	.000049	.4509
1620.0000	6296.3000	18.9520	.000051	.4487
1710.0000	6419.2000	18.9330	.000051	.4475

PRESSURE = 100.000ATM				
ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-630.0000	2351.2000	21.2950	.000027	.5154
-350.0000	2429.3000	20.8180	.000027	.5030
-360.0000	2618.0000	20.0230	.000029	.4814
-180.0000	2885.2000	19.5290	.000030	.4674
-90.0000	3058.3000	19.4180	.000032	.4641
90.0000	3446.8000	19.3490	.000034	.4617
180.0000	3646.2000	19.3400	.000036	.4612
360.0000	4041.0000	19.3310	.000038	.4603
540.0000	4425.2000	19.3220	.000040	.4593
720.0000	4794.5000	19.3050	.000043	.4580
900.0000	5147.7000	19.2760	.000045	.4565
1080.0000	5479.5000	19.2310	.000046	.4550
1260.0000	5788.1000	19.1670	.000048	.4532
1440.0000	6072.5000	19.0860	.000050	.4513
1620.0000	6335.2000	18.9870	.000051	.4492
1710.0000	6486.8000	18.9320	.000052	.4481

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

GENERAL INPUT INFORMATION *****

CCDY PT NO	INTEG PT NO	INT (I)	RATL NO	STREAM LENGTH INCH (S)	AXIAL LENGTH INCH (Z)	RADIAL LENGTH INCH (R)	BODY ANGLE DEG (THETB)	NORMALIZED ABLATION RATE (BPSP)	WALL TEMP DEG R (TW)	SURFACE ROUGHNESS RIL (RUFIL)	---EDGE CONDITION--- PRESSURE ATM (PE)	ENTHALPY BTU/LBM (HE)	VELOCITY FT/SEC (UE)
1	1	1	1	.00	.000	6.460	-42.418	.000	5500.00	.000	100.00	1692.20	.00
2	7	1	1	2.25	1.034	4.950	-45.334	.000	5500.00	.000	97.24	1658.70	1295.10
3	9	1	1	2.03	2.016	4.440	-47.770	.000	5500.00	.000	94.37	1637.89	1648.60
4	11	1	1	3.53	2.517	4.020	-34.150	.000	5500.00	.000	90.01	1603.28	2086.00
5	13	1	1	4.29	3.179	3.650	-25.127	.000	5500.00	.000	83.27	1592.10	2648.30
6	15	1	1	5.02	3.060	3.390	-10.264	.000	5500.00	.000	74.45	1477.10	3281.50
7	17	1	1	5.41	4.240	3.300	-12.612	.000	5500.00	.000	69.47	1431.66	3611.40
8	19	1	1	5.00	4.620	3.220	-8.437	.000	5500.00	.000	63.15	1370.15	4015.20
9	21	1	1	6.16	4.930	3.190	-3.845	.000	5500.00	.000	59.36	1331.20	4251.13
10	23	1	1	6.55	5.353	3.170	-4.319	.000	5500.00	.000	56.86	1304.30	4406.60
11	25	1	1	6.75	5.551	3.146	-3.305	.000	5500.00	.000	47.75	1197.36	4977.10
12	27	1	1	6.91	5.726	3.149	2.508	.000	5500.00	.000	44.59	1156.24	5179.60
13	29	1	1	7.16	5.972	3.164	4.753	.000	5500.00	.000	40.08	1094.15	5471.60
14	31	1	1	7.40	6.218	3.190	9.272	.000	5500.00	.000	35.70	1020.10	5765.60
15	33	1	1	7.82	6.621	3.270	13.563	.000	5500.00	.000	29.10	915.30	6236.50
16	35	1	1	8.22	7.006	3.300	21.472	.000	5500.00	.000	22.65	783.86	6743.20
17	37	1	1	9.21	7.918	3.780	28.187	.000	5500.00	.000	11.33	456.29	7065.70
18	39	1	1	13.12	13.039	6.640	25.916	.000	5500.00	.000	2.68	-81.62	5423.20
19	74	1	1	23.16	20.451	9.070	21.215	.000	5500.00	.000	1.27	-236.84	9978.50
20	102	1	1	54.09	30.764	13.500	17.835	.000	5500.00	.000	.64	-483.52	10308.00
21	123	1	1	40.03	44.164	17.500	16.618	.000	5500.00	.000	.34	-594.93	10700.00

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

VISCOS FLOW - EDGE PROPERTIES *****

BODY PT NO	INTS PT NO	STREAM LENGTH INCH	VELOCITY FT/SEC (UE)	MACH NO (MACH)	ENTHALPY BTU/LBM (HE)	TEMPERATURE DEG R (TE)	DENSITY LBM/FT3 (ROE)	VISCOSITY LBM/FT-SEC (VISE)	UNIT RE NO 1/FT (URE)
1	1	.0000	.0	.0000	1692.2	6434.0	4.031-01	5.154-05	0.000
2	7	2.2535	1295.1	.2759	1656.7	6384.2	3.954-01	5.128-05	9.985+06
3	9	2.8018	1646.8	.3574	1637.9	6351.7	3.859-01	5.112-05	1.245+07
4	11	3.0350	2086.0	.4542	1605.3	6299.8	3.714-01	5.084-05	1.524+07
5	13	4.2934	2348.3	.5509	1552.1	6213.6	3.487-01	5.039-05	1.833+07
6	15	5.0225	3281.5	.7274	1477.1	6094.2	3.184-01	4.976-05	2.100+07
7	17	5.4130	3611.4	.8058	1431.7	6021.3	3.018-01	4.937-05	2.202+07
8	19	5.8013	4015.2	.9042	1370.1	5917.8	2.787-01	4.861-05	2.293+07
9	21	6.1826	4281.1	.9630	1331.2	5853.1	2.611-01	4.846-05	2.326+07
10	23	6.5459	4405.6	1.0022	1304.3	5806.9	2.560-01	4.823-05	2.339+07
11	25	6.7960	4977.4	1.1513	1197.4	5627.0	2.224-01	4.723-05	2.343+07
12	27	6.9210	5175.8	1.2063	1156.2	5555.5	2.103-01	4.684-05	2.328+07
13	29	7.1975	5471.6	1.2873	1094.1	5449.1	1.931-01	4.626-05	2.284+07
14	31	7.4050	5755.0	1.3723	1026.1	5350.0	1.760-01	4.559-05	2.227+07
15	33	7.8158	6236.3	1.5146	918.3	5127.6	1.494-01	4.485-05	2.096+07
16	35	8.2162	6743.2	1.6003	783.9	4877.8	1.244-01	4.391-05	1.919+07
17	38	9.2117	7665.7	2.1090	456.3	4223.1	7.092-02	3.912-05	1.426+07
18	53	13.1212	9425.2	2.9745	-81.6	3051.7	2.321-02	3.153-05	6.924+06
19	74	23.1608	9976.5	3.4421	-296.6	2556.7	1.311-02	2.818-05	4.656+06
20	102	34.0932	10380.0	3.8909	-463.5	2169.8	7.760-03	2.521-05	3.197+06
21	138	48.0780	10700.0	4.3148	-595.0	1877.2	4.750-03	2.294-05	2.215+06

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

***** VISCIOUS FLOW - WALL AND B. L. RECOVERY PROPERTIES *****

BODY PT NO	INTS PT NO	STREAM LENGTH INCH	WALL TEMPERATURE DEG R	WALL ENTHALPY BTU/LBM	WALL DENSITY LBM/FT3	WALL VISCOSITY LBM/FT-SEC	RECOVERY ENTHALPY BTU/LBM	RECOVERY FACTOR	SENSBL CONV HEAT FLUX BTU/FT2-SEC	CF/2
(J)	(I)	(8)	(TM)	(HW)	(ROV)	(VISU)	(HR)	(RECOV)		
1	1	.0000	3500.0	1092.0	4.767-01	4.655-05	1692.2	.6721	2.664+02	1.000+30
2	7	2.2535	3500.0	1092.0	4.654-01	4.655-05	1684.4	.7673	8.660+02	2.264+03
3	9	2.6816	3500.0	1093.8	4.656-01	4.655-05	1679.5	.7673	9.407+02	2.096+03
4	11	3.5350	3500.0	1095.3	4.307-01	4.655-05	1672.0	.7673	1.030+03	1.922+03
5	13	4.2938	3500.0	1097.7	3.983-01	4.655-05	1659.6	.7673	1.104+03	1.797+03
6	15	5.0225	3500.0	1101.3	3.560-01	4.655-05	1642.1	.7673	1.128+03	1.703+03
7	17	5.4130	3500.0	1103.8	3.321-01	4.655-05	1631.6	.7673	1.112+03	1.652+03
8	19	5.6013	3500.0	1107.4	3.018-01	4.655-05	1617.3	.7673	1.073+03	1.616+03
9	21	6.1626	3500.0	1109.7	2.836-01	4.655-05	1608.3	.7673	1.033+03	1.560+03
10	23	6.5459	3500.0	1111.3	2.716-01	4.655-05	1602.0	.7673	1.006+03	1.548+03
11	25	6.7460	3500.0	1118.4	2.279-01	4.655-05	1577.2	.7673	8.963+02	1.574+03
12	27	6.9110	3500.0	1121.7	2.128-01	4.655-05	1567.7	.7673	8.456+02	1.546+03
13	29	7.1575	3500.0	1126.4	1.912-01	4.655-05	1553.3	.7673	7.705+02	1.525+03
14	31	7.4050	3500.0	1132.0	1.702-01	4.655-05	1538.0	.7673	6.905+02	1.503+03
15	33	7.6150	3500.0	1142.1	1.386-01	4.655-05	1512.0	.7673	5.597+02	1.471+03
16	35	8.2162	3500.0	1157.6	1.077-01	4.655-05	1481.6	.7673	4.182+02	1.437+03
17	38	9.8117	3500.0	1216.5	8.360-02	4.649-05	1406.0	.7673	1.479+02	1.332+03
18	53	15.1212	3500.0	1391.9	1.295-02	4.641-05	1281.8	.7673	-2.629+01	1.031+03
19	74	28.1600	3500.0	1550.6	9.813-03	4.635-05	1231.7	.7673	-3.575+01	8.782+04
20	102	34.0932	3500.0	1714.8	2.869-03	4.627-05	1191.9	.7673	-5.727+01	7.600+04
21	138	48.0780	3500.0	1953.9	1.485-03	4.618-05	1159.4	.7673	-8.687+01	6.692+04

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

VISCOS FLOW - BOUNDARY LAYER SOLUTION

BODY PT NO	1-126 PT NO	STREAM LENGTH INCH	MOMENTUM THICKNESS MIL	ENERGY THICKNESS MIL	SHAPE FACTOR	NON THICK RE NO	ENERGY THICK RE NO	HEAT TRANS COEFFICIENT LBM/FT ² -SEC	REYNOLDS ANAL FAC	INTER- MITTENCY	HEAT TRANS AUSMENT
(J)	(I)	(S)	(TME)	(PHI)	(HSF)	(RETH)	(REPH)	(NUCH)	(RAF)	(ADPL)	(RUFST)
1	1	.000	.422	1.026	1.975	0.000	0.000	4.771-01	.9780	.00	1.000
2	2	2.2535	1.658	3.502	1.096	1.376+03	2.981+03	1.464+00	1.2628	1.00	1.000
3	3	2.8618	1.74	4.801	1.081	2.012+03	4.981+03	1.606+00	1.2273	1.00	1.000
4	4	3.5350	2.085	5.832	1.083	2.677+03	7.405+03	1.786+00	1.2002	1.00	1.000
5	5	4.2388	2.261	6.963	1.100	3.433+03	1.063+04	1.765+00	1.1839	1.00	1.000
6	6	5.0223	2.403	8.037	1.133	4.208+03	1.406+04	2.085+00	1.1722	1.00	1.000
7	7	5.4130	2.523	8.654	1.155	4.630+03	1.590+04	2.108+00	1.1687	1.00	1.000
8	8	5.8013	2.594	9.384	1.190	4.937+03	1.784+04	2.104+00	1.1635	1.00	1.000
9	9	6.1628	2.636	9.976	1.211	5.477+03	1.523+04	2.072+00	1.1785	1.00	1.000
10	10	6.5459	3.068	10.654	1.225	5.981+03	2.077+04	2.051+00	1.1627	1.00	1.000
11	11	6.7460	2.741	11.379	1.299	5.333+03	2.222+04	1.953+00	1.1210	1.00	1.000
12	12	6.9110	2.769	11.890	1.328	5.370+03	2.296+04	1.896+00	1.1246	1.00	1.000
13	13	7.1073	2.863	12.591	1.372	5.430+03	2.397+04	1.805+00	1.1199	1.00	1.000
14	14	7.4088	2.971	13.446	1.424	5.512+03	2.495+04	1.701+00	1.1146	1.00	1.000
15	15	7.8158	3.173	15.099	1.518	5.533+03	2.629+04	1.514+00	1.1046	1.00	1.000
16	16	8.2162	3.398	17.344	1.645	5.430+03	2.770+04	1.291+00	1.0881	1.00	1.000
17	17	9.2117	4.247	26.760	2.052	5.046+03	3.180+04	7.608-01	1.0512	1.00	1.000
18	18	15.1212	9.441	63.936	3.204	5.477+03	3.690+04	2.388-01	1.0390	1.00	1.000
19	19	23.1600	15.329	123.554	4.005	5.947+03	4.570+04	1.196-01	1.0409	1.00	1.000
20	20	34.0922	25.402	36.436	4.867	6.235+03	2.570+04	7.129-02	1.1637	1.00	1.000
21	21	48.6780	38.608	50.479	5.799	6.251+03	9.320+03	4.761-02	1.3996	1.00	1.000

Sample Problem 2

A rough wall calculation for the C/CAN nozzle with a HT 90/18 propellant was performed. The details of this system were given in Section 3. Fifty-six body points were input. The surface roughness and the wall temperature used in this calculation are 2 mil and 4939°R respectively. Solutions at all the integration points were printed (1PRNT=2).

96178

2.

61

9 18 1

1.	26667+04	90000+03	28803+02	34863+00	-33776-01	14746-04	6444
	26990+04	12600+04	27118+02	32084+00	-4321+00	18310-04	3702
	19698+04	16200+04	22876+02	1123+01	-49873+00	21204-04	4607
	17560+04	19800+04	22341+02	44314+00	-3915-02	24118-04	4643
	18994+04	23400+04	22337+02	43167+00	-10621-02	26909-04	4746
	14428+04	27000+04	22327+02	44164+00	-6240-02	29563-04	4813
	12754+04	30600+04	22294+02	46731+00	-18977-01	32096-04	4871
	11871+04	34200+04	22236+02	48885+00	-27994-01	34326-04	4920
	92709+03	37800+04	22165+02	51523+00	-38372-01	36867-04	4954
	7125+03	41400+04	22664+02	58244+00	-6579-01	39124-04	4969
	4335+03	45000+04	21888+02	72885+00	-13551+00	41296-04	4959
	3171+03	48600+04	21957+02	10032+01	-27779+00	43365-04	4907
	4955+03	52200+04	20958+02	14912+01	-53823+00	45303-04	4799
	1211+03	55800+04	19364+02	22588+01	-96797+00	47063-04	4613
	19008+04	59400+04	18529+02	32253+01	-14434+01	48603-04	4346
	32249+04	63000+04	16811+02	40748+01	-13315+01	49928-04	4035
	4774+04	66600+04	15126+02	43731+01	-19062+01	51117-04	3746
	69360+04	72000+04	13237+02	55309+01	-14271+01	52916-04	3437
2.	26590+04	90000+03	28854+02	32882+00	-13201-01	14748-04	6473
	24880+04	12600+04	28006+02	64148+00	-23925+00	18362-04	6059
	11287+04	16200+04	24688+02	13833+01	-78374+00	21886-04	5082
	17427+04	19800+04	22408+02	52345+00	-74456-01	24143-04	4660
	15998+04	23400+04	22339+02	43147+00	-19958-02	26910-04	4746
	14445+04	27000+04	22333+02	43397+00	-30331-02	29563-04	4813
	12856+04	30600+04	22316+02	45123+00	-10426-01	32099-04	4861
	1180+04	34200+04	22276+02	47342+00	-20529-01	34332-04	4904
	94313+03	37800+04	22223+02	49298+00	-28673-01	36876-04	4941
	76260+03	41400+04	22154+02	52482+00	-41386-01	39141-04	4965
	54314+03	45000+04	22555+02	59065+00	-71052-01	41331-04	4973
	3545+03	48600+04	21889+02	70821+00	-13265+00	43442-04	4957
	42780+02	52200+04	21604+02	91314+00	-24632+00	45466-04	4913
	3411+03	55800+04	21129+02	12437+01	-43650+00	47382-04	4830
	8715+03	59400+04	20391+02	17263+01	-71892+00	49164-04	4693
	14990+04	63000+04	19851+02	23303+01	-10701+01	50745-04	4499
	23509+04	66600+04	18953+02	29463+01	-14121+01	52239-04	4261
	43277+04	72000+04	15963+02	35308+01	-16896+01	54168-04	3892
3.	26495+04	90000+03	28866+02	31416+00	-10725-01	14749-04	6482
	25088+04	12600+04	28249+02	56254+00	-17226+00	18376-04	6160
	21283+04	16200+04	25549+02	12181+01	-68520+00	21466-04	5390
	17797+04	19800+04	22379+02	69741+00	-23909+00	24144-04	4702
	14888+04	23400+04	22344+02	43581+00	-53166-02	26910-04	4748
	14880+04	27000+04	22335+02	43217+00	-23115-02	29564-04	4812
	12873+04	30600+04	22322+02	44597+00	-79521-02	32100-04	4859
	11280+04	34200+04	22292+02	46683+00	-17126-01	34334-04	4899
	95143+03	37800+04	22244+02	48604+00	-23321-01	36879-04	4934
	7740+03	41400+04	22184+02	51098+00	-35093-01	39146-04	4960
	58883+03	45000+04	22103+02	55846+00	-53653-01	41340-04	4973
	46647+03	48600+04	21376+02	64035+00	-98824-01	43462-04	4966

11397.03	5280.00	21766.02	70260.00	-17815.00	4990.00	4930
20751.03	5500.00	21422.02	10100.00	-3115.00	4740.00	4881
62059.03	3540.00	20885.02	13490.01	-52568.00	4930.00	4784
11521.00	6300.00	20185.02	17982.01	-79810.00	51019.00	4639
19389.04	6660.00	19879.02	23103.01	-10999.01	52587.00	4447
43727.00	7200.00	17232.02	29800.01	-19849.01	54670.00	4114
26						
26979.00	9000.00	20875.02	30940.00	-7996.02	14749.00	6400
25101.03	12600.00	24330.02	50310.00	-1240.00	18300.00	6237
22959.00	16200.00	23008.02	10311.01	-3551.00	21532.00	5561
18221.00	1980.00	25015.02	97447.00	-64448.00	24197.00	4812
16228.00	23400.00	22362.02	44942.00	-21289.01	26911.00	4752
14954.00	27000.00	22330.02	48144.00	-27953.02	29340.00	4812
12886.00	30600.00	2327.02	44180.00	-60799.02	32100.00	4837
11283.00	34200.00	22303.02	46050.00	-13092.01	34533.00	4894
95699.03	37800.00	22663.02	47961.00	-2029.01	36802.00	4928
78077.03	41000.00	22211.02	50057.00	-80218.01	39151.00	4954
59087.03	45000.00	22143.02	53567.00	-49802.01	41340.00	4971
39269.03	48600.00	22044.02	59317.00	-75000.01	43477.00	4970
16282.03	52200.00	21887.02	69211.00	-13039.00	45333.00	4954
11370.03	55800.00	21637.02	84995.00	-22368.00	47510.00	4913
45422.03	59400.00	21347.02	10049.01	-34840.00	49400.00	4846
9037.03	63000.00	20675.02	14060.01	-52030.00	51169.00	4743
14000.00	66600.00	19093.02	18000.01	-82368.00	52851.00	4597
86300.00	72000.00	18374.02	24140.01	-13101.01	55103.00	4317
20						
26801.00	9000.00	20879.02	30737.00	-61323.02	14750.00	4490
25100.00	12600.00	20512.02	47900.00	-10730.00	18391.00	5273
22716.00	16200.00	26691.02	93433.00	-4602.00	21544.00	5062
14600.00	19800.00	23420.02	11013.01	-61087.00	24245.00	4916
1647.00	23400.00	22389.02	47250.00	-45157.01	26916.00	4759
1457.00	27000.00	22341.02	43107.00	-3956.02	29564.00	4812
12092.00	30600.00	22330.02	43992.00	-53087.02	32101.00	4856
11379.00	34200.00	22309.02	45723.00	-12160.01	34536.00	4892
5967.03	37800.00	22273.02	47601.00	-20111.01	36840.00	4824
78512.03	41000.00	22225.02	49557.00	-27782.01	39133.00	4951
40101.03	45000.00	22163.02	52580.00	-40062.01	41332.00	4968
40503.03	48600.00	22077.02	57230.00	-44435.01	43484.00	4971
18573.03	52200.00	21944.02	65250.00	-10935.00	45549.00	4960
70484.03	55800.00	21735.02	78007.00	-10499.00	47541.00	4950
84330.03	59400.00	21412.02	96975.00	-30201.00	49451.00	4876
77748.03	63000.00	20936.02	12321.01	-47127.00	51247.00	4790
12786.00	66600.00	20278.02	15615.01	-60714.00	52973.00	4668
32696.00	72000.00	18955.02	21104.01	-10472.01	55512.00	4422
40						
26502.00	9000.00	20801.02	30610.00	-52886.02	14750.00	4491
25169.00	12600.00	20562.02	45924.00	-43794.01	18394.00	4294
2275.00	16200.00	26936.02	87210.00	-43765.00	21503.00	5761
18508.00	19800.00	23760.02	11503.01	-6492.00	24284.00	5004
16082.00	23400.00	22424.02	50171.00	-75503.01	26921.00	4768
2461.00	27000.00	22343.02	43299.00	-55623.02	29545.00	4813
12896.00	30600.00	22332.02	43802.00	-49400.02	32101.00	4856
11289.00	34200.00	22313.02	45502.00	-11052.01	34537.00	4891
96173.03	37800.00	22279.02	47349.00	-18760.01	36805.00	4922
78799.03	41000.00	22234.02	49235.00	-26175.01	39135.00	4948
60628.03	45000.00	22177.02	51933.00	-37063.01	41335.00	4967
41273.03	48600.00	22090.02	55987.00	-50117.01	43489.00	4971

..19373+03	..3220+04	..2179+02	..6234+00	..7602+01	..4537-04	..4962
..45950+02	..35800+04	..2179+02	..7280+00	..1620+00	..4753-04	..4938
..38864+03	..59400+04	..2179+02	..9014+00	..2637+00	..4947-04	..4892
..78207+03	..63000+04	..2179+02	..1122+01	..1018+00	..5133-04	..4918
..11385+04	..66600+04	..2179+02	..1416+01	..6019+00	..5307-04	..4711
..20366+04	..72000+04	..2179+02	..1915+01	..9378+00	..5541-04	..4490
80.						
..25553+04	..90800+03	..2888+02	..3032+00	..1706+02	..14750-04	..4492
..25166+04	..12600+04	..2888+02	..4777+00	..4036+01	..1639-04	..6309
..22587+04	..16206+04	..2711+02	..6275+00	..4022+00	..2157-04	..5817
..19387+04	..19800+04	..2404+02	..1164+01	..6897+00	..2431-04	..5978
..16123+04	..23400+04	..2247+02	..5397+00	..1101+00	..2627-04	..4779
..14464+04	..27000+04	..2347+02	..9361+00	..7781+02	..2958-04	..4814
..12399+04	..30600+04	..2233+02	..4381+00	..4815+02	..3210-04	..4856
..11296+04	..34200+04	..2213+02	..4534+00	..1026+01	..3457-04	..4496
..94212+03	..37800+04	..2284+02	..4713+00	..1729+01	..3685-04	..4820
..79018+03	..41400+04	..2241+02	..4901+00	..2498+01	..3915-04	..4946
..60952+03	..45000+04	..2217+02	..5150+00	..3497+01	..4135-04	..4963
..41818+03	..48600+04	..2213+02	..5513+00	..5378+01	..4342-04	..4470
..28947+03	..52200+04	..2204+02	..6132+00	..8228+01	..4563-04	..4964
..27427+02	..55800+04	..2183+02	..7189+00	..1463+00	..4757-04	..4943
..30806+03	..59400+04	..2181+02	..8593+00	..2371+00	..4947-04	..4803
..45649+03	..63000+04	..2205+02	..1037+01	..1688+00	..5135-04	..4837
..18765+04	..66600+04	..2068+02	..1316+01	..3423+00	..5308-04	..4780
..19096+04	..72000+04	..1959+02	..1762+01	..4761+00	..5553-04	..4537
60.						
..26353+04	..9400+03	..2888+02	..3068+00	..2707+02	..14750-04	..4492
..25199+04	..12600+04	..2888+02	..4777+00	..7732+01	..1639-04	..6321
..23711+04	..16206+04	..2744+02	..7930+00	..3748+00	..2160-04	..5861
..19363+04	..19800+04	..2262+02	..1162+01	..5961+00	..2434-04	..5141
..16173+04	..23400+04	..2215+02	..5703+00	..1471+00	..2693-04	..4791
..14468+04	..27000+04	..2231+02	..4370+00	..1075+01	..2958-04	..4815
..12392+04	..30600+04	..2233+02	..4534+00	..8324+02	..3210-04	..4856
..11292+04	..34200+04	..2217+02	..4528+00	..9680+02	..3457-04	..4496
..94413+03	..37800+04	..2284+02	..4703+00	..1690+01	..3685-04	..4819
..79175+03	..41400+04	..2247+02	..4818+00	..2498+01	..3915-04	..4946
..61203+03	..45000+04	..2194+02	..5119+00	..3332+01	..4135-04	..4964
..42323+03	..48600+04	..2124+02	..5451+00	..5078+01	..4342-04	..4470
..21678+03	..52200+04	..2203+02	..6014+00	..8228+01	..4563-04	..4964
..14427+02	..55800+04	..2186+02	..6903+00	..1348+00	..4757-04	..4943
..28344+03	..59400+04	..2163+02	..8232+00	..2147+00	..4947-04	..4803
..61388+03	..63000+04	..2287+02	..1037+01	..3749+00	..5135-04	..4837
..18488+04	..66600+04	..2083+02	..1241+01	..5778+00	..5313-04	..4782
..18003+04	..72000+04	..1979+02	..1678+01	..7934+00	..5560-04	..4537
70.						
..26353+04	..98000+03	..2888+02	..3068+00	..3937+02	..14750-04	..4492
..25199+04	..12600+04	..2888+02	..4777+00	..7109+01	..1639-04	..6329
..23711+04	..16206+04	..2735+02	..7659+00	..3271+00	..2161-04	..5893
..19363+04	..19800+04	..2262+02	..1151+01	..5911+03	..2436-04	..5193
..16173+04	..23400+04	..2215+02	..6061+00	..1846+00	..2694-04	..4803
..14468+04	..27000+04	..2231+02	..4391+00	..1362+01	..2956-04	..4814
..12392+04	..30600+04	..2233+02	..4573+00	..9605+02	..3210-04	..4856
..11292+04	..34200+04	..2219+02	..4512+00	..2120+02	..3457-04	..4496
..94413+03	..37800+04	..2291+02	..4678+00	..1621+01	..3685-04	..4820
..79175+03	..41400+04	..2251+02	..4849+00	..3250+01	..3915-04	..4946
..61203+03	..45000+04	..2201+02	..5093+00	..3218+01	..4135-04	..4963
..42323+03	..48600+04	..2184+02	..5402+00	..4807+01	..4342-04	..4470
..21678+03	..52200+04	..2218+02	..5402+00	..4807+01	..4563-04	..4964

.22259+03	.52200+00	.22037+02	.59236+00	.77009-01	.45571-04	.4966
.44459+01	.59000+00	.21052+02	.67448+00	.12592+00	.47561-04	.4950
.26761+03	.59400+00	.21675+02	.79603+00	.20223+00	.49522-04	.4916
.50336+03	.63000+00	.21351+02	.96546+00	.31336+00	.51307-04	.4861
.96908+03	.66000+00	.20908+02	.11856+01	.46272+00	.53166-04	.4779
.17151+04	.72000+00	.19950+02	.15074+01	.74292+00	.55633-04	.4603

SAMPLE PROBLEM 2 OUTPUT

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

NUMBER OF MATERIALS = 1
 CM/CH = .76168
 ISENTROPIC EXPONENT = 1.16490

MATL	STB	BTM	SLB	SLH
1	.35000	.35000	.50000	.50000

NS = 56
 ISRUPT = 1
 MKEYCR = 7
 IPANT = 2
 OLTRAN = .00000 INCHES

ABRUPT TRANSITION

FLOW IS TURBULENT

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

THERMODYNAMIC TABLE *****

PRESSURE = 1.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-2646.7000	900.0000	20.0000	.000015	.6444
-2435.0000	1200.0000	21.1180	.000016	.5702
-1969.0000	1620.0000	22.6700	.000021	.4607
-1756.0000	1980.0000	22.5410	.000024	.4653
-1595.4000	2340.0000	22.3370	.000027	.4746
-1442.8000	2700.0000	22.3270	.000030	.4815
-1279.4000	3060.0000	22.2940	.000032	.4871
-1107.1000	3420.0000	22.2360	.000035	.4920
-927.0900	3780.0000	22.1650	.000037	.4954
-731.2500	4140.0000	22.0640	.000039	.4969
-498.3500	4500.0000	21.8800	.000041	.4959
-191.7100	4860.0000	21.5570	.000043	.4907
249.8500	5220.0000	20.9580	.000045	.4799
916.1100	5580.0000	19.9640	.000047	.4613
1900.8000	5940.0000	18.5290	.000049	.4346
3224.9000	6300.0000	16.6110	.000050	.4035
4767.6000	6660.0000	15.1260	.000051	.3746
6954.0000	7200.0000	13.2370	.000053	.3437

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

PRESSURE = 5.000ATM				PRANDTL
ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	NUMBER
-2649.0000	900.0000	26.8540	.000015	.6475
-2486.0000	1260.0000	26.0000	.000018	.6059
-2126.7000	1620.0000	24.6880	.000021	.5082
-1762.7000	1980.0000	22.4080	.000024	.4660
-1595.8000	2340.0000	22.3320	.000027	.4746
-1444.5000	2700.0000	22.3330	.000030	.4813
-1283.6000	3060.0000	22.3160	.000032	.4861
-1119.0000	3420.0000	22.2780	.000035	.4904
-945.1300	3780.0000	22.2230	.000037	.4941
-762.6000	4140.0000	22.1540	.000039	.4965
-585.1400	4500.0000	22.0550	.000041	.4973
-331.4500	4860.0000	21.8890	.000043	.4957
-42.7800	5220.0000	21.6040	.000045	.4913
341.1100	5580.0000	21.1290	.000047	.4830
871.1500	5940.0000	20.3910	.000049	.4693
1599.0000	6300.0000	19.3510	.000051	.4499
2550.9000	6660.0000	16.0580	.000052	.4261
4327.7000	7200.0000	15.9630	.000054	.3892

PRESSURE = 10.000ATM				PRANDTL
ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	NUMBER
-2649.3003	900.0000	26.8660	.000015	.6482
-2500.8000	1260.0000	26.0490	.000018	.6160
-2192.3000	1620.0000	25.5490	.000021	.5330
-1779.7000	1980.0000	22.5790	.000024	.4702
-1600.3000	2340.0000	22.3440	.000027	.4748
-1445.0000	2700.0000	22.3350	.000030	.4812
-1287.3000	3060.0000	22.3220	.000032	.4859
-1123.0000	3420.0000	22.2920	.000035	.4899
-951.4500	3780.0000	22.2440	.000037	.4934
-772.4000	4140.0000	22.1840	.000039	.4960
-580.8300	4500.0000	22.1030	.000041	.4973
-366.4700	4860.0000	21.9760	.000043	.4966
-112.4700	5220.0000	21.7660	.000046	.4938
207.3100	5580.0000	21.4250	.000047	.4881
628.5000	5940.0000	20.8820	.000049	.4784
1192.1000	6300.0000	20.1010	.000051	.4639
1930.9000	6660.0000	19.0790	.000053	.4447
3372.7000	7200.0000	17.2320	.000055	.4114

MOMENTUM ENERGY INTEGRATION TECHNIQUE (WEII)

PRESSURE = 20.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-2.9000	900.0000	26.8750	.000015	.6486
-7.1000	1260.0000	26.8300	.000018	.6237
-15.9000	1620.0000	26.3080	.000022	.5561
-22.1000	1980.0000	23.0150	.000024	.4612
-1602.0000	2340.0000	22.3620	.000027	.4752
-1445.4000	2700.0000	22.3580	.000030	.4612
-1288.6000	3060.0000	22.3270	.000032	.4657
-1126.3000	3420.0000	22.3030	.000035	.4894
-956.9900	3780.0000	22.2630	.000037	.4928
-786.7700	4140.0000	22.2110	.000039	.4954
-595.8700	4500.0000	22.1830	.000041	.4971
-392.6900	4860.0000	22.0840	.000043	.4970
-162.6200	5220.0000	21.8870	.000046	.4954
112.7000	5580.0000	21.6370	.000048	.4915
458.4200	5940.0000	21.2770	.000049	.4848
904.3700	6300.0000	20.6750	.000051	.4743
1480.0000	6660.0000	17.8930	.000053	.4597
2620.4000	7200.0000	16.3740	.000055	.4317

PRESSURE = 30.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-2650.1000	900.0000	26.8750	.000015	.6498
-2514.4000	1260.0000	26.5120	.000018	.6273
-2271.6000	1620.0000	26.6910	.000022	.5662
-1869.0000	1980.0000	23.4200	.000024	.4916
-1604.7000	2340.0000	22.3690	.000027	.4759
-1445.7000	2700.0000	22.3410	.000030	.4612
-1289.2000	3060.0000	22.3300	.000032	.4856
-1127.9000	3420.0000	22.3030	.000035	.4892
-959.8700	3780.0000	22.2730	.000037	.4924
-786.1200	4140.0000	22.2230	.000039	.4931
-601.8100	4500.0000	22.1630	.000041	.4968
-405.0300	4860.0000	22.0770	.000043	.4971
-185.7500	5220.0000	21.9440	.000046	.4960
70.8840	5580.0000	21.7350	.000048	.4938
383.3600	5940.0000	21.4120	.000049	.4876
777.4800	6300.0000	20.9360	.000051	.4790
1278.6000	6660.0000	20.2780	.000053	.4668
2269.8000	7200.0000	18.9550	.000055	.4322

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

PRESSURE = 40.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-2650.2000	900.0000	26.8810	.000015	.6491
-2516.9000	1260.0000	26.5620	.000018	.6296
-2287.5000	1620.0000	26.9360	.000022	.5761
-1894.8000	1980.0000	23.7600	.000024	.5004
-1608.2000	2340.0000	22.4240	.000027	.4766
-1446.1000	2700.0000	22.3450	.000030	.4813
-1289.6000	3060.0000	22.3320	.000032	.4856
-1128.9000	3420.0000	22.3150	.000035	.4891
-961.7500	3780.0000	22.2790	.000037	.4922
-787.9900	4140.0000	22.2340	.000039	.4948
-606.2800	4500.0000	22.1770	.000041	.4967
-412.7300	4860.0000	22.0980	.000043	.4971
-199.7300	5220.0000	21.9790	.000046	.4962
45.0980	5580.0000	21.7940	.000048	.4938
338.6400	5940.0000	21.5120	.000049	.4892
702.0700	6300.0000	21.0950	.000051	.4818
1158.5000	6660.0000	20.5150	.000053	.4711
2056.6000	7200.0000	19.3260	.000055	.4490

PRESSURE = 50.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-2650.3000	900.0000	26.8830	.000015	.6492
-2518.6000	1260.0000	26.5970	.000018	.6309
-2299.7000	1620.0000	27.1110	.000022	.5817
-1915.7000	1980.0000	24.8400	.000024	.5078
-1612.5000	2340.0000	22.4670	.000027	.4779
-1446.4000	2700.0000	22.3470	.000030	.4814
-1289.9000	3060.0000	22.3350	.000032	.4856
-1129.6000	3420.0000	22.3150	.000035	.4890
-963.1200	3780.0000	22.2840	.000037	.4920
-790.1000	4140.0000	22.2410	.000039	.4946
-609.5200	4500.0000	22.1870	.000041	.4965
-418.1800	4860.0000	22.1150	.000043	.4970
-209.4700	5220.0000	22.0040	.000046	.4964
27.6270	5580.0000	21.8360	.000048	.4943
308.8800	5940.0000	21.5610	.000049	.4903
630.6200	6300.0000	21.2050	.000051	.4818
1076.5000	6660.0000	20.6800	.000053	.4711
1509.6000	7200.0000	19.5900	.000055	.4490

MOENTUM ENERGY INTEGRATION TECHNIQUE (WEII)

PRESSURE = 60.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-2659.3000	900.0000	26.6640	.000015	.6493
-2519.9000	1260.0000	26.6230	.000018	.6321
-2337.1000	1620.0000	27.2440	.000022	.5861
-1936.3000	1980.0000	24.2020	.000024	.5191
-1617.3000	2340.0000	22.5150	.000027	.4791
-1446.8000	2700.0000	22.3510	.000030	.4618
-1290.2000	3060.0000	22.3340	.000032	.4636
-1130.2000	3420.0000	22.3170	.000035	.4809
-969.1900	3780.0000	22.2800	.000037	.4919
-791.7500	4140.0000	22.2470	.000039	.4944
-618.0300	4500.0000	22.1940	.000041	.4964
-422.3300	4860.0000	22.1240	.000043	.4970
-216.7400	5220.0000	22.0280	.000046	.4965
15.6270	5580.0000	21.8670	.000048	.4947
285.4400	5940.0000	21.6320	.000050	.4910
612.6000	6300.0000	21.2870	.000051	.4854
1016.0000	6660.0000	20.8050	.000053	.4762
1600.3000	7200.0000	19.7900	.000056	.4574

PRESSURE = 70.000ATM

ENTHALPY (BTU/LBM)	TEMPERATURE (DEG R)	MOLECULAR WEIGHT	VISCOSITY (LB/SEC-FT)	PRANDTL NUMBER
-2659.4000	900.0000	26.6850	.000015	.6493
-2519.9000	1260.0000	26.6430	.000018	.6329
-2317.7000	1620.0000	27.3500	.000022	.5895
-1932.6000	1980.0000	24.4860	.000024	.5195
-1622.6000	2340.0000	22.5680	.000027	.4805
-1407.2000	2700.0000	22.3550	.000030	.4816
-1296.4000	3060.0000	22.3360	.000032	.4856
-1130.6000	3420.0000	22.3190	.000035	.4888
-963.0500	3780.0000	22.2910	.000037	.4917
-793.1000	4140.0000	22.2510	.000039	.4943
-614.0700	4500.0000	22.2010	.000041	.4952
-423.6500	4860.0000	22.1340	.000043	.4969
-222.3500	5220.0000	22.0370	.000046	.4966
4.4499	5580.0000	21.8920	.000048	.4950
267.6130	5940.0000	21.6730	.000050	.4916
583.3600	6300.0000	21.3510	.000051	.4861
969.0800	6660.0000	20.9000	.000053	.4779
1712.1000	7200.0000	19.9500	.000056	.4603

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

GENERAL INPUT INFORMATION

BODY PT NO	INTG PT NO	MATL NO	STREAM LENGTH INCH (S)	AXIAL LENGTH INCH (Z)	RADIAL LENGTH INCH (R)	BODY ANGLE DEG (THETB)	NORMALIZED ABLATION RATE (BPSP)	WALL TEMP DEG R (TW)	SURFACE ROUGHNESS MIL (RUFIL)	---EDGE CONDITION---		
										PRESSURE ATM (PE)	ENTHALPY BTU/LBM (HE)	VELOCITY FT/SEC (UE)
1	1	1	.00	-2.250	2.120	-80.015	.000	4939.00	2.000	68.03	909.76	.00
2	2	1	.05	-2.242	2.073	-79.511	.000	4939.00	2.000	67.86	908.61	93.51
3	3	1	.10	-2.233	2.025	-78.608	.000	4939.00	2.000	67.70	907.86	187.32
4	4	1	.14	-2.225	1.978	-77.904	.000	4939.00	2.000	67.54	906.92	278.40
5	5	1	.19	-2.217	1.931	-77.201	.000	4939.00	2.000	67.38	905.97	378.87
6	6	1	.24	-2.208	1.883	-76.497	.000	4939.00	2.000	67.21	905.02	463.33
7	7	1	.29	-2.200	1.836	-75.793	.000	4939.00	2.000	67.05	904.07	555.80
8	8	1	.33	-2.193	1.799	-71.358	.000	4939.00	2.000	66.37	903.57	578.98
9	9	1	.37	-2.167	1.762	-66.923	.000	4939.00	2.000	66.06	903.06	602.00
10	10	1	.41	-2.150	1.725	-62.488	.000	4939.00	2.000	66.00	902.56	625.18
11	11	1	.46	-2.125	1.684	-59.040	.000	4939.00	2.000	66.65	901.72	639.75
12	12	1	.51	-2.100	1.644	-55.592	.000	4939.00	2.000	66.51	900.88	694.40
13	13	1	.55	-2.075	1.612	-52.656	.000	4939.00	2.000	66.35	899.94	729.00
14	14	1	.59	-2.050	1.579	-49.720	.000	4939.00	2.000	66.20	899.01	763.68
15	15	1	.62	-2.025	1.552	-47.071	.000	4939.00	2.000	66.03	897.99	798.28
16	16	1	.66	-2.000	1.526	-44.421	.000	4939.00	2.000	65.85	896.98	832.80
17	17	1	.69	-1.975	1.504	-42.057	.000	4939.00	2.000	65.76	896.43	858.18
18	18	1	.73	-1.950	1.481	-39.693	.000	4939.00	2.000	65.67	895.89	887.48
19	19	1	.76	-1.925	1.462	-37.534	.000	4939.00	2.000	65.48	894.74	901.90
20	20	1	.79	-1.900	1.443	-35.375	.000	4939.00	2.000	65.29	893.59	936.98
21	21	1	.82	-1.875	1.427	-32.958	.000	4939.00	2.000	65.19	892.98	953.65
22	22	1	.85	-1.850	1.410	-30.541	.000	4939.00	2.000	65.09	892.37	970.90
23	23	1	.88	-1.825	1.397	-27.935	.000	4939.00	2.000	64.99	891.74	987.98
24	24	1	.91	-1.800	1.384	-26.330	.000	4939.00	2.000	64.88	891.11	1008.00
25	25	1	.96	-1.750	1.361	-24.779	.000	4939.00	2.000	64.85	889.09	1057.00
26	26	1	1.02	-1.700	1.339	-24.228	.000	4939.00	2.000	64.22	887.07	1109.00
27	27	1	1.07	-1.650	1.316	-23.868	.000	4939.00	2.000	63.98	885.61	1183.88
28	28	1	1.13	-1.600	1.294	-23.509	.000	4939.00	2.000	63.75	884.18	1178.00
29	29	1	1.18	-1.550	1.273	-22.778	.000	4939.00	2.000	63.37	881.81	1229.58
30	30	1	1.23	-1.500	1.252	-22.048	.000	4939.00	2.000	62.99	879.46	1261.08
31	31	1	1.29	-1.450	1.233	-21.302	.000	4939.00	2.000	62.58	876.92	1332.00
32	32	1	1.34	-1.400	1.213	-20.556	.000	4939.00	2.000	62.18	874.37	1383.00
33	33	1	1.39	-1.350	1.195	-19.795	.000	4939.00	2.000	61.75	871.64	1434.58
34	34	1	1.45	-1.300	1.177	-19.034	.000	4939.00	2.000	61.32	868.90	1486.00
35	35	1	1.50	-1.250	1.161	-18.259	.000	4939.00	2.000	60.87	865.97	1537.00
36	36	1	1.55	-1.200	1.144	-17.484	.000	4939.00	2.000	60.42	863.04	1588.08
37	37	1	1.61	-1.150	1.129	-16.696	.000	4939.00	2.000	59.78	859.84	1656.00
38	38	1	1.66	-1.100	1.114	-15.908	.000	4939.00	2.000	59.14	854.64	1724.00
39	39	1	1.71	-1.050	1.100	-15.241	.000	4939.00	2.000	58.64	851.26	1775.00
40	40	1	1.76	-.950	1.087	-14.574	.000	4939.00	2.000	58.14	847.89	1826.00
41	41	1	1.81	-.900	1.074	-13.763	.000	4939.00	2.000	57.43	843.10	1893.58
42	42	1	1.86	-.850	1.062	-12.953	.000	4939.00	2.000	56.74	838.31	1961.00
43	43	1	1.92	-.800	1.052	-12.131	.000	4939.00	2.000	56.00	833.18	2028.50
44	44	1	1.97	-.800	1.041	-11.310	.000	4939.00	2.000	55.26	828.06	2096.00

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

BODY PT NO	INTES PT NO	MATL NO	STREAM LENGTH INCH (S)	AXIAL LENGTH INCH (Z)	RADIAL LENGTH INCH (R)	BODY ANGLE DEG (THETB)	NORMALIZED ABLATION RATE (BPSP)	WALL TEMP DEG R (TW)	SURFACE ROUGHNESS RIL (RUFMIL)	---EDGE CONDITION---	VELOCITY FT/SEC (UE)
										PRESSURE ATM (PE)	ENTHALPY BTU/LBM (HE)
21	45	1	2.02	-.750	1.031	-10.757	.000	4939.00	2.000	39.52	822.60
21	46	1	2.07	-.700	1.022	-10.204	.000	4939.00	2.000	53.76	817.13
22	47	1	2.12	-.650	1.013	-9.507	.000	4939.00	2.000	53.76	809.87
23	48	1	2.17	-.600	1.005	-8.811	.000	4939.00	2.000	51.81	802.60
23	49	1	2.22	-.550	.998	-7.638	.000	4939.00	2.000	51.00	796.42
24	50	1	2.27	-.500	.991	-6.466	.000	4939.00	2.000	50.21	790.24
24	51	1	2.34	-.453	.984	-5.962	.000	4939.00	2.000	48.79	779.01
24	52	1	2.40	-.367	.978	-5.457	.000	4939.00	2.000	47.42	767.79
24	53	1	2.47	-.300	.971	-4.953	.000	4939.00	2.000	46.00	756.56
25	54	1	2.52	-.250	.968	-4.679	.000	4939.00	2.000	45.02	747.42
25	55	1	2.57	-.200	.965	-4.405	.000	4939.00	2.000	43.99	738.28
26	56	1	2.62	-.150	.963	-4.119	.000	4939.00	2.000	42.92	728.67
26	57	1	2.67	-.100	.961	-3.832	.000	4939.00	2.000	41.68	719.06
27	58	1	2.72	-.050	.961	-3.546	.000	4939.00	2.000	40.17	702.72
27	59	1	2.77	.000	.960	-3.260	.000	4939.00	2.000	38.53	686.39
28	60	1	2.82	.050	.961	-2.974	.000	4939.00	2.000	36.11	662.12
28	61	1	2.87	.100	.961	-2.688	.000	4939.00	2.000	37.70	677.86
29	62	1	2.92	.150	.963	-2.402	.000	4939.00	2.000	36.45	664.65
29	63	1	2.97	.200	.968	-2.116	.000	4939.00	2.000	35.24	651.44
30	64	1	3.02	.250	.971	-1.830	.000	4939.00	2.000	34.02	637.61
30	65	1	3.07	.300	.975	-1.544	.000	4939.00	2.000	32.83	623.78
31	66	1	3.12	.350	.980	-1.258	.000	4939.00	2.000	31.64	609.35
31	67	1	3.17	.400	.985	-0.972	.000	4939.00	2.000	30.49	594.92
32	68	1	3.22	.450	.991	-0.686	.000	4939.00	2.000	29.34	579.92
32	69	1	3.27	.500	.996	-0.400	.000	4939.00	2.000	28.13	564.91
33	70	1	3.32	.550	.998	-0.114	.000	4939.00	2.000	26.06	533.79
33	71	1	3.37	.600	1.005	0.172	.000	4939.00	2.000	25.01	517.59
34	72	1	3.42	.650	1.013	0.458	.000	4939.00	2.000	23.99	501.59
34	73	1	3.48	.700	1.022	0.744	.000	4939.00	2.000	22.98	484.98
35	74	1	3.53	.750	1.031	1.030	.000	4939.00	2.000	21.07	468.57
35	75	1	3.58	.800	1.041	1.316	.000	4939.00	2.000	19.15	451.27
36	76	1	3.63	.850	1.051	1.602	.000	4939.00	2.000	17.08	434.18
37	77	1	3.68	.900	1.062	1.888	.000	4939.00	2.000	15.86	416.62
37	78	1	3.73	.950	1.074	2.174	.000	4939.00	2.000	14.40	399.06
38	79	1	3.78	1.000	1.087	2.460	.000	4939.00	2.000	13.66	370.64
38	80	1	3.83	1.050	1.105	2.746	.000	4939.00	2.000	13.66	342.23
38	81	1	3.92	1.100	1.123	3.032	.000	4939.00	2.000	14.73	313.81
39	82	1	3.99	1.150	1.141	3.318	.000	4939.00	2.000	13.77	288.56
39	83	1	4.08	1.200	1.163	3.604	.000	4939.00	2.000	12.88	262.92
39	84	1	4.16	1.250	1.185	3.890	.000	4939.00	2.000	12.05	237.47
40	85	1	4.25	1.300	1.207	4.176	.000	4939.00	2.000	11.23	211.19
40	86	1	4.33	1.350	1.230	4.462	.000	4939.00	2.000	10.47	184.91
40	87	1	4.42	1.400	1.252	4.748	.000	4939.00	2.000	9.77	158.63
40	88	1	4.51	1.450	1.275	5.034	.000	4939.00	2.000	9.28	136.21
41	89	1	4.59	1.500	1.297	5.320	.000	4939.00	2.000	8.64	113.78
41	90	1	4.68	1.550	1.319	5.606	.000	4939.00	2.000	8.15	91.36
41	91	1	4.77	1.600	1.341	5.892	.000	4939.00	2.000		

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

BODY PT NO (J)	INTG PT NO (I)	MATL NO (MATL)	STREAM LENGTH INCH (S)	AXIAL LENGTH INCH (Z)	RADIAL LENGTH INCH (R)	BODY ANGLE DEG (THETA)	NORMALIZED ABLATION RATE (BPSP)	WALL TEMP DEG R (TW)	SURFACE ROUGHNESS MIL (AUFMIL)	PRESSURE ATM (PE)	---EDGE CONDITION--- ENTHALPY BTU/LBM (HE)	VELOCITY FT/SEC (UE)
42	92	1	4.88	2.033	1.363	14.931	.000	4939.00	2.800	7.66	68.57	6438.67
42	93	1	4.94	2.117	1.386	14.967	.000	4939.00	2.800	7.20	45.79	6518.33
42	94	1	5.02	2.200	1.408	15.003	.000	4939.00	2.800	6.77	23.00	6598.08
43	95	1	5.11	2.283	1.430	15.039	.000	4939.00	2.800	6.43	4.57	6631.67
43	96	1	5.20	2.367	1.453	15.075	.000	4939.00	2.800	6.11	-13.85	6713.33
43	97	1	5.28	2.450	1.475	15.111	.000	4939.00	2.800	5.81	-32.27	6778.00
44	98	1	5.37	2.533	1.497	15.147	.000	4939.00	2.800	5.52	-50.81	6838.00
44	99	1	5.46	2.617	1.520	15.183	.000	4939.00	2.800	5.24	-69.33	6898.00
44	100	1	5.54	2.700	1.542	15.219	.000	4939.00	2.800	4.98	-87.85	6958.00
45	101	1	5.63	2.783	1.564	15.255	.000	4939.00	2.800	4.72	-106.49	7018.67
45	102	1	5.72	2.867	1.587	15.291	.000	4939.00	2.800	4.48	-125.08	7078.33
45	103	1	5.80	2.950	1.609	15.327	.000	4939.00	2.800	4.25	-143.68	7138.00
46	104	1	5.89	3.033	1.631	15.363	.000	4939.00	2.800	4.08	-157.63	7198.67
46	105	1	5.97	3.117	1.654	15.399	.000	4939.00	2.800	3.92	-171.59	7258.33
46	106	1	6.06	3.200	1.676	15.435	.000	4939.00	2.800	3.77	-185.54	7318.00
47	107	1	6.15	3.283	1.698	15.471	.000	4939.00	2.800	3.62	-199.47	7378.67
47	108	1	6.23	3.367	1.721	15.507	.000	4939.00	2.800	3.48	-213.41	7438.33
47	109	1	6.32	3.450	1.743	15.543	.000	4939.00	2.800	3.34	-227.34	7498.00
48	110	1	6.41	3.533	1.766	15.579	.000	4939.00	2.800	3.16	-245.85	7558.67
48	111	1	6.49	3.617	1.788	15.615	.000	4939.00	2.800	2.99	-264.36	7618.33
48	112	1	6.58	3.700	1.810	15.651	.000	4939.00	2.800	2.84	-282.87	7678.00
49	113	1	6.66	3.783	1.832	15.687	.000	4939.00	2.800	2.72	-296.67	7738.67
49	114	1	6.75	3.867	1.855	15.723	.000	4939.00	2.800	2.61	-310.46	7798.33
49	115	1	6.84	3.950	1.877	15.759	.000	4939.00	2.800	2.51	-324.26	7858.00
50	116	1	6.92	4.033	1.899	15.795	.000	4939.00	2.800	2.40	-337.96	7918.67
50	117	1	7.01	4.117	1.922	15.831	.000	4939.00	2.800	2.31	-351.67	7978.33
50	118	1	7.10	4.200	1.944	15.867	.000	4939.00	2.800	2.21	-365.37	8038.00
51	119	1	7.18	4.283	1.966	15.903	.000	4939.00	2.800	2.15	-374.44	8098.67
51	120	1	7.27	4.367	1.989	15.939	.000	4939.00	2.800	2.09	-383.52	8158.33
51	121	1	7.35	4.450	2.011	15.975	.000	4939.00	2.800	2.04	-392.59	8218.00
52	122	1	7.44	4.533	2.033	16.011	.000	4939.00	2.800	1.98	-406.09	8278.67
52	123	1	7.53	4.617	2.056	16.047	.000	4939.00	2.800	1.95	-415.59	8338.33
52	124	1	7.61	4.700	2.078	16.083	.000	4939.00	2.800	1.87	-433.09	8398.00
53	125	1	7.70	4.783	2.100	16.119	.000	4939.00	2.800	1.79	-453.09	8458.67
53	126	1	7.79	4.867	2.123	16.155	.000	4939.00	2.800	1.65	-459.42	8518.33
53	127	1	7.87	4.950	2.145	16.191	.000	4939.00	2.800	1.58	-473.19	8578.00
54	128	1	7.96	5.033	2.167	16.227	.000	4939.00	2.800	1.54	-482.03	8638.67
54	129	1	8.04	5.117	2.190	16.263	.000	4939.00	2.800	1.49	-490.68	8698.33
54	130	1	8.13	5.200	2.212	16.299	.000	4939.00	2.800	1.45	-499.72	8758.00
55	131	1	8.22	5.283	2.234	16.335	.000	4939.00	2.800	1.41	-508.46	8818.67
55	132	1	8.30	5.367	2.257	16.371	.000	4939.00	2.800	1.37	-517.24	8878.33
55	133	1	8.39	5.450	2.279	16.407	.000	4939.00	2.800	1.33	-526.00	8938.00
56	134	1	8.48	5.533	2.301	16.443	.000	4939.00	2.800	1.30	-534.77	9000.00
56	135	1	8.56	5.617	2.324	16.479	.000	4939.00	2.800	1.26	-543.34	9060.67
56	136	1	8.65	5.700	2.346	16.515	.000	4939.00	2.800	1.22	-552.61	9120.33

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

VISCOS FLOW - EDGE PROPERTIES

BODY PT NO	INTG PT NO	STREAM LENGTH INCH	VELOCITY FT/SEC (UE)	MACH NO (MACH)	ENTHALPY BTU/LBM (HE)	TEMPERATURE DEG R (TE)	DENSITY LBM/FT3 (RDE)	VISCOSITY LBM/FT-SEC (VISE)	UNIT RE NO 1/FT (URE)
1	1	.0000	0	.0000	909.8	6597.1	2.960-01	5.285-05	0.000
	2	.0401	93.5	.0219	908.8	6595.5	2.953-01	5.284-05	5.237+05
	3	.0961	187.3	.0439	907.9	6594.0	2.947-01	5.283-05	1.083+06
	4	.1442	278.4	.0652	906.9	6592.5	2.941-01	5.283-05	1.350+06
	5	.1922	370.9	.0869	906.0	6591.0	2.934-01	5.282-05	2.060+06
	6	.2403	463.3	.1086	905.0	6589.5	2.928-01	5.281-05	2.569+06
2	7	.2884	555.8	.1303	904.1	6588.0	2.922-01	5.280-05	3.075+06
	8	.3289	578.9	.1527	903.6	6587.2	2.916-01	5.280-05	3.200+06
	9	.3695	602.0	.1751	903.1	6586.4	2.912-01	5.279-05	3.328+06
3	10	.4101	625.1	.1975	902.6	6585.6	2.906-01	5.279-05	3.448+06
	11	.4517	659.7	.2200	901.7	6584.3	2.901-01	5.278-05	3.632+06
4	12	.4933	694.4	.2425	900.9	6583.0	2.894-01	5.277-05	3.816+06
	13	.5350	729.0	.2650	899.9	6581.5	2.888-01	5.276-05	3.999+06
5	14	.5766	763.6	.2875	899.0	6580.0	2.882-01	5.275-05	4.180+06
	15	.6182	798.2	.3100	897.0	6578.5	2.875-01	5.274-05	4.360+06
6	16	.6598	832.8	.3325	896.4	6576.9	2.868-01	5.274-05	4.539+06
	17	.7014	867.4	.3550	895.9	6575.2	2.862-01	5.274-05	4.717+06
7	18	.7429	901.9	.3775	894.7	6573.4	2.855-01	5.273-05	4.894+06
	19	.7845	936.4	.4000	893.0	6570.6	2.848-01	5.272-05	5.067+06
8	20	.8261	970.9	.4225	891.7	6567.7	2.841-01	5.271-05	5.241+06
	21	.8677	1005.0	.4450	889.1	6564.6	2.834-01	5.270-05	5.418+06
9	22	.9093	1039.0	.4675	887.1	6561.5	2.827-01	5.268-05	5.593+06
	23	.9509	1073.0	.4900	885.6	6559.2	2.820-01	5.265-05	5.768+06
10	24	.9925	1107.0	.5125	884.2	6557.0	2.813-01	5.264-05	5.943+06
	25	1.0341	1141.0	.5350	881.8	6553.4	2.806-01	5.263-05	6.118+06
11	26	1.0757	1175.0	.5575	879.5	6549.9	2.799-01	5.262-05	6.293+06
	27	1.1173	1209.0	.5800	876.9	6545.9	2.792-01	5.260-05	6.468+06
12	28	1.1589	1243.0	.6025	874.4	6542.1	2.785-01	5.258-05	6.643+06
	29	1.2005	1277.0	.6250	871.6	6537.9	2.778-01	5.257-05	6.818+06
13	30	1.2421	1311.0	.6475	868.9	6533.8	2.771-01	5.256-05	6.993+06
	31	1.2837	1345.0	.6700	866.0	6529.4	2.764-01	5.255-05	7.168+06
14	32	1.3253	1379.0	.6925	863.0	6525.1	2.757-01	5.254-05	7.343+06
	33	1.3669	1413.0	.7150	860.0	6520.8	2.750-01	5.253-05	7.518+06
15	34	1.4085	1447.0	.7375	857.0	6516.5	2.743-01	5.252-05	7.693+06
	35	1.4501	1481.0	.7600	853.0	6512.3	2.736-01	5.251-05	7.868+06
16	36	1.4917	1515.0	.7825	850.0	6508.0	2.729-01	5.250-05	8.043+06
	37	1.5333	1549.0	.8050	847.0	6503.7	2.722-01	5.249-05	8.218+06
17	38	1.5749	1583.0	.8275	844.0	6500.0	2.715-01	5.248-05	8.393+06
	39	1.6165	1617.0	.8500	841.0	6495.9	2.708-01	5.247-05	8.568+06
18	40	1.6581	1651.0	.8725	838.0	6491.7	2.701-01	5.246-05	8.743+06
	41	1.6997	1685.0	.8950	835.0	6487.2	2.694-01	5.245-05	8.918+06
19	42	1.7413	1719.0	.9175	832.0	6483.0	2.687-01	5.244-05	9.093+06
	43	1.7829	1753.0	.9400	829.0	6478.5	2.680-01	5.243-05	9.268+06
20	44	1.8245	1787.0	.9625	826.0	6474.2	2.673-01	5.242-05	9.443+06
	45	1.8661	1821.0	.9850	823.0	6469.9	2.666-01	5.241-05	9.618+06
	46	1.9077	1855.0	1.0075	820.0	6465.6	2.659-01	5.240-05	9.793+06

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

BODY PT NO	INTG PT NO	STREAM LENGTH INCH	VELOCITY FT/SEC (UE)	MACH NO (MACH)	ENTHALPY BTU/LBM (HE)	TEMPERATURE DEG R (TE)	DENSITY LBM/FT3 (HOE)	VISCOSITY LBM/FT-SEC (VISE)	UNIT RE NO 1/FT (UNLE)
21	48	2.0173	2162.5	.5123	822.6	6464.7	2.426-01	5.215-05	1.006+07
21	46	2.0582	2229.0	.5284	817.2	6456.8	2.356-01	5.212-05	1.023+07
22	47	2.1190	2312.5	.5487	809.9	6446.4	2.357-01	5.207-05	1.047+07
22	48	2.1697	2396.0	.5690	802.6	6436.1	2.318-01	5.201-05	1.068+07
23	49	2.2202	2462.0	.5851	796.4	6427.4	2.283-01	5.197-05	1.082+07
23	50	2.2706	2528.0	.6013	790.2	6418.9	2.253-01	5.192-05	1.097+07
24	51	2.3376	2637.3	.6282	779.0	6402.9	2.195-01	5.184-05	1.117+07
24	52	2.4096	2746.7	.6551	767.8	6387.2	2.150-01	5.176-05	1.135+07
24	53	2.4716	2856.0	.6822	756.6	6371.7	2.085-01	5.168-05	1.152+07
25	54	2.5217	2937.0	.7023	747.4	6359.4	2.042-01	5.162-05	1.162+07
25	55	2.5718	3010.0	.7225	738.3	6347.2	1.999-01	5.155-05	1.176+07
26	56	2.6219	3086.3	.7426	728.7	6334.5	1.955-01	5.149-05	1.177+07
26	57	2.6719	3179.0	.7628	719.1	6322.1	1.912-01	5.143-05	1.162+07
27	58	2.7219	3306.0	.7948	702.7	6301.4	1.841-01	5.132-05	1.186+07
27	59	2.7719	3433.0	.8272	686.4	6275.0	1.774-01	5.118-05	1.198+07
28	60	2.8219	3464.9	.8593	682.1	6268.2	1.737-01	5.111-05	1.198+07
28	61	2.8719	3496.0	.8934	677.9	6261.3	1.700-01	5.111-05	1.198+07
29	62	2.9219	3539.3	.9275	664.7	6240.5	1.659-01	5.108-05	1.189+07
29	63	2.9720	3683.0	.9618	651.4	6219.9	1.639-01	5.069-05	1.164+07
30	64	3.0221	3776.0	.9960	637.6	6198.9	1.588-01	5.077-05	1.181+07
30	65	3.0722	3869.0	.9404	623.8	6178.2	1.538-01	5.067-05	1.178+07
31	66	3.1224	3960.9	.9645	609.3	6157.1	1.488-01	5.058-05	1.164+07
31	67	3.1726	4052.0	.9886	594.9	6136.4	1.440-01	5.044-05	1.157+07
32	68	3.2229	4142.3	1.0128	579.9	6114.5	1.391-01	5.033-05	1.149+07
32	69	3.2732	4233.0	1.0370	564.9	6092.6	1.344-01	5.021-05	1.130+07
33	70	3.3237	4322.0	1.0610	549.3	6070.3	1.297-01	5.009-05	1.129+07
33	71	3.3741	4411.0	1.0851	533.8	6048.7	1.251-01	4.998-05	1.104+07
34	72	3.4243	4499.0	1.1090	517.7	6026.8	1.205-01	4.986-05	1.087+07
34	73	3.4756	4587.0	1.1330	501.6	6005.4	1.161-01	4.978-07	1.078+07
35	74	3.5265	4628.3	1.1457	485.0	5984.0	1.117-01	4.964-05	1.041+07
35	75	3.5774	4670.0	1.1583	468.4	5963.0	1.074-01	4.953-05	1.013+07
36	76	3.6283	4800.3	1.1932	451.3	5942.0	1.032-01	4.942-05	1.008+07
36	77	3.6795	4931.0	1.2286	431.2	5914.2	9.924-02	4.928-05	9.938+06
37	78	3.7311	5015.3	1.2530	417.4	5887.4	9.853-02	4.912-05	9.735+06
37	79	3.7826	5100.0	1.2775	399.1	5859.0	9.156-02	4.897-05	9.536+06
38	80	3.8317	5227.7	1.3150	370.6	5814.6	8.574-02	4.873-05	9.198+06
38	81	3.9207	5355.3	1.3527	342.2	5772.0	8.027-02	4.850-05	8.664+06
38	82	3.9558	5483.0	1.3905	313.8	5731.4	7.513-02	4.828-05	8.533+06
39	83	4.0760	5586.3	1.4222	288.4	5696.3	7.076-02	4.809-05	7.223+06
39	84	4.1622	5693.7	1.4540	262.9	5662.5	6.653-02	4.791-05	7.191+06
39	85	4.2484	5799.0	1.4859	237.5	5629.3	6.253-02	4.773-05	7.021+06
40	86	4.3347	5901.0	1.5172	211.2	5597.4	5.830-02	4.755-05	7.308+06
40	87	4.4211	6003.0	1.5491	184.9	5561.7	5.532-02	4.735-05	7.012+06
40	88	4.5074	6105.0	1.5819	158.6	5520.5	5.211-02	4.713-05	6.737+06
40	89	4.5936	6167.0	1.6089	136.2	5484.1	4.932-02	4.693-05	6.502+06
40	90	4.6798	6269.0	1.6360	113.8	5448.9	4.677-02	4.673-05	6.273+06
41	91	4.7660	6331.0	1.6632	91.4	5414.8	4.434-02	4.655-05	6.058+06

MOMENTUM ENERGY INTEGRATION TECHNIQUE (HEIT)

BODY PT NO	INTES PT NO	STREAM LENGTH INCH (S)	VELOCITY FT/SEC (UE)	MACH NO (MACH)	ENTHALPY BTU/LBM (HE)	TEMPERATURE DEG R (TE)	DENSITY LBM/FT ³ (ROE)	VISCOSITY LBM/FT-SEC (VISE)	UNIT RE NC 1/F ² (URE)
42	92	4.823	6430.7	1.6899	68.6	5301.2	4.196-02	4.636-03	5.631-16
	93	4.9389	6510.3	1.7167	45.8	5348.7	3.971-02	4.618-03	5.598-16
	94	5.0248	6590.0	1.7436	23.0	5377.5	3.757-02	4.601-03	5.582-16
	95	5.111	6631.7	1.7646	4.6	5292.5	3.590-02	4.587-03	5.564-16
	96	5.1974	6713.3	1.7850	-13.8	5271.5	3.428-02	4.575-03	5.539-06
	97	5.2836	6775.0	1.8063	-32.3	5277.3	3.276-02	4.562-03	4.865-16
	98	5.3699	6835.0	1.8277	-50.8	5221.3	3.129-02	4.548-03	4.703-16
	99	5.4562	6895.0	1.8493	-69.4	5192.4	2.989-02	4.531-03	4.549-16
	100	5.5425	6955.0	1.8711	-87.9	5153.1	2.856-02	4.515-03	4.401-16
	101	5.6287	7013.7	1.8927	-106.5	5133.0	2.727-02	4.497-03	4.253-16
	102	5.7150	7072.3	1.9143	-125.1	5103.5	2.603-02	4.480-03	4.108-06
	103	5.8013	7131.0	1.9361	-143.7	5074.5	2.484-02	4.463-03	3.969-06
	104	5.8876	7173.7	1.9521	-157.6	5033.0	2.398-02	4.451-03	3.864-16
	105	5.9738	7216.3	1.9681	-171.6	5031.0	2.314-02	4.439-03	3.782-16
	106	6.0601	7259.0	1.9842	-185.5	5010.9	2.234-02	4.427-03	3.668-06
	107	6.1464	7301.0	2.0004	-199.5	4989.7	2.155-02	4.415-03	3.564-06
	108	6.2327	7343.0	2.0167	-213.4	4968.2	2.080-02	4.403-03	3.469-06
	109	6.3189	7385.0	2.0331	-227.3	4946.8	2.007-02	4.391-03	3.376-16
	110	6.4052	7429.3	2.0548	-241.8	4918.3	1.913-02	4.374-03	3.284-06
	111	6.4915	7473.7	2.0766	-255.8	4889.9	1.824-02	4.358-03	3.191-16
	112	6.5778	7518.0	2.0987	-269.4	4861.5	1.729-02	4.342-03	3.098-06
	113	6.6640	7567.7	2.1146	-286.7	4830.4	1.676-02	4.330-03	2.998-06
	114	6.7503	7627.3	2.1305	-310.5	4819.4	1.616-02	4.317-03	2.894-06
	115	6.8366	7667.0	2.1466	-324.3	4798.3	1.558-02	4.305-03	2.793-06
	116	6.9229	7706.0	2.1628	-338.0	4776.4	1.502-02	4.292-03	2.697-06
	117	7.0091	7745.0	2.1794	-351.7	4753.4	1.449-02	4.279-03	2.602-06
	118	7.0954	7784.0	2.1960	-365.4	4730.7	1.397-02	4.265-03	2.508-06
	119	7.1817	7823.7	2.2069	-374.4	4715.8	1.363-02	4.256-03	2.414-06
	120	7.2679	7864.7	2.2179	-388.5	4701.0	1.330-02	4.248-03	2.320-06
	121	7.3542	7905.0	2.2288	-392.6	4686.4	1.298-02	4.239-03	2.226-06
	122	7.4405	7947.3	2.2451	-406.1	4664.7	1.251-02	4.227-03	2.132-06
	123	7.5268	7994.7	2.2614	-419.6	4643.3	1.206-02	4.214-03	2.038-06
	124	7.6130	8044.7	2.2777	-433.1	4622.2	1.162-02	4.202-03	1.944-06
	125	7.6993	8095.3	2.2938	-446.5	4601.5	1.120-02	4.190-03	1.850-06
	126	7.7855	8145.7	2.3098	-459.8	4581.1	1.079-02	4.178-03	1.756-06
	127	7.8719	8196.0	2.3260	-473.2	4560.9	1.039-02	4.166-03	1.662-06
	128	7.9581	8246.3	2.3423	-486.6	4540.6	1.013-02	4.158-03	1.568-06
	129	8.0444	8296.0	2.3586	-499.9	4521.2	9.661-03	4.150-03	1.474-06
	130	8.1307	8346.3	2.3749	-513.2	4501.9	9.637-03	4.143-03	1.380-06
	131	8.2170	8396.7	2.3912	-526.6	4482.6	9.613-03	4.134-03	1.286-06
	132	8.3032	8447.0	2.4075	-540.0	4463.3	9.589-03	4.125-03	1.192-06
	133	8.3895	8497.3	2.4238	-553.4	4444.0	9.565-03	4.115-03	1.108-06
	134	8.4758	8547.0	2.4401	-566.8	4424.7	9.541-03	4.106-03	1.024-06
	135	8.5621	8597.3	2.4564	-580.2	4405.4	9.517-03	4.097-03	1.733-16
	136	8.6483	8647.0	2.4727	-593.6	4386.1	9.493-03	4.088-03	1.641-16

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)
 VISCIOUS FLOW - WALL AND B. L. RECOVERY PROPERTIES

BODY PT NO (J)	INTG PT NO (I)	STREAM LENGTH INCH (S)	WALL TEMPERATURE DEG R (TW)	WALL ENTHALPY BTU/LBM (MW)	WALL DENSITY LBM/FT3 (RHO)	WALL VISCOSITY LBM/FT-SEC (VISH)	RECOVERY ENTHALPY BTU/LBM (MR)	RECOVERY FACTOR (RECUV)	SENSBL CONV HEAT FLUX BTU/FT2-SEC	CF/2
1	1	.0008	939.0	-380.4	0.170-01	0.395-05	909.8	.6998	9.480+02	1.000+00
	2	.0081	939.0	-380.3	0.160-01	0.395-05	908.9	.6998	9.464+02	2.719-02
	3	.0061	939.0	-380.2	0.150-01	0.395-05	908.4	.6998	9.435+02	1.358-02
	4	.0442	939.0	-380.1	0.140-01	0.395-05	908.0	.6998	8.312+02	1.116-02
	5	.1222	939.0	-380.1	0.130-01	0.395-05	908.1	.7882	1.746+03	1.432-02
	6	.2403	939.0	-380.1	0.120-01	0.395-05	908.4	.7882	1.713+03	1.855-02
2	7	.2884	939.0	-380.0	0.110-01	0.395-05	908.9	.7882	1.750+03	0.588+03
	8	.3229	939.0	-380.0	0.105-01	0.395-05	908.0	.7882	1.599+03	7.079+03
	9	.3695	939.0	-379.9	0.099-01	0.395-05	908.8	.7882	1.538+03	6.611-03
3	10	.4101	939.0	-379.9	0.094-01	0.395-05	908.7	.7882	1.544+03	6.562-03
	11	.4577	939.0	-379.9	0.085-01	0.395-05	908.6	.7882	1.563+03	6.219-03
4	12	.5053	939.0	-379.8	0.077-01	0.395-05	908.5	.7882	1.585+03	6.181-03
	13	.5463	939.0	-379.7	0.067-01	0.395-05	908.3	.7882	1.620+03	6.845-03
5	14	.5873	939.0	-379.7	0.057-01	0.395-05	908.2	.7882	1.656+03	8.594+03
	15	.6237	939.0	-379.6	0.047-01	0.395-05	908.0	.7882	1.698+03	9.970-03
6	16	.6602	939.0	-379.6	0.036-01	0.395-05	907.9	.7882	1.720+03	9.784-03
	17	.6930	939.0	-379.5	0.031-01	0.395-05	907.8	.7882	1.700+03	9.524+03
7	18	.7274	939.0	-379.5	0.025-01	0.395-05	907.7	.7882	1.721+03	9.468-03
	19	.7588	939.0	-379.4	0.013-01	0.395-05	907.6	.7882	1.783+03	9.688-03
8	20	.7902	939.0	-379.3	0.002-01	0.395-05	907.4	.7882	1.813+03	9.868-03
	21	.8202	939.0	-379.3	3.995-01	0.395-05	907.3	.7882	1.800+03	9.834-03
9	22	.8501	939.0	-379.3	3.989-01	0.395-05	907.2	.7882	1.806+03	9.778-03
	23	.8783	939.0	-379.2	3.983-01	0.395-05	907.1	.7882	1.814+03	9.716-03
10	24	.9045	939.0	-379.2	3.976-01	0.395-05	907.0	.7882	1.830+03	9.689-03
	25	.9313	939.0	-379.1	3.966-01	0.395-05	906.9	.7882	1.849+03	9.655-03
11	26	1.0162	939.0	-378.9	3.936-01	0.395-05	906.2	.7882	1.957+03	9.902-03
	27	1.0362	939.0	-378.8	3.921-01	0.395-05	906.0	.7882	1.983+03	9.965-03
12	28	1.0551	939.0	-378.7	3.907-01	0.395-05	905.3	.7882	2.042+03	9.983-03
	29	1.0710	939.0	-378.6	3.883-01	0.395-05	905.6	.7882	2.092+03	9.988-03
13	30	1.0800	939.0	-378.4	3.860-01	0.395-05	905.3	.7882	2.138+03	9.984-03
	31	1.0879	939.0	-378.3	3.835-01	0.395-05	904.5	.7882	2.182+03	9.986-03
14	32	1.0946	939.0	-378.1	3.810-01	0.395-05	904.8	.7882	2.221+03	9.988-03
	33	1.0979	939.0	-377.8	3.784-01	0.395-05	904.0	.7882	2.265+03	9.989-03
15	34	1.1006	939.0	-377.6	3.758-01	0.395-05	903.7	.7882	2.303+03	9.768-03
	35	1.1032	939.0	-377.4	3.733-01	0.395-05	903.2	.7882	2.345+03	9.765-03
16	36	1.1058	939.0	-377.1	3.702-01	0.395-05	902.8	.7882	2.410+03	9.799-03
	37	1.1076	939.0	-376.8	3.663-01	0.395-05	901.5	.7882	2.461+03	9.786-03
17	38	1.1094	939.0	-376.6	3.593-01	0.395-05	900.9	.7882	2.514+03	9.653-03
	39	1.1112	939.0	-376.4	3.562-01	0.395-05	900.4	.7882	2.563+03	9.648-03
18	40	1.1127	939.0	-376.1	3.519-01	0.395-05	899.6	.7882	2.605+03	9.648-03
	41	1.1144	939.0	-375.7	3.476-01	0.395-05	898.9	.7882	2.643+03	9.648-03
19	42	1.1154	939.0	-375.4	3.431-01	0.395-05	898.0	.7882	2.677+03	9.597-03
	43	1.1164	939.0	-375.0	3.386-01	0.395-05	897.3	.7882		

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

BODY PT NO (J)	INTEG PT NO (I)	STREAM LENGTH INCH (S)	WALL TEMPERATURE DEG R (TU)	WALL ENTHALPY BTU/LBM (HU)	WALL DENSITY LBM/FT ³ (RHO)	WALL VISCOSITY LBM/FT-SEC (VISM)	RECOVERY ENTHALPY BTU/LBM (HRI)	RECOVERY FACTOR (RECOV)	SENSBL CONV HEAT FLUX BTU/FT ² -SEC	CF/2
21	45	2.0173	4939.0	-374.7	3.339-01	4.395-05	896.3	.7882	2.705+03	0.567-03
	46	2.0682	4939.0	-374.3	3.293-01	4.395-05	895.4	.7882	2.735+03	0.561-03
22	47	2.1190	4939.0	-373.8	3.233-01	4.395-05	894.1	.7882	2.775+03	0.573-03
	48	2.1697	4939.0	-373.3	3.173-01	4.395-05	893.0	.7882	2.804+03	0.580-03
23	49	2.2202	4939.0	-372.9	3.124-01	4.395-05	891.9	.7882	2.812+03	0.582-03
	50	2.2706	4939.0	-372.5	3.075-01	4.395-05	890.9	.7882	2.825+03	0.581-03
	51	2.3374	4939.0	-371.7	2.988-01	4.395-05	888.6	.7882	2.845+03	0.583-03
24	52	2.4046	4939.0	-370.9	2.903-01	4.395-05	885.0	.7882	2.858+03	0.584-03
	53	2.4716	4939.0	-370.0	2.821-01	4.395-05	883.3	.7882	2.865+03	0.585-03
25	54	2.5217	4939.0	-369.4	2.756-01	4.394-05	881.7	.7882	2.860+03	0.586-03
	55	2.5718	4939.0	-368.7	2.692-01	4.394-05	879.9	.7882	2.854+03	0.587-03
26	56	2.6219	4939.0	-368.0	2.627-01	4.394-05	878.2	.7882	2.840+03	0.582-03
	57	2.6719	4939.0	-367.3	2.563-01	4.394-05	876.9	.7882	2.834+03	0.583-03
27	58	2.7219	4939.0	-366.1	2.498-01	4.394-05	874.9	.7882	2.818+03	0.581-03
	59	2.7719	4939.0	-364.8	2.357-01	4.394-05	872.0	.7882	2.778+03	0.575-03
28	60	2.8219	4939.0	-364.5	2.332-01	4.394-05	871.2	.7882	2.731+03	0.568-03
	61	2.8719	4939.0	-364.1	2.306-01	4.394-05	870.4	.7882	2.719+03	0.563-03
29	62	2.9219	4939.0	-363.1	2.230-01	4.394-05	867.6	.7882	2.690+03	0.558-03
	63	2.9720	4939.0	-362.0	2.155-01	4.394-05	865.1	.7882	2.652+03	0.553-03
30	64	3.0221	4939.0	-360.9	2.080-01	4.394-05	862.2	.7882	2.607+03	0.548-03
	65	3.0722	4939.0	-359.8	2.008-01	4.394-05	859.5	.7882	2.561+03	0.543-03
31	66	3.1224	4939.0	-358.6	1.934-01	4.394-05	856.4	.7882	2.508+03	0.538-03
	67	3.1726	4939.0	-357.4	1.864-01	4.394-05	853.5	.7882	2.456+03	0.533-03
32	68	3.2229	4939.0	-356.1	1.793-01	4.394-05	850.2	.7882	2.398+03	0.528-03
	69	3.2732	4939.0	-354.7	1.725-01	4.394-05	847.1	.7882	2.340+03	0.523-03
33	70	3.3237	4939.0	-353.3	1.657-01	4.394-05	843.6	.7882	2.277+03	0.518-03
	71	3.3741	4939.0	-351.8	1.592-01	4.393-05	840.2	.7882	2.216+03	0.513-03
34	72	3.4249	4939.0	-350.3	1.527-01	4.393-05	836.5	.7882	2.151+03	0.508-03
	73	3.4756	4939.0	-348.8	1.465-01	4.393-05	833.0	.7882	2.082+03	0.503-03
35	74	3.5265	4939.0	-347.3	1.403-01	4.393-05	828.4	.7882	1.973+03	0.498-03
	75	3.5774	4939.0	-345.7	1.344-01	4.393-05	824.9	.7882	1.886+03	0.493-03
36	76	3.6285	4939.0	-344.1	1.286-01	4.393-05	821.3	.7882	1.860+03	0.493-03
	77	3.6795	4939.0	-342.5	1.230-01	4.393-05	817.2	.7882	1.825+03	0.493-03
37	78	3.7311	4939.0	-340.5	1.175-01	4.393-05	812.9	.7882	1.793+03	0.491-03
	79	3.7826	4939.0	-338.5	1.122-01	4.393-05	808.8	.7882	1.689+03	0.486-03
38	80	3.8317	4939.0	-335.1	1.042-01	4.392-05	801.1	.7882	1.583+03	0.481-03
	81	3.9207	4939.0	-331.7	9.667-02	4.392-05	794.0	.7882	1.484+03	0.476-03
39	82	3.9898	4939.0	-328.3	8.973-02	4.392-05	787.4	.7882	1.388+03	0.471-03
	83	4.0760	4939.0	-325.3	8.308-02	4.392-05	780.3	.7882	1.300+03	0.466-03
40	84	4.1622	4939.0	-322.2	7.842-02	4.392-05	773.5	.7882	1.220+03	0.461-03
	85	4.2484	4939.0	-319.2	7.331-02	4.392-05	767.2	.7882	1.144+03	0.456-03
41	86	4.3347	4939.0	-316.0	6.834-02	4.391-05	759.7	.7882	1.067+03	0.451-03
	87	4.4211	4939.0	-312.6	6.370-02	4.391-05	752.5	.7882	9.950+02	0.446-03
42	88	4.5074	4939.0	-309.3	5.937-02	4.391-05	745.7	.7882	9.269+02	0.441-03
	89	4.5936	4939.0	-305.3	5.538-02	4.391-05	739.2	.7882	8.692+02	0.436-03
43	90	4.6798	4939.0	-301.9	5.254-02	4.391-05	732.6	.7882	8.157+02	0.431-03
	91	4.7660	4939.0	-298.2	4.949-02	4.390-05	726.7	.7882	7.652+02	0.426-03

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

BOOY PT NO	INTES PT NO	STREAM LENGTH INCH (S)	WALL TEMPERATURE DEG R (TW)	WALL ENTHALPY BTU/LBM (MW)	WALL DENSITY LBM/FT3 (ROW)	WALL VISCOSITY LBM/FT-SEC (VISH)	RECOVERY ENTHALPY BTU/LBM (HR)	RECOVERY FACTOR (RECOV)	SENSBL CONV HEAT FLUX BTU/FT2-SEC	CF/2
42	92	4.823	4339.0	-234.3	4.649-02	4.390-05	719.9	.7882	7.153+02	2.867-03
	93	4.9385	4339.0	-230.5	4.367-02	4.390-05	713.4	.7882	6.686+02	2.818-03
	94	5.0248	4339.0	-286.7	4.103-02	4.390-05	707.1	.7882	6.243+02	2.768-03
	95	5.1111	4339.0	-283.6	3.898-02	4.390-05	701.5	.7882	5.893+02	2.708-03
	96	5.1974	4339.0	-280.5	3.704-02	4.389-05	696.1	.7882	5.567+02	2.668-03
	97	5.2836	4339.0	-277.3	3.519-02	4.389-05	690.8	.7882	5.255+02	2.624-03
	98	5.3699	4339.0	-274.2	3.341-02	4.389-05	685.1	.7882	4.953+02	2.581-03
	99	5.4562	4339.0	-271.0	3.171-02	4.389-05	679.6	.7882	4.669+02	2.539-03
	100	5.5425	4339.0	-267.6	3.010-02	4.389-05	674.2	.7882	4.399+02	2.496-03
	101	5.6287	4339.0	-261.9	2.855-02	4.388-05	668.4	.7882	4.124+02	2.452-03
	102	5.7150	4339.0	-256.3	2.707-02	4.388-05	662.8	.7882	3.866+02	2.409-03
	103	5.8013	4339.0	-250.6	2.566-02	4.388-05	657.2	.7882	3.618+02	2.357-03
	104	5.8876	4339.0	-246.3	2.465-02	4.387-05	652.0	.7882	3.437+02	2.313-03
	105	5.9738	4339.0	-242.0	2.367-02	4.387-05	648.4	.7882	3.270+02	2.288-03
	106	6.0601	4339.0	-237.7	2.273-02	4.387-05	644.2	.7882	3.110+02	2.266-03
	107	6.1464	4339.0	-233.3	2.182-02	4.387-05	639.0	.7882	2.955+02	2.213-03
	108	6.2327	4339.0	-229.0	2.093-02	4.386-05	635.5	.7882	2.807+02	2.179-03
	109	6.3189	4339.0	-224.7	2.011-02	4.386-05	631.3	.7882	2.669+02	2.158-03
	110	6.4052	4339.0	-218.8	1.933-02	4.386-05	625.4	.7882	2.549+02	2.118-03
	111	6.4915	4339.0	-212.9	1.862-02	4.386-05	619.6	.7882	2.418+02	2.074-03
	112	6.5778	4339.0	-207.1	1.795-02	4.385-05	613.9	.7882	2.215+02	2.021-03
	113	6.6640	4339.0	-202.4	1.659-02	4.385-05	605.2	.7882	2.037+02	1.979-03
	114	6.7503	4339.0	-198.2	1.569-02	4.385-05	600.9	.7882	1.829+02	1.945-03
	115	6.8366	4339.0	-193.8	1.505-02	4.384-05	596.6	.7882	1.625+02	1.912-03
	116	6.9229	4339.0	-189.3	1.443-02	4.384-05	592.4	.7882	1.431+02	1.877-03
	117	7.0091	4339.0	-184.8	1.393-02	4.384-05	588.2	.7882	1.259+02	1.842-03
	118	7.0954	4339.0	-180.4	1.346-02	4.384-05	585.3	.7882	1.079+02	1.797-03
	119	7.1817	4339.0	-177.4	1.290-02	4.384-05	582.5	.7882	1.000+02	1.763-03
	120	7.2679	4339.0	-174.4	1.234-02	4.383-05	579.7	.7882	1.000+02	1.727-03
	121	7.3542	4339.0	-171.4	1.219-02	4.383-05	571.3	.7882	1.000+02	1.727-03
	122	7.4405	4339.0	-166.9	1.168-02	4.383-05	562.9	.7882	1.000+02	1.727-03
	123	7.5268	4339.0	-162.3	1.120-02	4.382-05	558.7	.7882	1.000+02	1.727-03
	124	7.6130	4339.0	-157.0	1.073-02	4.382-05	551.9	.7882	1.000+02	1.727-03
	125	7.6993	4339.0	-153.5	1.028-02	4.382-05	546.5	.7882	1.000+02	1.727-03
	126	7.7856	4339.0	-148.7	9.844-03	4.382-05	541.1	.7882	1.000+02	1.727-03
	127	7.8719	4339.0	-144.2	9.443-03	4.382-05	535.6	.7882	1.000+02	1.727-03
	128	7.9581	4339.0	-141.1	9.176-03	4.382-05	531.9	.7882	1.000+02	1.727-03
	129	8.0444	4339.0	-138.1	8.916-03	4.381-05	527.2	.7882	1.000+02	1.727-03
	130	8.1307	4339.0	-135.0	8.664-03	4.381-05	523.0	.7882	1.000+02	1.727-03
	131	8.2170	4339.0	-132.0	8.419-03	4.381-05	518.4	.7882	1.000+02	1.727-03
	132	8.3032	4339.0	-128.9	8.181-03	4.381-05	513.1	.7882	1.000+02	1.727-03
	133	8.3895	4339.0	-125.9	7.949-03	4.381-05	508.4	.7882	1.000+02	1.727-03
	134	8.4758	4339.0	-122.0	7.724-03	4.381-05	503.7	.7882	1.000+02	1.727-03
	135	8.5621	4339.0	-119.0	7.505-03	4.380-05	500.0	.7882	1.000+02	1.727-03
	136	8.6483	4339.0	-116.7	7.292-03	4.380-05	500.0	.7882	1.000+02	1.727-03

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

VISCOS FLOW - BOUNDARY LAYER SOLUTION

BODY PT NO	INTG PT NO	STREAM LENGTH INCH	MOMENTUM THICKNESS MIL	ENERGY THICKNESS MIL	SHAPE FACTOR	FORM THICK RE NO	ENERGY THICK RE NO	HEAT TRANS COEFFICIENT LBM/FT ² -SEC	REYNOLDS ANAL FAC	INTER- MITTENCY	HEAT TRANS AUGMENT
(J)	(I)	(S)	(TME)	(PHI)	(NSF)	(RETH)	(REPM)	(RUCH)	(RAF)	(ADML)	(HUFERT)
1	1	.000	.261	.638	1.654	0.000	0.000	7.348-01	.9777	.00	1.808
	2	.041	.261	.639	1.654	1.223-01	2.782-01	7.341-01	.9774	.00	1.808
	3	.091	.261	.640	1.654	2.448-01	5.576-01	7.322-01	.9765	.00	1.808
	4	.142	.310	.852	1.655	9.004-01	1.100-02	6.453-01	.7060	.00	1.808
	5	.192	.317	1.101	1.332	8.882-01	1.891-02	1.353-00	.8574	1.00	1.546
	6	.243	.691	1.387	1.173	1.479-02	2.949-02	1.330-00	.9291	1.00	1.542
2	7	.284	.788	1.591	1.095	2.020-02	4.078-02	1.354-00	.9736	1.00	1.559
	8	.329	1.142	1.876	1.038	2.630-02	5.083-02	1.241-00	1.0377	1.00	1.518
3	9	.401	1.271	2.130	1.003	3.163-02	6.806-02	1.209-00	1.0424	1.00	1.507
	10	.457	1.367	2.369	.979	3.653-02	7.886-02	1.198-00	1.0349	1.00	1.504
4	11	.503	1.448	2.603	.944	4.138-02	9.010-02	1.213-00	1.0174	1.00	1.511
	12	.563	1.491	2.803	.933	4.605-02	1.001-03	1.258-00	1.0014	1.00	1.518
5	13	.587	1.533	3.073	.924	5.069-02	1.184-03	1.288-00	.9868	1.00	1.529
	14	.627	1.554	3.171	.917	5.340-02	1.297-03	1.319-00	.9728	1.00	1.539
6	15	.682	1.588	3.308	.910	5.606-02	1.399-03	1.336-00	.9605	1.00	1.558
	16	.727	1.684	3.429	.894	6.006-02	1.567-03	1.321-00	.9649	1.00	1.556
7	17	.758	1.757	3.764	.891	6.355-02	1.800-03	1.337-00	.9795	1.00	1.549
	18	.802	1.795	3.844	.882	7.110-02	1.957-03	1.386-00	.9444	1.00	1.551
8	19	.850	1.825	4.060	.872	7.439-02	2.158-03	1.403-00	.9475	1.00	1.566
	20	.883	1.898	4.193	.862	8.290-02	2.431-03	1.399-00	.9613	1.00	1.573
9	21	.905	1.957	4.306	.859	9.058-02	2.811-03	1.404-00	.9628	1.00	1.567
	22	.963	2.009	4.419	.869	9.684-02	3.229-03	1.410-00	.9634	1.00	1.567
10	23	1.012	2.021	4.539	.865	1.008-03	3.625-03	1.423-00	.9585	1.00	1.569
	24	1.042	2.044	4.704	.861	1.089-03	4.035-03	1.479-00	.9420	1.00	1.583
11	25	1.071	2.147	4.917	.855	1.168-03	4.461-03	1.517-00	.9419	1.00	1.592
	26	1.126	2.242	5.129	.850	1.221-03	4.851-03	1.523-00	.9505	1.00	1.590
12	27	1.150	2.258	5.272	.848	1.276-03	5.298-03	1.544-00	.9452	1.00	1.592
	28	1.243	2.276	5.421	.845	1.334-03	5.831-03	1.590-00	.9344	1.00	1.602
13	29	1.279	2.301	5.570	.843	1.396-03	6.461-03	1.629-00	.9344	1.00	1.602
	30	1.316	2.332	5.722	.841	1.459-03	7.103-03	1.666-00	.9292	1.00	1.610
14	31	1.348	2.364	5.871	.839	1.526-03	7.850-03	1.701-00	.9253	1.00	1.617
	32	1.479	2.401	6.023	.837	1.595-03	8.610-03	1.735-00	.9220	1.00	1.623
15	33	1.506	2.440	6.174	.836	1.661-03	9.480-03	1.768-00	.9192	1.00	1.629
	34	1.552	2.475	6.330	.835	1.702-03	1.035-03	1.798-00	.9159	1.00	1.638
16	35	1.603	2.455	6.453	.835	1.753-03	1.141-03	1.832-00	.9099	1.00	1.644
	36	1.657	2.450	6.544	.835	1.803-03	1.255-03	1.884-00	.9086	1.00	1.644
17	37	1.709	2.505	6.702	.834	1.852-03	1.373-03	1.925-00	.9000	1.00	1.661
	38	1.761	2.559	6.863	.833	1.901-03	1.493-03	1.943-00	.9042	1.00	1.662
18	39	1.812	2.564	6.962	.833	1.956-03	1.616-03	1.969-00	.9011	1.00	1.664
	40	1.864	2.572	7.108	.834	2.022-03	1.741-03	2.009-00	.8951	1.00	1.671
19	41	1.918	2.584	7.251	.835	2.078-03	1.866-03	2.044-00	.8929	1.00	1.676
	42	1.964	2.603	7.360	.835	2.139-03	2.000-03	2.075-00	.8901	1.00	1.681
20	43						2.104-00	2.104-00	.8888	1.00	1.684

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MLIT)

BODY PT NO	INTEL PT NO	STREAM LENGTH INCH	MOMENTUM THICKNESS MIL	ENERGY THICKNESS MIL	SHAPE FACTOR	MON THICK RE NO	ENERGY THICK RE NO	HEAT TRANS COEFFICIENT LB/FT ² -SEC	REYNOLDS ANAL FAC	INTER- MITTENCY	HEAT TRANS AUGMENT
(J)	(I)	(SI)	(THE)	(PHI)	(MSF)	(RETH)	(REPH)	(KUCH)	(RAF)	(ADML)	(HJFSMT)
21	45	2.0173	2.629	7.995	.836	2.203+03	6.282+03	2.128+00	.8880	1.00	1.687
21	46	2.0882	2.653	7.635	.837	2.266+03	6.520+03	2.154+00	.8842	1.00	1.690
22	47	2.1190	2.643	7.748	.839	2.305+03	6.758+03	2.189+00	.8703	1.00	1.696
22	48	2.1697	2.644	7.869	.841	2.352+03	7.001+03	2.214+00	.8783	1.00	1.700
23	49	2.2202	2.688	8.021	.842	2.425+03	7.235+03	2.223+00	.8816	1.00	1.699
23	50	2.2706	2.734	8.176	.843	2.499+03	7.472+03	2.236+00	.8802	1.00	1.700
24	51	2.3376	2.751	8.356	.846	2.560+03	7.777+03	2.258+00	.8757	1.00	1.702
24	52	2.4046	2.774	8.547	.850	2.625+03	8.087+03	2.272+00	.8741	1.00	1.704
25	53	2.4716	2.809	8.748	.853	2.697+03	8.401+03	2.283+00	.8734	1.00	1.705
25	54	2.5217	2.840	8.905	.856	2.749+03	8.621+03	2.283+00	.8732	1.00	1.704
25	55	2.5718	2.873	9.067	.858	2.802+03	8.843+03	2.282+00	.8732	1.00	1.703
26	56	2.6219	2.911	9.235	.861	2.854+03	9.055+03	2.276+00	.8734	1.00	1.701
26	57	2.6719	2.937	9.408	.864	2.894+03	9.268+03	2.275+00	.8673	1.00	1.701
27	58	2.7219	2.904	9.590	.871	2.871+03	9.480+03	2.270+00	.8572	1.00	1.703
27	59	2.7719	2.897	9.779	.878	2.873+03	9.699+03	2.270+00	.8638	1.00	1.701
28	60	2.8219	3.019	9.956	.879	2.994+03	9.877+03	2.245+00	.8810	1.00	1.681
28	61	2.8719	3.141	10.133	.879	3.117+03	1.005+04	2.203+00	.8735	1.00	1.686
29	62	2.9219	3.178	10.332	.885	3.148+03	1.024+04	2.203+00	.8723	1.00	1.681
29	63	2.9720	3.203	10.538	.891	3.165+03	1.042+04	2.161+00	.8714	1.00	1.677
30	64	3.0221	3.233	10.756	.897	3.181+03	1.058+04	2.131+00	.8708	1.00	1.673
30	65	3.0722	3.267	10.980	.903	3.198+03	1.075+04	2.100+00	.8705	1.00	1.668
31	66	3.1214	3.307	11.214	.909	3.213+03	1.090+04	2.065+00	.8702	1.00	1.662
31	67	3.1725	3.349	11.455	.915	3.228+03	1.104+04	2.028+00	.8702	1.00	1.656
32	68	3.2229	3.396	11.710	.922	3.240+03	1.117+04	1.988+00	.8703	1.00	1.650
32	69	3.2732	3.445	11.971	.923	3.253+03	1.132+04	1.947+00	.8706	1.00	1.643
33	70	3.3237	3.499	12.244	.935	3.261+03	1.141+04	1.903+00	.8709	1.00	1.636
33	71	3.3741	3.553	12.523	.942	3.269+03	1.152+04	1.859+00	.8712	1.00	1.629
34	72	3.4249	3.611	12.813	.949	3.272+03	1.161+04	1.812+00	.8768	1.00	1.620
34	73	3.4756	3.670	13.109	.956	3.273+03	1.169+04	1.762+00	.8860	1.00	1.606
35	74	3.5265	3.801	13.554	.962	3.299+03	1.176+04	1.687+00	.8767	1.00	1.596
35	75	3.5774	3.930	14.010	.969	3.318+03	1.183+04	1.629+00	.8658	1.00	1.584
36	76	3.6285	3.916	14.215	.976	3.327+03	1.188+04	1.606+00	.8679	1.00	1.589
36	77	3.6793	3.914	14.422	.985	3.338+03	1.193+04	1.573+00	.8632	1.00	1.579
37	78	3.7311	3.983	14.765	.995	3.350+03	1.198+04	1.520+00	.8726	1.00	1.570
37	79	3.7826	4.046	15.118	1.004	3.357+03	1.201+04	1.472+00	.8708	1.00	1.555
38	80	3.8317	4.147	15.736	1.020	3.379+03	1.206+04	1.393+00	.8701	1.00	1.540
38	81	3.8807	4.244	16.385	1.035	3.405+03	1.210+04	1.318+00	.8733	1.00	1.524
38	82	3.9298	4.355	17.066	1.049	3.437+03	1.213+04	1.244+00	.8805	1.00	1.507
39	83	4.0760	4.511	17.720	1.062	3.491+03	1.214+04	1.176+00	.8837	1.00	1.491
39	84	4.1622	4.681	18.401	1.074	3.509+03	1.214+04	1.113+00	.8869	1.00	1.475
39	85	4.2484	4.851	19.112	1.086	3.561+03	1.214+04	1.053+00	.8900	1.00	1.458
40	86	4.3347	5.036	19.909	1.098	3.667+03	1.212+04	9.917+01	.8925	1.00	1.441
40	87	4.4211	5.217	20.729	1.111	3.748+03	1.211+04	9.339+01	.8970	1.00	1.424
40	88	4.5074	5.399	21.571	1.127	3.831+03	1.211+04	8.766+01	.9021	1.00	1.409
40	89	4.5936	5.581	22.342	1.141	3.924+03	1.211+04	8.320+01	.9052	1.00	1.394
41	90	4.6798	5.768	23.142	1.155	3.915+03	1.210+04	7.863+01	.9084	1.00	1.379
41	91	4.7660	5.955	23.974	1.166	3.902+03	1.209+04	7.467+01		1.00	

MOMENTUM ENERGY INTEGRATION TECHNIQUE (MEIT)

BODY PT NO	INTS PT NO	STREAM LENGTH INCH	MOMENTUM THICKNESS MIL	ENERGY THICKNESS MIL	SHAPE FACTOR	MOV THICK RE NO	ENERGY THICK RE NO	HEAT TRANS COEFFICIENT LBH/FI2-SEC	REYNOLDS ANAL FAC	INTER- MITTENCY	HEAT TRANS AUGMENT
(J)	(I)	(S)	(THE)	(PHI)	(HSE)	(RETH)	(REPH)	(MUCH)	(RAF)	(ADML)	(RUFST)
92	92	9.828	6.153	24.005	1.182	2.985+03	1.207+04	7.053-01	.9116	1.00	1.363
93	93	9.935	6.351	25.832	1.195	2.963+03	1.203+04	6.660-01	.9144	1.00	1.348
94	94	9.024	6.557	26.820	1.208	2.940+03	1.203+04	6.282-01	.9194	1.00	1.332
95	95	9.111	6.745	27.630	1.219	2.926+03	1.199+04	5.982-01	.9250	1.00	1.318
96	96	9.197	6.945	28.450	1.228	2.911+03	1.194+04	5.700-01	.9264	1.00	1.305
97	97	9.283	7.139	29.352	1.238	2.894+03	1.190+04	5.428-01	.9319	1.00	1.292
98	98	9.369	7.338	30.263	1.249	2.876+03	1.186+04	5.164-01	.9355	1.00	1.278
99	99	9.452	7.536	31.193	1.262	2.857+03	1.183+04	4.912-01	.9387	1.00	1.265
100	100	9.542	7.732	32.168	1.275	2.839+03	1.180+04	4.671-01	.9421	1.00	1.252
101	101	9.628	7.938	33.212	1.288	2.813+03	1.179+04	4.433-01	.9453	1.00	1.238
102	102	9.719	8.144	34.416	1.302	2.788+03	1.178+04	4.206-01	.9485	1.00	1.224
103	103	9.801	8.358	35.601	1.315	2.764+03	1.177+04	3.985-01	.9545	1.00	1.210
104	104	9.887	8.532	36.460	1.325	2.748+03	1.174+04	3.823-01	.9608	1.00	1.198
105	105	9.973	8.714	37.533	1.335	2.732+03	1.171+04	3.672-01	.9644	1.00	1.187
106	106	10.061	8.895	38.250	1.343	2.715+03	1.167+04	3.528-01	.9681	1.00	1.177
107	107	10.144	9.080	39.200	1.355	2.697+03	1.164+04	3.384-01	.9719	1.00	1.166
108	108	10.237	9.264	40.170	1.365	2.678+03	1.161+04	3.247-01	.9756	1.00	1.155
109	109	10.319	9.439	41.166	1.376	2.656+03	1.158+04	3.118-01	.9763	1.00	1.144
110	110	10.402	9.681	42.703	1.390	2.625+03	1.158+04	2.948-01	.9781	1.00	1.130
111	111	10.493	9.915	43.948	1.405	2.591+03	1.157+04	2.784-01	.9820	1.00	1.115
112	112	10.578	10.158	45.948	1.419	2.559+03	1.157+04	2.624-01	.9893	1.00	1.099
113	113	10.660	10.346	47.164	1.430	2.533+03	1.153+04	2.508-01	.9966	1.00	1.087
114	114	10.750	10.545	48.417	1.441	2.509+03	1.152+04	2.400-01	1.0009	1.00	1.075
115	115	10.836	10.743	49.703	1.452	2.484+03	1.149+04	2.296-01	1.0053	1.00	1.063
116	116	10.929	10.944	51.050	1.464	2.460+03	1.147+04	2.193-01	1.0103	1.00	1.051
117	117	11.021	11.143	52.401	1.476	2.435+03	1.145+04	2.098-01	1.0151	1.00	1.048
118	118	11.134	11.351	53.803	1.488	2.411+03	1.143+04	2.003-01	1.0244	1.00	1.027
119	119	11.247	11.584	54.607	1.497	2.393+03	1.138+04	1.935-01	1.0331	1.00	1.018
120	120	11.362	11.828	55.450	1.505	2.377+03	1.133+04	1.881-01	1.0376	1.00	1.009
121	121	11.482	12.044	56.270	1.513	2.359+03	1.129+04	1.827-01	1.0379	1.00	1.002
122	122	11.605	12.268	57.445	1.525	2.335+03	1.127+04	1.763-01	1.0335	1.00	1.000
123	123	11.732	12.504	59.472	1.537	2.309+03	1.123+04	1.703-01	1.0306	1.00	1.000
124	124	11.861	12.746	61.152	1.549	2.283+03	1.124+04	1.645-01	1.0240	1.00	1.000
125	125	11.993	12.997	62.913	1.562	2.258+03	1.122+04	1.588-01	1.0253	1.00	1.000
126	126	12.128	13.256	64.734	1.574	2.232+03	1.120+04	1.533-01	1.0224	1.00	1.000
127	127	12.267	13.509	66.615	1.585	2.209+03	1.119+04	1.479-01	1.0234	1.00	1.000
128	128	12.409	13.782	68.663	1.593	2.191+03	1.115+04	1.443-01	1.0261	1.00	1.000
129	129	12.554	14.064	70.080	1.601	2.174+03	1.111+04	1.410-01	1.0249	1.00	1.000
130	130	12.702	14.352	71.175	1.609	2.158+03	1.107+04	1.378-01	1.0238	1.00	1.000
131	131	12.852	14.644	72.366	1.619	2.143+03	1.103+04	1.346-01	1.0228	1.00	1.000
132	132	13.004	14.944	73.589	1.628	2.128+03	1.100+04	1.315-01	1.0219	1.00	1.000
133	133	13.158	15.253	74.848	1.637	2.114+03	1.097+04	1.284-01	1.0203	1.00	1.000
134	134	13.317	15.573	76.133	1.647	2.099+03	1.093+04	1.254-01	1.0191	1.00	1.000
135	135	13.481	15.893	77.446	1.656	2.084+03	1.090+04	1.225-01	1.0177	1.00	1.000
136	136	13.643	16.210		1.666	2.070+03	1.087+04	1.196-01	1.0163	1.00	1.000

Section 6. Program Listing

A listing of the Fortran source deck is given in this section. The common block and block data are presented first, the driver routine which is the main program is given next, followed by all the subroutines in the program.

COMBLK

```

PE 1
2
3
4
5
6
7
8
9
10
11
12
13
14
15
16
17
18
19
20
21
22
23
24
25
26
27
28
29
30
31
32
33
34
35
36
37
38
39
40
41
42
43
44
45
46
47
48
49
50
51
52
53
54
55

      COMMON /CONST/
      * ALMAX, ALMIN, DEXMIN, DLTRIN, DLTRAN, USHANG, HJUNCTN, HZEROT, IATH,
      * IBRUPT, ICARB, IFL609, IHMAX, IL, IFMAX, IPRFL6, IPRNT, IRON,
      * IRSTRY, ISHFLG, ISS, JL, LG, LL, MATN, NAM, NCL,
      * NOMEAL, NOSLO, NPRTBL, NREYCR, NSHTBL, NTFIX, NTINT, NTRUSR, OX,
      * OY, PR, RNI, RSIDE, SPHTC, STRD, THETA, TRNTIM, ZHAX,
      * ZSIDE1, ZSTAG1,
      * AGLAW(3), ALCL(50), ALT(60), AM(60), BGLAW(3), BLN(3),
      * BLS(3), BTH(3), BTS(3), CGRAW(3), CHOSTT(60), CMH(3),
      * CZI(50), DEL(19), DGLAW(3), DM1(50,25), DPI(50), EGLAW(3),
      * ENT(35,21), ET(35,21), FE(35,21), FLPT(21), FLTT(35,21),
      * GT(35,21), HFO(3), HT(35), JROUGH(3), KHI(5,5,3),
      * MERODE(3), NLO(5,5,3), NMAT(50,25), NMG(3), NPR(3),
      * PA(60), PAM(60), PSTT(60), PT(21), RECORD(36), REM(30),
      * RHO(3), RUFL(3), RUFMAX(3), RUF1(3), SGI(50), TA(60),
      * TBFP(1950), TCHEM(1950), YCP(30,3), TENT(35,21), TEP(30,3), TFO(3),
      * THZ(60,3), TIMT(60), TIMUSR(250), TKP(60,3), TLMC(1950), TNG(5,3),
      * TPR(5,3), TPESTR(60), TTP(60,3), TTS(1950), VEL(60), X(50),
      * XDIF(60), XINIT(50), XPHTBL(60), Y(25), YOIF(5), YINIT(50)

      COMMON /ENVR/
      * ALTINF, AMACH, A1, A2, CDRA6, DEN, DUOZ, EMW2, EMW2,
      * E2, GAM1, GAM2, METAUG, HT2, H1, H2, INOSE,
      * KSHOLD, LCT, LTT, NOSTRN, NPGENV, NT, NTS, PT2,
      * P1, P2, REYCR, RN, ROT2, RO1, RO2, SC, IC, STRAN,
      * TSTAGP, TT2, T1, T2, UR1, VIST2, VIS2, V1, V2,
      * ADML(150), ALTEND(250), BETA(150), BETP(150), BP(150), DRGED(250),
      * CSEE(150), DROS(150), ENTR(150), HCAR(150), HE(150), HR(150),
      * HSF(150), HW(150), IPT(150), MATL(150), PE(150), PEPI(150),
      * PHI(150), R(150), RAF(150), REPH(150), RETH(150), ROE(150),
      * ROUE(150), ROW(150), RUCH(150), RUF(150), RUFST(150), S(150),
      * SOR(150), SRB(150), TE(150), THE(150), THETB(150), TIMEND(250),
      * TP(150), TUE(150), TW(150), UE(150), URE(150), VISE(150),
      * VISW(150), XSHC(150), YBAR(150), YSHC(150), Z(150), ZSIDED(250),
      * ZSPEND(250)

      COMMON /RECS/
      * CZ, OPART1, OTH, IUSER, MT, MTNU, NPG, NS, S6,
      * TIMENU, TIMEP, TS, VR,
      * BLEN(60,2), BPSP(60), CMGX(60), CMFX(60), DELKE(60), DFIF(60),
      * OPART(60), EFFK(60), EMOOT(60), FI(60), FVM(60), GKR(60),
      * HRSP(60), INI(38), ILO(38), IMAT(60,18), IR(38), NB(60,3),
      * PRES(60), RI(60,2), RSP(60), RSPNU(60), RUCHSP(60), SDOT(60),
      * SDOTE(60), SP(60), SRAY(60), TANFI(60), THETSP(60), TSP(60),
      * VIMP(60), ZI(60,2), ZSP(60), ZSPNU(60)

      COMMON /COND/
      * ANGLE, DLTC, DLT, DLTS, FIKLM, KEND, KL, KLF, KMAX,
      * KSTART, NOUT, QOOTRM, QOOTMO, STRM, TERMA, TERMB, TERMC,
      * DELTAA(60), DOR(60), NREG(80,25), QW(60), T(50,25), TIW1(60),
      * TT(60,18), X8(60,15), Y8(60,15)

      END
      COMMON /PROC
      COMMON /UNITS /
      * ATM, BTU, BTUCAL, CMFT, DEGFR, DEGRK, DENH2O, EINRIC, ELBFT3,
      * EMETER, ERICR, ENHFT, FT, FTHIL, FT2, GC, P1, P102,
      * RAD, RU, SIG, STOTEN

```

86

00111	110	C	•	FT-LBF/BTU
00111	120	C	•	•
00111	130	C	•	MIL/FT
00111	140	C	•	ENEYER / 3.280039
00111	150	C	•	FT/METER
00111	160	C	•	STOYER / 930.
00111	170	C	•	STANDARD TEMPERATURE
00111	180	C	•	CEGFR / 459.7
00111	190	C	•	DEG R = DEG F + DEGFR
00111	200	C	•	RU / .73043
00111	210	C	•	UNIVERSAL GAS CONSTANT,
00111	220	C	•	(LBM/HOLE)/(LBM/FT ³)-(DEG R)
00111	230	C	•	816 / 4.75502E-13
00111	240	C	•	STEFAN-BOLTZMANN CONSTANT,
00111	250	C	•	BTU/FT ² -DEG R ⁴ -SEC
00130	260	C	•	DATA ELDFTS / 62.4280E-6
00130	270	C	•	(LBM/FT ³)/(IN ³ /H ³)
00130	280	C	•	BTUCAL / 251.996
00130	290	C	•	CAL/BTU
00130	300	C	•	DEH20 / 62.4280
00130	310	C	•	DENSITY OF WATER
00130	320	C	•	DEGRK / 1.8
00130	330	C	•	DEG R/DEG K
00130	340	C	•	ENHFT / 3.280039E-3
00130	350	C	•	FT/MM
00130	360	C	•	EMICMM / .001
00130	370	C	•	MM/MICRON
00130	380	C	•	EINPIC / 39.3701E-6
00130	390	C	•	INCH/MICRON
00130	400	C	•	CMFT / .03280839
00130	410	C	•	FT/CM
00141	420	C	•	END

```

00101 10
00107 20
00110 30
00111 40
00112 50
00113 60
00114 70
00119 80
00124 90
00125 95
00127 100
00131 110
00132 120
00137 130
00137 140
00140 150
00144 160
00144 170
00145 180
00147 190
00152 200
00161 210
00161 220
00174 230
00176 240
00201 250
00202 260
00203 270
00205 280
00206 290
00207 300
00210 310
00213 320
00215 330
00217 340
00221 350
00224 360
00226 370
00227 380
00241 390
00242 400
00250 410
00254 420
00258 430
00263 440
00264 450
00265 460
00267 470
00271 480
00271 490
00273 500
00276 510
00277 520
00282 530
00303 540
00305 550
00307 560
00307 570

```

DRIVEN

```

INCLUDE COMON
COMMON/RUFF/ROUGH,RUF2(150)
COMMON/TABLE/LTB
DIMENSION STOR(35,21)
CZ=0.
OPART1=0.
READ(5,99) NSM,ROUGH,CMH(1),GAM2,S(1),RM
FORMAT(211,F8.3,F10.5)
IF(CMH(1)-LT-.00001) CMH(1)=1.
IF(GAM2-LT-.00001) GAM2=1.2
CALL LCOUNT(-94)
WRITE(6,101) NSM,CMH(1),GAM2
FORMAT(///,T10,22NUMBER OF MATERIALS = ,I3,T10,8MCM/CM = ,F10.5,
* /T10,22MISCENTROPIC EXPONENT = ,F10.5)
IF(ABS(RM)-GT-.00001) WRITE(6,101)RM
FORMAT(110,76THE INITIAL SOLUTION IS THE STAGNATION SOLUTION OF A
* SPHERE WITH A RADIUS OF ,F8.3,6INCHES)
IF(ABS(RM)-LT-.00001) RM=1.0
DO 102 I=1,NSM
IF(ROUGH.EQ.1) READ(5,170) B7S(I),B7H(I),BLS(I),BLH(I)
IF(ROUGH.EQ.0) READ(5,103) B7S(I),B7H(I),BLS(I),BLH(I),RUF1(I),
* RUF2(I),RUF1(I)
IF(ROUGH.EQ.1) GO TO 600
DO 601 I=1,NSM
RUF1(I)=RUF1(I)/12000.
RUF2(I)=RUF2(I)/12000.
RUF1(I)=RUF1(I)/12000.
CONTINUE
FORMAT(4F10.5)
FORMAT(7F10.5)
DO 104 I=1,NSM
IF(ABS(B7S(I))-LT-.00001) B7S(I)=0.35
IF(ABS(B7H(I))-LT-.00001) B7H(I)=.35
IF(ABS(BLS(I))-LT-.00001) BLS(I)=0.5
IF(ABS(BLH(I))-LT-.00001) BLH(I)=0.5
WRITE(6,106)
FORMAT(///,T10,4WHATL,727,3B7S,744,3B7H,759,3BLS,775,3BLH/)
WRITE(6,105) (I,B7S(I),B7H(I),BLS(I),BLH(I),I=1,NSM)
FORMAT(111,12,728,F10.5,T59,F10.5,T59,F10.5,T71,F10.5)
READ(5,120) NS,IBRUPT,NREYCR,IPANT,DLTRAN,ICARD,JROUGH(1)
FORMAT(412,F10.5,212)
WRITE(6,50) NS,IBRUPT,NREYCR,IPANT,DLTRAN
FORMAT(///,T10,5NHS = ,I2/T10,9HIBRUPT = ,I2/T10,9HNREYCR = ,I2/
* T10,9HIPRANT = ,I2/T10,9HOLTRAN = ,F10.5,8H INCHES/)
DLTRAN=DLTRAN/12.
IF(ABS(JROUGH(1))-NE.1) GO TO 131
WRITE(6,1130)
FORMAT(///,T10,93HTRANSITION PROXIMITY AUGMENTATION TO LAMINAR HEATI
* NG )
CONTINUE
IF(IBRUPT.EQ.0) WRITE(6,1120)
FORMAT(///,T10,20HTRANSITIONAL HEATING)
IF(IBRUPT.EQ.1) WRITE(6,2120)
FORMAT(///,T10,17HABRUPT TRANSITION)
IF(ABS(NREYCR).EQ.0) NREYCR=7
IF(ABS(NREYCR).EQ.2) GO TO 122
IF(ABS(NREYCR).EQ.3) GO TO 122

```

```

000001
000001
000001
000001
000002
000003
000022
000022
000030
000036
000041
000041
000051
000051
000051
000071
000071
000071
000102
000102
000114
000114
000134
000142
000142
000144
000144
000154
000154
000154
000154
000161
000166
000174
000202
000212
000217
000217
000237
000237
000253
000253
000265
000265
000265
000270
000275
000301
000301
000301
000307
000307
000317
000317
000324
000327

```

```

000312 11*(NREYCR.EQ.1) WRITE(6,104)
000313 FORMAT(//T10.17NFLOW IS LAMINAR)
000314 IF(NREYCR.EQ.1) WRITE(6,151) DLYNAM
000315 FORMAT(//T10.20TRANSITION OCCURS AT F10.7 INCHES)
000316 IF(NREYCR.EQ.5) WRITE(6,121)
000317 FORMAT(//T10.50TRANSITION DETERMINED BY ANDERSON NOSE CRITERION(N
000318 NREYCR=5))
000319 IF(NREYCR.EQ.6) WRITE(6,132) ICARB
000320 FORMAT(//T10.60TRANSITION DETERMINED BY ANDERSON NOSE CRITERION (
000321 NREYCR=6),ICARB=12.1M)
000322 IF(NREYCR.EQ.7) WRITE(6,1152)
000323 FORMAT(//T10.17NFLOW IS TURBULENT)
000324 GO TO 145
000325 READ(15,120) N2M
000326 READ(15,2) (REM(I),I=1,N2M)
000327 READ(15,2) (AM(I),I=1,N2M)
000328 IF(IABS(NREYCR).EQ.2) GO TO 127
000329 WRITE(6,128)
000330 FORMAT(//T10.49TRANSITION DETERMINED BY CRITICAL MOMENTUM THICKN.
000331 S=0.4*WESS REYNOLDS NO. VS. EDGE MACH NO.,
000332 /T24.22CRITICAL STREAM LENGTH,T64.11MACH NUMBER./T29.
000333 0.15MREYNOLDS NUMBER./)
000334 FORMAT(//T10.47TRANSITION DETERMINED BY CRITICAL STREAM LENGTH,
000335 S=0.8MREYNOLDS NO. VS. EDGE MACH NO.,
000336 /T24.22CRITICAL STREAM LENGTH,T64.11MACH NUMBER./T29.
000337 0.15MREYNOLDS NUMBER./)
000338 GO TO 150
000339 WRITE(6,129)
000340 WRITE(6,134) (REM(I),I=1,N2M)
000341 FORMAT(//T32.610.6.T68.E10.6)
000342 CONTINUE
000343 READ(15,5) (IMAT(I),I=1,NS)
000344 FORMAT(//110)
000345 READ(15,2) (ZSPI(I),I=1,NS)
000346 READ(15,2) (RSP(I),I=1,NS)
000347 READ(15,2) (PE(I),I=1,NS)
000348 READ(15,2) (ME(I),I=1,NS)
000349 READ(15,2) (UE(I),I=1,NS)
000350 READ(15,2) (TSP(I),I=1,NS)
000351 READ(15,2) (BSP(I),I=1,NS)
000352 IF(1/ROUGH.EQ.1) READ(5,2) (RUF2(I),I=1,NS)
000353 IF(1/ROUGH.EQ.0) GO TO 801
000354 DO 802 I=1,NS
000355 RUF2(I)=RUF2(I)/12000.
000356 CONTINUE
000357 IF(IPRINT.NE.9) GO TO 1101
000358 CALL LCOUNT(-8)
000359 IF(1/ROUGH.EQ.1) WRITE(6,245)
000360 IF(1/ROUGH.EQ.0) WRITE(6,109)
000361 FORMAT(//T5. 8MATERIAL,T20.5AXIAL,T33.6RADIAL, T49.4WEDGE.
000362 0.165.4WEDGE.
000363 0.179.4WEDGE,T99.4WALL,T109.10NORMALLIZED/T6 .6MNUMBER,T19.
000364 0.6LENGTH,T55.6LENGTH,T47.8MPRESSURE,T63.8ENTHALPY,T77.8VELOCITY
000365 0.172.11TEMPERATURE,T108.13ABSLATION RATE/T20.4WINDCH,T34.4WINDCH,
000366 0.149.3WATM,T63.7WBTU/LBM,T78.6GHFT/SEC,T94.5HDEG R/T6.6H(IMAT).T20.
000367 0.5H(ZSPI).T34.5H(RSP). T49.4H(PE).T64.4H(ME).T79.4H(UE).T94.
000368 0.5H(TSPI).T111.6H(BSP)/)

```

90


```

00163 630
00164 640
00165 650
00166 660
00171 670
00173 680
00175 690
00176 700
00177 710
00200 720
00200 730
00200 740
00200 750
00201 760
00202 770
00205 780
00207 790
00211 800
00212 810
00213 820
00213 830
00213 840
00213 850
00214 860
00215 870
00216 880
00217 890
00217 900
00217 910
00217 920
00220 930
00221 940
00222 950
00223 960
00224 970
00225 980
00227 990
00231 1000
00232 1010
00234 1020
00233 1030
00233 1040
00233 1050
00235 1060
00235 1070
00237 1080
00230 1090
00231 1100
00242 1110
00233 1120
00234 1130
00234 1140
00234 1150
00234 1160
00244 1170
00235 1180
00246 1190

000121
000124
000126
000161
000161
000170
000170
000173
000175
000217
000217
000217
000217
000233
000233
000237
000245
000245
000250
000252
000252
000252
000252
000263
000263
000303
000320
000320
000320
000334
000355
000370
000403
000414
000415
000417
000425
000427
000439
000446
000446
000446
000446
000450
000450
000460
000501
000514
000527
000532
000532
000532
000532
000532
000532
000554

      IT = IMAX
      320 IT1 = IT-1
      ML = FLINE(TEMP,TENT(IT1,IP1),TENT(IT,IP1),MT(IT1),MT(IT))
      DO 330 IT=ISTRT,IMMAX
      IF (TENT(IT,IP1),GT,TEMP) GO TO 340
      330 CONTINUE
      340 IT1 = IT-1
      IM = IMAX
      MU = FLINE(TEMP,TENT(IT1,IP1),TENT(IT,IP1),MT(IT1),MT(IT))
      M = FLINE(FLP,FLPT(IP1),FLPT(IP),ML,MU)
      C *** START OF ITERATION LOOP ON ENTHALPY
      C
      100 CONTINUE
      120 DO 130 IM=ISTRT,IMMAX
      IF (MT(IM),GT,M) GO TO 140
      130 CONTINUE
      IM = IMAX
      140 IM1 = IM-1
      GO TO (150,150,180), INDU
      C
      C LOOK UP VISCOSITY FROM ENTHALPY AND PRESSURE
      C
      150 CONTINUE
      160 EL = FLINE(IM,MT(IM1),MT(IM),ET(IM,IP1),ET(IM,IP1))
      EU = FLINE(IM,MT(IM1),MT(IM),ET(IM,IP),ET(IM,IP))
      170 E = FLINE(FLP,FLPT(IP1),FLPT(IP),EL,EU)
      C
      C LOOK UP TEMPERATURE FROM ENTHALPY AND PRESSURE
      C
      180 TL = FLINE(IM,MT(IM1),MT(IM),TENT(IM1,IP1),TENT(IM,IP1))
      TU = FLINE(IM,MT(IM1),MT(IM),TENT(IM1,IP),TENT(IM,IP))
      TEMP = FLINE(FLP,FLPT(IP1),FLPT(IP),TL,TU)
      GO TO (150,150,420), INDU
      420 YIND = TEMP
      430 IF(YGIVN,EG,0.) GO TO 440
      IF(ABS(YIND-YGIVN)/YGIVN,LT,.00010) GO TO 500
      GO TO 450
      440 IF(ABS(YIND-YGIVN),LT,.00100) GO TO 500
      450 CALL XSOLVEIM,YIND,YGIVN,COUNT,XLO,YLO,XHI,YHI
      GO TO 100
      C
      C *** END OF ITERATION LOOP ON ENTHALPY
      C
      500 CONTINUE
      GO TO (150,200,520), INDU
      520 EL = FLINE(IM,MT(IM1),MT(IM),ET(IM,IP1),ET(IM,IP1))
      EU = FLINE(IM,MT(IM1),MT(IM),ET(IM,IP),ET(IM,IP))
      530 E = FLINE(FLP,FLPT(IP1),FLPT(IP),EL,EU)
      TEMP = YGIVN
      550 CONTINUE
      C
      C LOOK UP MOLECULAR WT. AND GAMMA FROM ENTHALPY AND PRESSURE
      C
      C AND CALCULATE DENSITY AND SPEED OF SOUND
      C
      EML = FLINE(IM,MT(IM1),MT(IM),EMT(IM1,IP1),EMT(IM,IP1))
      EMU = FLINE(IM,MT(IM1),MT(IM),EMT(IM1,IP),EMT(IM,IP))

```

000567
000602
000607
000614
000625
000630
000632
000634
000636
000643
000656
000770

CM = FLIN(FLP,FLPT(IP1),FLPT(IP1),EVL,EMU)
CL = FLIN(M,MT(IM1),MT(IM1),GT(IM1,IP1),GT(IM,IP1))
CU = FLIN(M,MT(IM1),MT(IM1),GT(IM1,IP1),GT(IM,IP1))
G = FLIN(FLP,FLPT(IP1),FLPT(IP1),6L,6U)
IF (L78-NE,1) GO TO 510
YSTORETEMP
TEMPH
H=STORE
CONTINUE
NO = P/(TEMP*RU/EM)
A=SQRT(GAR2*P/NO*5C*ATN*F12)
RETURN
END

510

00297 1200
00298 1210
00299 1220
00300 1230
00301 1240
00302 1250
00303 1260
00304 1270
00305 1280
00306 1290
00307 1300
00308 1310
00309 1320

```

00101 10
00102 20
00103 30
00104 40
00105 50
00106 60
00107 70
00108 80
00109 90
00110 100
00111 110
00112 120
00113 130
00114 140
00115 150
00116 160
00117 170
00120 180
00121 190
00122 200

SUBROUTINE MSHAPE(I,ILT,SHPFAC)
C-----
C
C THIS ROUTINE COMPUTES THE LAMINAR AND TURBULENT SHAPE FACTORS
C-----
C
C
C INCLUDE COMMON
C 80 TO (10,20), ILT
10 CONTINUE
SHPFAC=5.029*TM(I)/TE(I)-0.64
60 TO 30
20 CONTINUE
ALRTH=ALOG(RETH(I))
EN=10.37*ALRTH/(12.79-0.19*ALRTH)
SHPFAC=2.285*(1.+3.2*EXP(-EN))*TM(I)/TE(I)-0.96
30 CONTINUE
RETURN
END

```

```

000010
000010
000014
000016
000016
000023
000031
000045
000045
000062

```

```

00101 10 SUBROUTINE LARAUS(I,RSRL)
00102 20 INCLUDE COMON
00103 30 INCLUDE COMUNT
00104 40 MCOUNT=1
00105 50 IOCBUS=0
00106 60 RSRL=0.
00107 70
00108 80 10 SOTKL=STRAN/THE(I)/RSRL**1.3
00109 90 IF (NREYCR.EQ.0) SOTKL=STRAN/THE(I)/RSRL
00110 100 IF (SOTKL.GT.1000.) 60 TO 20
00111 110 DUMMY=RSRL-7.6/SOTKL**0.366*EXP(5.E-04*SOTKL)
00112 120 IF (ABS(RSRL-RSRL)/RSRL.LT..01) 60 TO 20
00113 130 RSRL=RSRL
00114 140
00115 150 C CALL XSOLVE(RSRL,DUMMY,0.,MCOUNT,XLO,YLO,XHI,YHI)
00116 160 C
00117 170 IF (IOCBUS.EQ.1)
00118 180 WRITE(6,100) MCOUNT,RSRL,RSRL,SOTKL,DUMMY,STRAN,THE(I)
00119 190 100 FORMAT(1H0,2HMCOUNT,RSRL,RSRL,SOTKL,DUMMY,STRAN,THE(I)/IX,2H,1X,
00120 200 2P6E12.5)
00121 210 50 TO 10
00122 220 20 CONTINUE
00123 230 IF (RSRL.LT.1.) RSRL=1.
00124 240 IF (RSRL.GT.5.) RSRL=5.
00125 250 RETURN
00126 260 END
00127
00128
00129
00130
00131
00132
00133
00134
00135
00136
00137
00138
00139
00140
00141
00142
00143
00144
00145
00146
00147
00148
00149
00150
00151
00152
00153
00154
00155
00156
00157

```

00101	10				
00102	20				
00103	30				
00104	40				
00105	50				
00106	60				
00107	70				
00108	80				
00109	90				
00110	100				
00111	110				
00112	120				
00113	130				
00114	140				
00115	150				
00116	160				
00117	170				
00118	180				
00119	190				
00120	200				
00121	210				
00122	220				
00123	230				
00124	240				
00125	250				
00126	260				
00127	270				
00128	280				
00129	290				
00130	300				
00131	310				
00132	320				
00133	330				
00134	340				
00135	350				


```

SUBROUTINE LCOUNT(I)
C-----
C THIS ROUTINES COUNTS, TITLES AND NUMBERS EACH PAGE
C-----
C
C *** INPUT ***
C I = NUMBER OF LINES TO BE WRITTEN IN SUCCEEDING WRITE STATEMENTS
C IN THE CALLING ROUTINE
C NOTES TO START A NEW PAGE USE NEGATIVE I
C
C INCLUDE COMON
C DATA LCTMAX/ 54 /
C
C LCTMAX IS THE MAXIMUM NUMBER OF LINES ON A PAGE
C
C J = I
C IF (J.LT.0) GO TO 10
C
C SUBTRACT J FROM THE LINE COUNT AND CHECK IF NEW PAGE IS REQUIRED
C
C LCT = LCT-J
C IF (LCT.GE.0) RETURN
C
C J = -J
C
C INCREMENT PAGE COUNT AND START NEW PAGE
C
C 10 NPG = NPG+1
C LCT = LCTMAX+J
C WRITE(6,20)
C 20 FORMAT(1X,90X,49HMONTEUR ENERGY INTEGRATION TECHNIQUE (MEIT))
C RETURN
C END

```

```

000001
000002
000003
000004
000005
000006
000007
000008
000009
000010
000011
000012
000013
000014
000015
000016
000017
000018
000019
000020
000021
000022
000023
000024
000025
000026
000027
000028
000029
000030
000031
000032
000033
000034
000035
000036
000037
000038
000039
000040
000041
000042
000043
000044
000045
000046
000047
000048
000049
000050
000051
000052
000053
000054
000055
000056
000057
000058
000059
000060
000061
000062
000063
000064
000065
000066
000067
000068
000069
000070
000071
000072
000073
000074
000075
000076
000077
000078
000079
000080
000081
000082
000083
000084
000085
000086
000087
000088
000089
000090
000091
000092
000093
000094
000095
000096
000097
000098
000099
000100

```

```

00101 SUBROUTINE NEST
00102 INCLUDE COMMON
00103 INCLUDE COMMON
00104 COMMON/RUFF/ROUGH,RUF2(150)
00105 COMMON/PRCAL/PRL,PAT
00106 DIMENSION OPF(150),OTF(150),EMW(50),ZETA(150),CI(150),DPOS(150),
00107 *STORE(25),UEIP(150)
00108 C-----
00109 C *** ASSIGN INITIAL OR KNOWN VALUES
00110 CALL ESTATE(1,PE(1),HE(1),VISE(1),TE(1),EMW(1),PRE,ROE(1),AE)
00111 CALL ESTATE(3,PE(1),HW(1),VISV(1),TSP(1),EMW,PRW,ROW(1),AW)
00112 MPR=.42*HE(1)+.58*HW(1)+.19*(PRW+.5)*UE(1)+.2/6C/8TU/2.
00113 CALL ESTATE(1,PE(1),HPR,VISPR,TR,EMPR,PR,HOPR,APR)
00114 RECOV=SOR(PR)
00115 DO 3 I=1,NTY
00116   SOR(I)=S(I)/RN
00117   ZETA(I)=0.25*(SOR(I)+2)-0.25*SOR(I)*SIN(2.0*SOR(I))-
00118     * 0.125*COS(2.0*SOR(I))
00119   RUCH(I)=0.0
00120   TUE(I)=0.0
00121   AQML(I)=0.0
00122   3 CONTINUE
00123   RAF(I)=RECOV
00124   MR(I)=MT2
00125   HCAR(I)=0.0
00126   URE(I)=0.0
00127   YBAR(I)=0.0
00128   RETH(I)=0.0
00129   REPH(I)=0.0
00130   CSEE(I)=0.0
00131   BETP(1)=0.5
00132   BETP(2)=0.5
00133   CI(1)=0.0
00134   STIRAG=1.
00135   UE(1)=0.0
00136   TUT=0.0
00137   MSFT=0.0
00138   ACT=0.0
00139   ASRL=1.
00140   ASRT=1.
00141   RATIO=0.
00142   NOSTRAN=0
00143   STRAN=1.E10
00144   *****
00145   IF(ROUGH.EQ.1) RUF(1)=RUF2(1)
00146   IF(ROUGH.EQ.0) CALL RUFNEST(RUF(1))
00147   *****
00148 C
00149 C

```

```

000013
000026
000051
000064
000075
000077
000077
000122
000123
000124
000126
000126
000130
000132
000133
000134
000135
000136
000137
000140
000142
000143
000144
000146
000147
000150
000151
000152
000153
000154
000155
000156
000156
000160
000165

```

```

00164 000165
00166 000166
00170 000173
00173 000212
00175 000223
00200 000225
00201 000250
00202 000263
00203 000301
00205 000314
00206 000327
00207 000337
00211 000337
00213 000342
00214 000350
00215 000350
00220 000351
00221 000351
00222 000357
00223 000361
00224 000362
00226 000365
00230 000372
00231 000375
00234 000401
00236 000434
00237 000435
00240 000435
00241 000440
00241 000442
00247 000442
00250 000461
00251 000461
00251 000470
00252 000470
00255 000503
00256 000530
00256 000530
00256 000530
00260 000530
00260 000530

C *** FILL IN INTEGRATION POINT VARIABLES DEFINED AT BODY POINTS
IF(UE(1).LT..0000001) UE(1)=0
9999 PE(1)=ALOS(PE(1))
DO 7 I=1,NT
CALL TBLP(S(I),SP,TW(I),TSP,NS)
CALL TBLP(S(I),SP,WP(I),WPSP,NS)
CALL TBLP(S(I),SP,HV(I),HE,NS)
IF(THROUGH.EQ.1) CALL TBLP(S(I),SP, KUF(I),KUF2,NS)
CALL TBLP(S(I),SP,UEIP(I),UE,NS)
CALL TBLP(S(I),SP,PEPI(I),PE,NS)
IF(EP(1).LT..0000001) EP(1)=0.000001
7 CONTINUE
NSH1=NS-1
I=0
DO 995 IXX=1,NT
HE(1)=HW(1)
PEPI(1)=EXP(PEPI(1))
UE(1)=UEIP(1)
PE(1)=PEPI(1)
995 PEPI(1)=PEPI(1)/PE(1)
IF(UE(1).LT..0) UE(1)=0
NTW1=NT-1
DO 27 I=2,NTW1
27 CALL @ORTC(2,S(I-1),S(I),S(I+1),S(I),PE(I-1),PE(I),PE(I+1),OPDS(I
*)))
OPDS(1)=0
OPDS(NT)=OPDS(NT-1)
I=2
IF (IOEBUG.EQ.1)
WRITE(6,1001) I,PEPI(1),UE(1)
1001 FORMAT(15X,I6H1,PEPI(1),UE(1)/10X,I5.2E15.6)
ALFA=(1.0-PEPI(1))/(SOR(1)+2)
OUDZ=(UE(2)-UE(1))/(S(2)-S(1))
C *** COMPUTE WALL PROPERTIES
DO 45 I=1,NT
CALL ESTATE(3,PE(I),HW(I),VISH(I),TW(I),EMW,PRW,ROW(I),AW)
45 CONTINUE
C *** BEGINNING OF LOOP TO CALCULATE
C *** LAMINAR AUG. DUE TO TRANSITION PROXIMITY, RSRL
C *** KLIT=0
C ****

```

```

00261 910
00262 920
00263 930
00264 940
00265 950
00266 960
00267 970
00268 980
00269 990
00270 1000
00271 1010
00272 1020
00273 1030
00274 1040
00275 1050
00276 1060
00277 1070
00278 1080
00279 1090
00280 1100
00281 1110
00282 1120
00283 1130
00284 1140
00285 1150
00286 1160
00287 1170
00288 1180
00289 1190
00290 1200
00291 1210
00292 1220
00293 1230
00294 1240
00295 1250
00296 1260
00297 1270
00298 1280
00299 1290
00300 1300
00301 1310
00302 1320
00303 1330
00304 1340
00305 1350
00306 1360
00307 1370
00308 1380
00309 1390
00310 1400
00311 1410
00312 1420
00313 1430
00314 1440
00315 1450
00316 1460
00317 1470

S4 CONTINUE
C KLIT=KLIT+1
C MAT = MATL(1)
C IF (IOEUC.EQ.1)
C WRITE(6,1006) KLIT,STRAN,THE(1),RSRL
C 1006 FORMAT(10D,22M1IT,STRAN,THE(1),RSRL /1X,13.3X,1P3E13.6)
C IF (NOSTRAN.EQ.1.AND..XROUGH(1).GT.0.AND.KLIT.GT.1)
C S CALL LAMRUS(1,RSRL)
C ASRLAMRSL=02
C DUOS=DUOZ
C LIT=1
C *** ITERATE S.P. SOLUTIONS
C DO 60 ITER=1,3
C CALL SRI(1,C1,C2)
C CALL MSHAPE(1,1,MSF(1))
C THE(1)=SORT(C1*(1.0+KAF(1)*BP(1)*CMH(1))*VISE(1)/
C (ROE(1)*(1.0+MSF(1))*DUOS))
C PHI(1)=SORT(C2*(1.0+BP(1)*CMH(1))*VISE(1)/(2.0*ROE(1)*DUOS))
C RAF(1)=C2*THE(1)/(C1*PHI(1))
C 60 CONTINUE
C THE(1)=THE(1)*RSRL
C PHI(1)=PHI(1)*RSRL
C C1=C1*RSRLA
C C2=C2*RSRLA
C RUCH(1)=C2*VISE(1)/PHI(1)
C TUE(1)=0.0
C RUFST(1)=RSRL
C IF (KLIT.EQ.1) RUCHN=RUCH(1)
C METAUS=RUCH(1)/RUCHN
C DTF(1)=0.0
C OPF(1)=0.0
C *** SERIES SOLUTION FOR I=2,3
C GAM2 = (GAM2-1.)/GAM2
C A=(0.3333+(13.0*MSF(1))*ALFA/(4.0*GAM2))-
C S (MSF(1)+0.614)*ALFA*GAM2-0.659*ALFA*GAM2*(3.0+MSF(1))/
C S (8.0+2.0*MSF(1))
C B=(0.3333+3.0*ALFA/GAM2-
C S 1.318*ALFA*GAM2-2.0*ALFA*GAM2*(1.0-RECOV))/(1.0*BP(1)*CMH(1))/
C S (1.0-TW(1)/TE(1))/6.
C DO 63 I=2,3
C IF (XROUGH.EQ.1) GO TO 2001
C CALL RUFNES(I,RUF(I))
C 2001 CONTINUE
C THE(1)=THE(1)*(1.0+AS(SOR(I)*2))
C PHI(1)=PHI(1)*(1.0+BS(SOR(I)*2))
C UE(1)=DUOZ*(1.0+1.0*ALFA*(SOR(I)*2)/(4.0*GAM2))
C ROE(1)=ROE(1)*(1.0+ALFA*(SOR(I)*2)/GAM2)
C MAT1 = MAT
C MAT = MATL(1)

```



```

00334 2630 IF (THE(11).LE.0.) THE(11) = THEN
00335 2631 IF (ITER.LE.2) GO TO 80
00336 2632 IF (ABS(RESIP-RESIPE).LT.1.E-10) GO TO 80
00337 2633 PHI(11) = PHIN - (PHIN - PHIO)*RESIP/(RESIP - RESIPE)
00338 2634 RAT = PHI(11)/PHIN
00339 2635 IF (RAT .GT. 2 .OR. RAT .LT. .5) PHI(11) = PHIN - RESIP
00340 2636 80 CONTINUE
00341 2637 IF (PHI(11).LE.0.) PHI(11) = PHIN
00342 2638 REPH(11) = URE(11)*THE(11)
00343 2639 REPH(11) = URE(11)*PHI(11)
00344 2640 C *** COMPUTE LAMINAR INPUTS TO MEIT
00345 2641 IF (IDEBUG.NE.0)
00346 2642 WRITE(6,999) I,ITER,LYT,DUOS,DUOZ,UE(11),CI(11),CSEE(11),BETPI(11),
00347 2643 THE(11),PE(11),THE(11),PHI(11)
00348 2644 999 FORMAT(1H0,62HPRGM MEIT I,ITER,LYT,DUOS,DUOZ,UE,CI,CSEE,BETP,NE,
00349 2645 SPE,THE,PHI /1X,315,1X,8(E15.6))
00350 2646 IF (LYT.EQ.3) GO TO 100
00351 2647 C *****
00352 2648 CALL SR1(11,C1,C2)
00353 2649 C *****
00354 2650 TUL=C1*VISE(11)/THE(11)
00355 2651 RCL=C2*VISE(11)/PHI(11)
00356 2652 IF (S(11).GE.STRAM) GO TO 90
00357 2653 TUL=TUL*RSRLA
00358 2654 RCL=RCL*RSRLA
00359 2655 90 CONTINUE
00360 2656 IF (IDEBUG.NE.0)
00361 2657 WRITE(6,998) I,LYT,TUL,C1,C2,BETP(11),BP(11)
00362 2658 998 FORMAT(15X,29H1,LYT,TUL,C1,C2,BETP(11),BP(11)/10X,213,1P5E15.6)
00363 2659 C *****
00364 2660 CALL HSHAPE(11,1,MSFL)
00365 2661 C *****
00366 2662 IF (LYT.EQ.1) GO TO 120
00367 2663 C *** COMPUTE TURBULENT INPUTS TO MEIT
00368 2664 C *****
00369 2665 100 CALL SR2 (1, CFO2, CH, RSRTM, RSRTM)
00370 2666 TUT=ROE(11)*UE(11)*CFO2
00371 2667 TUT = RSRTM*TUTS
00372 2668 IF (LYT.LT.3.AND.TUT.LT.TUL) TUT=TUL
00373 2669 C *****
00374 2670 RCT=ROE(11)*UE(11)*CH
00375 2671 RCT = RSRTM*ACTS
00376 2672 IF (LYT.LT.3.AND.RCT.LT.RCL) RCT=RCL
00377 2673 RSRT=RCT/RCT8
00378 2674 C *****
00379 2675 CALL HSHAPE(11,2,MSFT)
00380 2676 C *****
00381 2677 IF (LYT.EQ.3) ADML(1)=1.0
00382 2678 IF (LYT.EQ.2) GO TO 110
00383 2679 GO TO 120
00384 2680 C *** COMPUTE INTERMITTENCY, PERSCH
00385 2681 110 TUE(11)=TUT-ROE(11)*UE(11)*TAMP/RET(11)*PERSH
00386 2682 IF (IDEBUG.NE.0)
00387 2683 WRITE(6,1005) TUE(11),TUL,TUT,TUTS,RSRTM,RCL,RCT,ACTS,RSRTM,CFO2,CH
00388 2684 1005 FORMAT(1H0,49HTUE,TUL,TUT,TUTS,RSRTM,RCL,RCT,ACTS,RSRTM,CFO2,CH
00389 2685 , /E15.6))
00390 2686 C *****

```

```

00664 3190 IF (ABS(TUT-TUL),LT,1.E-7) GO TO 119
00666 3200 ADML(I)=TUE(I)-TUL/(TUT-TUL)
00667 3210 IF (ADML(I),LT,0.) ADML(I)=1.
00671 3220 IF (ADML(I),GT,0.999) LTT=5
00673 3230 GO TO 120
00674 3240 LTT=0
00675 3250 ADML(I)=0.
00676 3260 INXT = I
00677 3270 C *** COMPUTE TRANSITIONAL MIX
00700 3280 120 CONTINUE
00701 3290 PR=PRL+ADML(I)*(PRT-PRL)
00702 3300 RECOV=SORT(PRL)+ADML(I)*(PRT-OC.3333-SORT(PRL))
00703 3310 TUE(I)=TUL+ADML(I)*(TUT-TUL)
00704 3320 RUCH(I)=RCL+ADML(I)*(RCT-RCL)
00705 3330 RAF(I)=RUCH(I)/TUE(I)
00706 3340 IF (IDEBUG,NE,0)
00707 3350 SWRITE(6,1000) ADML(I),PR,MI(I),ROE(I),UE(I),THE(I),ROI,
00708 3360 * V1,TW(I),TE(I),MCAM(I),GAZ,MSFT,TUL,TUE(I),TUT,TRNP,RETH(I)
00709 3370 * ,RSRTH,RCL,RCT,ACTS,RSRTH,CF02,CH
00710 3380 FORMAT(1H0,100H ADML(I),PR,MI(I),ROE(I),UE(I),THE(I),ROI,
00711 3390 SV1,TW(I),TE(I),MCAM(I),GAZ,MSFT,TUL,TUE,TUT,TRNP,RETH(I) /
00712 3400 S 2X,32HRSRTH,RCL,RCT,ACTS,RSRTH,CF02,CH/
00713 3410 80(1X,E15.6))
00714 3420 RUFST(I)=RSRL+ADML(I)*(RSRT-RSRL)
00715 3430 MSF(I)=MSFL+ADML(I)*(MSFT-MSFL)
00716 3440 MR(I)=ME(I)+RECOV *UE(I)*2/2./BTU/6C
00717 3450 IF (IDEBUG,NE,0)
00718 3460 *WRITE (6,173) I,ITER,ADML(I),TUE(I),RUCH(I),ROE(I),UE(I),
00719 3470 * ,TE(I),THE(I),VISE(I),ENTR(I),DTF(I),DPF(I),THE(I),PHI(I),
00720 3480 * VISE(I),ENTR(I),DTF(I),DPF(I),THE(I),PHI(I),VISE(I),THE(I),PHI(I),VISE
00721 3490 * ,1PTE13.6)
00722 3500 C *** INTEGRAL MOMENTUM AND ENERGY EONS
00723 3510 HT2=ME(I)+UE(I)*2/2./6C/RTU
00724 3520 DTF(I)=R(I)+UE(I)+TUE(I)-1.+RAF(I)*BP(I)*CMH(I)
00725 3530 DPF(I)=R(I)+RUCH(I)*MR(I)-MW(I)+HT2-MW(I)*BP(I)*CMH(I)
00726 3540 C
00727 3550 IF (ITER,EQ,1) GO TO 161
00728 3560 C
00729 3570 RAIT=ABS((TUE(I)-TUEOLD)/TUE(I))
00730 3580 RATR=ABS((RUCH(I)-RUCHO)/RUCH(I))
00731 3590 IF (RATR,LT,.001,AND,RATR,LT,.001) GO TO 162
00732 3600 GO TO 160
00733 3610 161 CONTINUE
00734 3620 LTTSTR = LTT
00735 3630 STORE(1) = ME(I)
00736 3640 STORE(2) = ENTR(I)
00737 3650 STORE(3) = TE(I)
00738 3660 STORE(4) = VISE(I)
00739 3670 STORE(5) = ROE(I)
00740 3680 STORE(6) = UE(I)
00741 3690 STORE(7) = MCAM(I)
00742 3700 STORE(8) = URE(I)
00743 3710 STORE(9) = BETPI(I)
00744 3720 STORE(10) = THE(I)
00745 3730 STORE(11) = PHI(I)
00746 3740 STORE(12) = RETH(I)
00747 3750
002435 002435 IF (ABS(TUT-TUL),LT,1.E-7) GO TO 119
002443 002443 ADML(I)=TUE(I)-TUL/(TUT-TUL)
002452 002452 IF (ADML(I),LT,0.) ADML(I)=1.
002460 002460 IF (ADML(I),GT,0.999) LTT=5
002467 002467 GO TO 120
002471 002471 LTT=0
002472 002472 ADML(I)=0.
002473 002473 INXT = I
002474 002474 C *** COMPUTE TRANSITIONAL MIX
002475 002475 120 CONTINUE
002476 002476 PR=PRL+ADML(I)*(PRT-PRL)
002502 002502 RECOV=SORT(PRL)+ADML(I)*(PRT-OC.3333-SORT(PRL))
002507 002507 TUE(I)=TUL+ADML(I)*(TUT-TUL)
002520 002520 RUCH(I)=RCL+ADML(I)*(RCT-RCL)
002525 002525 RAF(I)=RUCH(I)/TUE(I)
002532 002532 IF (IDEBUG,NE,0)
002536 002536 SWRITE(6,1000) ADML(I),PR,MI(I),ROE(I),UE(I),THE(I),ROI,
002536 002536 * V1,TW(I),TE(I),MCAM(I),GAZ,MSFT,TUL,TUE(I),TUT,TRNP,RETH(I)
002536 002536 * ,RSRTH,RCL,RCT,ACTS,RSRTH,CF02,CH
002536 002536 FORMAT(1H0,100H ADML(I),PR,MI(I),ROE(I),UE(I),THE(I),ROI,
002603 002603 SV1,TW(I),TE(I),MCAM(I),GAZ,MSFT,TUL,TUE,TUT,TRNP,RETH(I) /
002608 002608 S 2X,32HRSRTH,RCL,RCT,ACTS,RSRTH,CF02,CH/
002608 002608 80(1X,E15.6))
002608 002608 RUFST(I)=RSRL+ADML(I)*(RSRT-RSRL)
002608 002608 MSF(I)=MSFL+ADML(I)*(MSFT-MSFL)
002613 002613 MR(I)=ME(I)+RECOV *UE(I)*2/2./BTU/6C
002613 002613 IF (IDEBUG,NE,0)
002623 002623 *WRITE (6,173) I,ITER,ADML(I),TUE(I),RUCH(I),ROE(I),UE(I),
002623 002623 * ,TE(I),THE(I),VISE(I),ENTR(I),DTF(I),DPF(I),THE(I),PHI(I),
002623 002623 * VISE(I),ENTR(I),DTF(I),DPF(I),THE(I),PHI(I),VISE(I),THE(I),PHI(I),VISE
002653 002653 * ,1PTE13.6)
002653 002653 C *** INTEGRAL MOMENTUM AND ENERGY EONS
002653 002653 HT2=ME(I)+UE(I)*2/2./6C/RTU
002653 002653 DTF(I)=R(I)+UE(I)+TUE(I)-1.+RAF(I)*BP(I)*CMH(I)
002653 002653 DPF(I)=R(I)+RUCH(I)*MR(I)-MW(I)+HT2-MW(I)*BP(I)*CMH(I)
002674 002674 C
002674 002674 IF (ITER,EQ,1) GO TO 161
002674 002674 C
002674 002674 RAIT=ABS((TUE(I)-TUEOLD)/TUE(I))
002674 002674 RATR=ABS((RUCH(I)-RUCHO)/RUCH(I))
002674 002674 IF (RATR,LT,.001,AND,RATR,LT,.001) GO TO 162
002674 002674 GO TO 160
002674 002674 161 CONTINUE
002674 002674 LTTSTR = LTT
002674 002674 STORE(1) = ME(I)
002674 002674 STORE(2) = ENTR(I)
002674 002674 STORE(3) = TE(I)
002674 002674 STORE(4) = VISE(I)
002674 002674 STORE(5) = ROE(I)
002674 002674 STORE(6) = UE(I)
002674 002674 STORE(7) = MCAM(I)
002674 002674 STORE(8) = URE(I)
002674 002674 STORE(9) = BETPI(I)
002674 002674 STORE(10) = THE(I)
002674 002674 STORE(11) = PHI(I)
002674 002674 STORE(12) = RETH(I)
002674 002674

```

```

01020 376* STORE(14) = REPH(I)
01021 377* STORE(15) = HR(I)
01022 378* STORE(16) = ADML(I)
01023 379* STORE(17) = RUCH(I)
01024 310* STORE(18) = RAF(I)
01025 311* STORE(19) = RUFST(I)
01026 312* STORE(21) = HSF(I)
01027 313* STORE(22) = DTF(I)
01030 384* STORE(23) = DPF(I)
01031 385* STORE(24) = TUE(I)
01031 386*
01032 387*
01034 388*
01034 389*
01037 390*
01037 391*
01040 392*
01041 393*
01044 394*
01044 395*
01045 396*
01045 397*
01046 398*
01047 399*
01051 400*
01052 401*
01057 402*
01057 403*
01057 404*
01057 405*
01058 406*
01059 407*
01061 408*
01063 409*
01064 410*
01066 411*
01067 412*
01070 413*
01072 414*
01072 415*
01102 416*
01102 417*
01103 418*
01103 419*
01103 420*
01107 421*
01111 422*
01113 423*
01114 424*
01115 425*
01116 426*
01116 427*
01116 428*
01116 429*
01120 430*
01123 431*
01124 432*

376* STORE(14) = REPH(I)
377* STORE(15) = HR(I)
378* STORE(16) = ADML(I)
379* STORE(17) = RUCH(I)
310* STORE(18) = RAF(I)
311* STORE(19) = RUFST(I)
312* STORE(21) = HSF(I)
313* STORE(22) = DTF(I)
384* STORE(23) = DPF(I)
385* STORE(24) = TUE(I)
386*
387*
388*
389*
390*
391*
392*
393*
394*
395*
396*
397*
398*
399*
400*
401*
402*
403*
404*
405*
406*
407*
408*
409*
410*
411*
412*
413*
414*
415*
416*
417*
418*
419*
420*
421*
422*
423*
424*
425*
426*
427*
428*
429*
430*
431*
432*

C 160 CONTINUE
  IF (RAT - .05) 60, 67, 67
C *****
C 67 CALL MEIEX(I,1,DTF(I),DPF(I),RSRL,LTSTR,STORE)
C *****
  GO TO 71
60 IF (RAT - .05) 71, 69, 69
69 DPF(I) = DPF(I-1)
C *****
C CALL MEIEX(I,2,DTF(I),DPF(I),RSRL,LTSTR,STORE)
C *****
C 71 CONTINUE
  IF (IDEBUG.EQ.0) GO TO 162
  CALL LCOUN(5)
  WRITE(6,150) I,RAT,RATR
150 FORMAT(/,30X,56H COMPUTATION OF MEIT EQUATIONS DID NOT CONVERGE AT
  * POINT,14/
  * 55X,18H(TUE-TUE010)/TUE =,1PE12.5/
  * 55X,19H(RUCH-RUCH01)/RUCH =,1PE12.5)
162 CONTINUE
C *** DETERMINE TRANSITION PARAMETERS
170 IF (LT.NE.0) GO TO 175
  LTT=2
  IF (IBRUPT.EQ.1) LTT = 3
  PERSH = 2.
  TRNP = (TUT-TUL)*RETH(I)*PEKSH/ROE(I)/UE(I)
  IF (INXT.NE.I) STRAN = S(I)-RATIO(S(I)-S(INXT))
  IF (IDEBUG.EQ.1)
    $WRITE(6,1007) I,INXT,LTT,RATIO,STRAN
1007 FORMAT(1H0,22H,1,INXT,LTT,RATIO,STRAN /1X,313,2X,1PE12.5)
C *****
C 175 IF (LTT.LE.1) CALL TRANS(I,INXT,RATIO)
C *****
  IF (LTT.EQ.0) GO TO 65
  IF (KLIT.EQ.2) GO TO 176
  IF (NOSTRN.NE.1) GO TO 176
  GO TO 54
176 CONTINUE
  I=I+1
  IF (I.LE.NTT) GO TO 65
C *** END OF LOOP
C
  GO 180 I=1,NS
  ISUB = IPT(I)
  RUCHSPI(I) = RUCH(ISUB)
00180 00181 NS
00182 00182 IPT(I)
00183 00183 RUCH(ISUB)
00184 00184
00185 00185
00186 00186
00187 00187
00188 00188
00189 00189
00190 00190
00191 00191
00192 00192
00193 00193
00194 00194
00195 00195
00196 00196
00197 00197
00198 00198
00199 00199
00200 00200
00201 00201
00202 00202
00203 00203
00204 00204
00205 00205
00206 00206
00207 00207
00208 00208
00209 00209
00210 00210
00211 00211
00212 00212
00213 00213
00214 00214
00215 00215
00216 00216
00217 00217
00218 00218
00219 00219
00220 00220
00221 00221
00222 00222
00223 00223
00224 00224
00225 00225
00226 00226
00227 00227
00228 00228
00229 00229
00230 00230
00231 00231
00232 00232
00233 00233
00234 00234
00235 00235
00236 00236
00237 00237
00238 00238
00239 00239
00240 00240
00241 00241
00242 00242
00243 00243
00244 00244
00245 00245
00246 00246
00247 00247
00248 00248
00249 00249
00250 00250
00251 00251
00252 00252
00253 00253
00254 00254
00255 00255
00256 00256
00257 00257
00258 00258
00259 00259
00260 00260
00261 00261
00262 00262
00263 00263
00264 00264
00265 00265
00266 00266
00267 00267
00268 00268
00269 00269
00270 00270
00271 00271
00272 00272
00273 00273
00274 00274
00275 00275
00276 00276
00277 00277
00278 00278
00279 00279
00280 00280
00281 00281
00282 00282
00283 00283
00284 00284
00285 00285
00286 00286
00287 00287
00288 00288
00289 00289
00290 00290
00291 00291
00292 00292
00293 00293
00294 00294
00295 00295
00296 00296
00297 00297
00298 00298
00299 00299
00300 00300
00301 00301
00302 00302
00303 00303
00304 00304
00305 00305
00306 00306
00307 00307
00308 00308
00309 00309
00310 00310
00311 00311
00312 00312
00313 00313
00314 00314
00315 00315
00316 00316
00317 00317
00318 00318
00319 00319
00320 00320
00321 00321
00322 00322
00323 00323
00324 00324
00325 00325
00326 00326
00327 00327
00328 00328
00329 00329
00330 00330
00331 00331
00332 00332
00333 00333
00334 00334
00335 00335
00336 00336
00337 00337
00338 00338
00339 00339
00340 00340
00341 00341
00342 00342
00343 00343
00344 00344
00345 00345
00346 00346
00347 00347
00348 00348
00349 00349
00350 00350
00351 00351
00352 00352
00353 00353
00354 00354
00355 00355
00356 00356
00357 00357
00358 00358
00359 00359
00360 00360
00361 00361
00362 00362
00363 00363
00364 00364
00365 00365
00366 00366
00367 00367
00368 00368
00369 00369
00370 00370
00371 00371
00372 00372
00373 00373
00374 00374
00375 00375
00376 00376
00377 00377
00378 00378
00379 00379
00380 00380
00381 00381
00382 00382
00383 00383
00384 00384
00385 00385
00386 00386
00387 00387
00388 00388
00389 00389
00390 00390
00391 00391
00392 00392
00393 00393
00394 00394
00395 00395
00396 00396
00397 00397
00398 00398
00399 00399
00400 00400
00401 00401
00402 00402
00403 00403
00404 00404
00405 00405
00406 00406
00407 00407
00408 00408
00409 00409
00410 00410
00411 00411
00412 00412
00413 00413
00414 00414
00415 00415
00416 00416
00417 00417
00418 00418
00419 00419
00420 00420
00421 00421
00422 00422
00423 00423
00424 00424
00425 00425
00426 00426
00427 00427
00428 00428
00429 00429
00430 00430
00431 00431
00432 00432

```

003227
003231
003234
003234
003265

MRSP(I) = MRISUB)
PRES(I) = PEISUB)
100 CONTINUE
RETURN
END

4330
4340
4350
4360
4370

01125
01126
01127
01131
01132

```

00101 10 SUBROUTINE MEITER(I, ITR, DIF, OPF, RSHL, LTTSTR, STORE)
00102 20 DIMENSION STORE(25)
00103 30 INCLUDE COMON
00104 40 C-----
00105 50 GO TO (100, 200), ITR
00106 60 100 CONTINUE
00107 70 LTT = LTTSTR
00108 80 ME(I) = STORE(1)
00109 90 ENTR(I) = STORE(2)
00110 100 TE(I) = STORE(3)
00111 110 VISE(I) = STORE(4)
00112 120 ROE(I) = STORE(5)
00113 130 UE(I) = STORE(6)
00114 140 MCAM(I) = STORE(7)
00115 150 URE(I) = STORE(9)
00116 160 BETP(I) = STORE(10)
00117 170 THE(I) = STORE(11)
00118 180 PHI(I) = STORE(12)
00119 190 REYN(I) = STORE(13)
00120 200 REPH(I) = STORE(14)
00121 210 HR(I) = STORE(15)
00122 220 ADML(I) = STORE(16)

```

```

000010
000011
000012
000013
000014
000015
000016
000017
000018
000019
000020
000021
000022
000023
000024
000025
000026
000027
000028
000029
000030
000031
000032
000033
000034
000035
000036
000037
000038
000039
000040
000041
000042
000043
000044
000045
000046

```



```

00101 10 SUBROUTINE OUTPUT
00102 20 C
00103 30 C
00104 40 C
00105 50 C
00106 60 C
00107 70 C
00108 80 C
00109 90 C
00110 100 C
00111 110 C
00112 120 C
00113 130 C
00114 140 C
00115 150 C
00116 160 C
00117 170 C
00118 180 C
00119 190 C
00120 200 C
00121 210 C
00122 220 C
00123 230 C
00124 240 C
00125 250 C
00126 260 C
00127 270 C
00128 280 C
00129 290 C
00130 300 C
00131 310 C
00132 320 C
00133 330 C
00134 340 C
00135 350 C
00136 360 C
00137 370 C
00138 380 C
00139 390 C
00140 400 C
00141 410 C
00142 420 C
00143 430 C
00144 440 C
00145 450 C
00146 460 C
00147 470 C
00148 480 C
00149 490 C
00150 500 C

      THIS ROUTINE WRITES THE RESULTS OF THE INVISCID FLOW SOLUTION

      INCLUDE CORON
      INCLUDE CORUNT
      WRITE TITLE AND HEADING

      CALL LCOUNT(-3)
      WRITE(6,20040)
20040 FORMAT(50X,25HGENERAL INPUT INFORMATION/50X,25(1H*))
      CALL LCOUNT(6)
      WRITE(6,20060)
20060 FORMAT(75,4HBODY,T11,4HINTG,T19,4HMAIL,T26,6HSTREAM,T36,8HAXIAL,
+74S,6HRAID,T36,4HBODY,T65,18HNORMALIZED,T61,4HMAIL,T69,
+74SURFACE,T105,20M---EDGE CONDITION---/73,2HPT,T6,2HNO,T11,2HPT,
+714,2HNO,T20,2HNO,T26,6HLENGTH,T36,6HLENGTH,T45,6HLENGTH,T56,
+5HANGLE,T64,13HABLATION RATE,T81,4HICMP,T88,9HROUGHNESS,T101,
+8HMPRESSURE,T112,8HENTHALPY,T129,8HVELOCITY/T27,4HINCH,T37,4HINCH,
+746,4HINCH,
+756,3HDEC,T69,3HDEC,R,T91,3HML,T103,3HATN,T112,7HBTU/LBM,T124,
+6HFT/SEC,T74,3H(J),T12,3H(J),T18,6H(MATL),T27,3H(S),T37,3H(2),T46,
+3H(R),T55,7H(THE),T67,6H(BSP),T81,4H(TW),T89,8H(RUFIL),T103,
+4H(PE),T114,4H(ME),T125,4H(UE)/)
20121 FORMAT(1X,14,T11,13,T20,12,T25,F7.2,T35,F8.3,T44,F9.3,T54,F8.3,
+T64,F8.3,T79,F7.2,T89,F8.3,T101,F6.2,T111,F9.2,T123,F8.2)
      J = 1
      DO 100 I=1,NT
      IF (LCI-ST.1) GO TO 300
      CALL LCOUNT(-6)
      WRITE(6,20060)
      300 IF (IPT(J),NE.1) GO TO 400
      SINCH=S(I)*FT
      ZINCH=(Z(I)+28P(1))*FT
      RINCH=R(I)*FT
      THERAD = THE78(I)*RAD
      RUFIL=RUF(I)*FTIL
      CALL LCOUNT(1)
      WRITE(6,20121) J,I,MATL(I),SINCH,ZINCH,RINCH,THERAD,BSP(I),TW(I),
+RUFIL,PE(I),ME(I),UE(I)
      J = J+1
      60 TO 100
      900 IF (IABS(IPRNT),NE.2) GO TO 100
      SINCH=S(I)*FT
      ZINCH=(Z(I)+28P(1))*FT

```

000131
000134
000137
000137
000142
000145
000145
000171
000171
000171
000214

```

RINCHSR(I)OFT
THERAD = THETB(I)*RAD
RUFILRUF(I)*FTIL

C
CALL LCOUNT(I)
WRITE(6,20121) J,I,NATL(I),SINCH,ZINCH,RINCH,THERAD,BPSP(I),TV(I),
  *RUFIL,PE(I),NE(I),UE(I)
100 CONTINUE
C
RETURN
END

```

00171
00172
00173
00173
00174
00174
00175
00175
00214
00214
00216
00217

510
520
530
540
550
560
570
580
590
600
610

00161	CALL LCOUNT(1)	000105
00162	WRITE(6,20120) I,SIMCH,UE(1),MEAN(1),WE(1),TE(1),ROE(1),VISE(1),	000110
00162	U RE(1)	000110
00175	20120 FORMAT(1X,I10,F13.4,F13.1,F14.3,F13.1,F13.1,1PE13.3,1PE14.3,	000130
00175	1PE16.3)	000130
00176	100 CONTINUE	000130
00176	C	000130
00176	C	000130
00176	C	000130
00200	CALL LCOUNT(-3)	000130
00201	WRITE(6,40120)	000130
00203	40120 FORMAT(73X,59HVISCOS FLOW - WALL AND B. L. RECOVERY PROPERTIES/	000133
00203	59X,49(13H))	000140
00203	C	000140
00204	CALL LCOUNT(6)	000140
00205	WRITE(6,40140)	000140
00207	40140 FORMAT(4X,4HBOOT,4X,5HINIEG,4X,6HSTREAR,8X,4HWALL,9X,4HWALL,9X,	000143
00207	4HWALL,8X,4HWALL,7X,4HRECOVERY,4X,8HRECOVERY,3X,11HSENSBL CONV,	000148
00207	6X,4HCF/2/	000148
00207	3X,5HPT NO,4X,5HPT NO,4X,6HLENGTH,4X,11HTEMPERATURE,4X,	000150
00207	8HENTHALPY,5X,7HDENSITY,5X,9HVISCOSITY,4X,8HENTHALPY,5X,	000150
00207		000150

114

```

00101 10 SUBROUTINE QADRTC(J,X1,X2,X3,X,Y1,Y2,Y3,V)
00101 20 C-----
00101 30 C-----
00101 40 C-----
00101 50 C-----
00101 60 C-----
00101 70 C-----
00101 80 C-----
00101 90 C-----
00103 100 A=Y2
00104 110 O=(X3-X2)*(Y2-Y1)*(X3-X1)
00105 120 B=((Y3-Y2)*(X2-X1)*(Y2-Y1)*(X3-X2)*(Y2-Y1))/O
00106 130 C=((Y3-Y2)*(X2-X1)*(Y2-Y1)*(X3-X2))/O
00107 140 IF (J.GT.1) GO TO 10
00111 150 Y2=B*(X-X2)+C*(Y-X2)*(Y2-Y1)
00112 160 RETURN
00113 170 10 Y2=B+2.0*C*(X-X2)
00114 180 RETURN
00110 190 END
00001
00002
00003
00004
00005
00006
00007
00013

```

```
00101
00102
00103
00104
00105
00106
00107
00108
00109
00110
00111
00112
00113
00114
00115
00116
00117
00118
00119
00120
00121
00122
00123
00124
00125
00126
00127
00128
00129
00130
00131
00132
00133
00134
00135
00136
00137
00138
00139
00140
00141
00142
00143
00144
00145
00146
00147
00148
00149
00150
00151
00152
00153
00154
00155
00156
00157
00158
00159
00160
00161
00162
00163
00164
00165
00166
00167
00168
00169
00170
00171
00172
00173
00174
00175
00176
00177
00178
00179
00180
00181
00182
00183
00184
00185
00186
00187
00188
00189
00190
00191
00192
00193
00194
00195
00196
00197
00198
00199
00200
```

```
10
20
30
40
50
60
70
80
90
100
110
120
130
140
150
160
170
180
190
200
```

```
SUBROUTINE RUFES(I,RIF)
INCLUDE COMON
INCLUDE COMUNT
MAT = MATL(I)
RUFES(I)
CALL TBLPIS(I,SP,EFFKI,EFFKINS)
SCALLOPE ROUGHNESS MODEL *****
IF (RUF1(MAT).LE.1.E-7) GO TO 8
IF (I.GT.KSHOLD) GO TO 10
RUFES(I) = RUFES(I) * (1.0 + 0.77 * RUFES(I) * RUFES(I))
IF (RUFES(I).GT.0.9) RUFES(I) = 0.9
IF (THETB(I).GT.0.9) THETB(I) = 0.9
RAT = (RUFES - RUF1(MAT)) / (0.5 - THETB(I))
RUFES(I) = RUFES(I) * RAT + (THETB(I) - THETB(NTT))
GO TO 9
8 RUFES(I) = RUFES(I) * RUFES(I)
9 RUFES(I) = RUFES(I) * RUFES(I)
10 RUFES(I) = RUFES(I) * RUFES(I)
RETURN
END
```

```
000003
000004
000005
000006
000007
000008
000009
000010
000011
000012
000013
000014
000015
000016
000017
000018
000019
000020
000021
000022
000023
000024
000025
000026
000027
000028
000029
000030
000031
000032
000033
000034
000035
000036
000037
000038
000039
000040
000041
000042
000043
000044
000045
000046
000047
000048
000049
000050
000051
000052
000053
000054
000055
000056
000057
000058
000059
000060
000061
000062
000063
000064
000065
000066
000067
000068
000069
000070
000071
000072
000073
000074
000075
000076
000077
000078
000079
000080
000081
000082
000083
000084
000085
000086
000087
000088
000089
000090
000091
000092
000093
000094
000095
000096
000097
000098
000099
000100
000101
000102
000103
000104
000105
000106
000107
000108
000109
000110
000111
000112
000113
000114
000115
000116
000117
000118
000119
000120
000121
000122
000123
000124
000125
000126
000127
000128
000129
000130
000131
000132
000133
000134
000135
000136
000137
000138
000139
000140
000141
000142
000143
000144
000145
000146
000147
000148
000149
000150
000151
000152
000153
000154
000155
000156
000157
000158
000159
000160
000161
000162
000163
000164
000165
000166
000167
000168
000169
000170
000171
000172
000173
000174
000175
000176
000177
000178
000179
000180
000181
000182
000183
000184
000185
000186
000187
000188
000189
000190
000191
000192
000193
000194
000195
000196
000197
000198
000199
000200
```



```

00101 SUBROUTINE SR1(I,C1,C2)
00102 INCLUDE COMON
00103 COMMON/PACAL/PRL,PRT
00104 C *** LAMINAR SHEAR AND HEAT TRANSFER FACTORS
00105 MAT = MATL(I)
00106 C8=2.*BL3(MAT)*BP(I)*RAF(3)*CMH(1)
00107 C1=0.245
00108 IF (C8.GT.0.001) C1=C1*ALOG(1.0+C8)/C8
00109 IF (BETP(I).GT.0.) C1=C1*(1.0+3.0*BETP(I))*0.3333
00110 RECOV=SQRT(PR)
00111 HREF=0.42*HE(I)+0.58*HW(I)+0.19*RECOV*(HT2-HE(I))
00112 CALL ESTATE(1,PE(I),HREF,EREF,RNW,PRL,RORF,AA)
00113 VISR=EREF
00114 HT2=HE(I)+UE(I)*2./32.174/770.150
00115 REFFRORF=VISR*(HT2-HW(I))/(ROE(I)*VISE(I)*(HR(I)-HW(I)))
00116 IF (REFF.LE.0.) REFF=1.
00117 C8=2.*BLN(MAT)*BP(I)*CMH(1)
00118 C2=220*REFF/PR*0.3333
00119 IF (BETP(I).GT.0.) C2=C2*(1.0+4.*BETP(I))*0.1667
00120 IF (C8.GT..001) C2=C2*ALOG(1.0+C8)/C8
00121 RETURN
00122 END
00123
00124
00125
00126
00127
00128
00129
00130
00131
00132
00133
00134
00135
00136
00137
00002
00003
00004
00005
00006
00007
00008
00009
00010
00011
00012
00013
00014
00015
00016
00017
00018
00019
00020
00021
00022
00023

```

00101	1*	SUBROUTINE SR2 (I, C3, C5, RSKTH, RSKTH)	000005
00103	2*	INCLUDE COMMON	000020
00110	3*	COMMON/PRCAL/PRL,PR	000035
00110	4*	TURBULENT SHEAR AND HEAT TRANSFER FACTORS	000037
00111	5*	RECOV=PR**0.3333	000051
00112	6*	HREF=0.55*HE(I)*0.45*H(I)*0.15*RECOV*(MT2-HE(I))	000053
00113	7*	CALL ESTATE(1,PE(I),HREF,EREF,TRF,MMW,PRT,RORF,AA)	000062
00114	8*	VISR=ENERF	000065
00115	9*	REFR=ROF/ROE(I)*(VISR/VISE(I))*0.25	000101
00116	10*	MAT = MATL(I)	000103
00117	11*	CB=2.*BYS(MAT)*BP(I)*RAF(I)*CMH(I)	000117
00120	12*	BC=1.0	000125
00121	13*	IF (CB.GT.0.001) BC=ALOG(1.0+CB)/CB	
00123	14*	C4=1.	
00124	15*	IF (BETP(I).GT.0.) C4=(1.+3.*BETP(I))*0.3333	
00126	16*	C3 = .245*C4/RETH(I)	
00127	17*	IF (RETH(I).GT.2.) C3 = C3*.0123*RETH(I)/(100.*RETH(I))/	

```

00127
00131
00132
00133
00134
00135
00136
00137
00141
00142
00142
00144
00144
00145
00146
00147
00151
00152
00153
00154
00155
00156
00157
00160
00161

```

```

      S ALOG10(RETH(I))=1.6
      C3=C3*REFP*BC
      CB=2.*BTH(MAT)*BP(I)*CNH(1)
      BC=1.0
      IF (CB.GT.0.001) BC=ALOG(1.0+CB)/CB
      C6=1.
      IF (BETP(I).GT.0.) C6=1.+*.8BETP(I))=0.1667
      C5 = .22/PR=1.3333*C6/REPH(I)
      IF (REPH(I).GT.2.) C5 = C5+.0123/SQRT(PR)*REPH(I)/(100.+REPH(I))/
      S ALOG10(REPH(I))=1.6
      C3=C3*REFP*BC
      C
      ROUGHNESS INFLUENCE COEFFICIENTS -
      RSRTM = 1.
      RSRTM = 1.
      IF (RUF(I) .LE. 0.) GO TO 10
      ROVIS = VISE(I) / VISW(I) * SORT (ROW(I) / ROE(I))
      SLOPE = .09*RUF(I)/THE(I) + .53*(1. - EXP(-RUF(I)/THE(I))) + 1.
      ABSIS = ALOG10(REPH(I))*RUF(I)*ROVIS *SQRT(C3)/15.5)
      FUNCT = ABSIS - 1.5*(EXP(-ABSIS) - 1.)
      RSRTM = 1. + AMAX1(.5*SLOPE*FUNCT, 0.)
      RSRTM = 1. + AMAX1(.3*SLOPE*FUNCT, 0.)
10 CONTINUE
      RETURN
      END

```

```

000123
000133
000157
000165
000167
000203
000205
000221
000232
000232
000266
000266
000272
000274
000275
000300
000313
000331
000347
000357
000370
000402
000402
000445

```



```

00101 SUBROUTINE TRANS(I,INXT,RATIO)
00102 INCLUDE COMMON
00103 INCLUDE COMUNT
00104 INXT=I
00105 GO TO (100,200,300,400,500,500,500,700),NREYCH
00106
00107 C *** ALL LAMINAR FLOW
00108 100 GO TO 1000
00109
00110 C *** RE THEA VS. EDGE MACH NO.
00111 200 CALL TBLP(MCAM(I),AR,REYCH,REM,NAR)
00112 IF (RETH(I),LT,REYCH) GO TO 1000
00113 RATIO=(RETH(I)-REYCH)/(RETH(I)-RETH(I-1))
00114 INXT=I-1
00115 GO TO 700
00116
00117 C *** RE STREAMLENGTH VS. EDGE MACH NO.
00118 300 CALL TBLP(MCAM(I),AR,REYCH,REM,NAR)
00119 IF (S(I),URE(I),LT,REYCH) GO TO 1000
00120 RATIO=(S(I)-URE(I)-REYCH)/(S(I)-URE(I)-S(I-1)*URE(I-1))
00121 INXT=I-1
00122 GO TO 700
00123
00124 C *** AXIAL DISTANCE VS. ALTITUDE
00125 400 ZTRAN=DLTRAN
00126 IF (Z(I),LT,ZTRAN) GO TO 1000
00127 RATIO=(Z(I)-ZTRAN)/(Z(I)-Z(I-1))
00128 INXT=I-1
00129 GO TO 700
00130
00131 C *** PANT ROUGH WALL CRITERION
00132 500 IF (I,GT,KSHOLD) GO TO 600
00133 IF (NREYCH,EG,6) GO TO 504
00134 PSYETH(I)/TE(I)
00135 GO TO 506
00136
00137 504 PSY = 1.08*(I)+(9+.1*(CARB))*.1+.25*(P(I))*ROE(I)/ROW(I)
00138 506 TPII=RETH(I)*((RUF(I))/(PSY*THE(I)))*.0.70)
00139 IF (TPII),LT,255.0) GO TO 1000
00140 DO 510 J=1,I
00141 IF (TP(J),GE,215.0) GO TO 515
00142 510 CONTINUE
00143 515 I=J-1
00144 IF (I,LT,4) I=4
00145 IF (I,GT,4) RATIO=(215.-TP(I))/(TP(I+1)-TP(I))
00146 INXT=I+1
00147 GO TO 700
00148
00149 C *** CONE TRANSITION
00150 600 IF (RETH(I),LT,275.0*EXP(0.13*(MCA(I))) GO TO 1000
00151 GO TO 700
00152
00153 C *** TRANSITION AT I=4
00154 700 LTY=0
00155 IF (I,LT,KSHOLD) NOSTRM = 1
00156 1000 CONTINUE
00157 RETURN
00158 END
00159
00160
00161
00162
00163
00164
00165
00166
00167
00168
00169
00170
00171
00172
00173
00174
00175
00176
00177
00178
00179
00180
00181
00182
00183
00184
00185
00186
00187
00188
00189
00190
00191
00192
00193
00194
00195
00196
00197
00198
00199
00200
00201
00202
00203
00204
00205
00206
00207
00208
00209
00210
00211
00212
00213
00214
00215
00216
00217
00218
00219
00220
00221
00222
00223
00224
00225
00226
00227
00228
00229
00230
00231
00232
00233
00234
00235
00236
00237
00238
00239
00240
00241
00242
00243
00244
00245
00246
00247
00248
00249
00250
00251
00252
00253
00254
00255
00256
00257
00258
00259
00260
00261
00262
00263
00264
00265
00266
00267
00268
00269
00270
00271
00272
00273
00274
00275
00276
00277
00278
00279
00280
00281
00282
00283
00284
00285
00286
00287
00288
00289
00290
00291
00292
00293
00294
00295
00296
00297
00298
00299
00300

```

000081
000001
000001
000001
000007
000011
000015
000016
000025
000031
000035
000046
000055
000067
000102
000120
000131
CJ0140
000146
000146
000146
000146
000151
000154
G00159
000154
000157
000163
000163
000168
000168
000177
000203
000203
000209
000213
000213
000220
000220
000222

```

00161 530 Z(J) = Z(J-1)+02
00162 540 TMTB(J) = TMTB(J-1)+DTMET
00163 550 IF (J.LT.NIPT(I)+IPT(I)) GO TO 60
00164 560 J = J+1
00165 570 Z(J) = ZSP(I+1)
00166 580 TMTB(J) = TMTBSP(I+1)
00167 590 R(J) = RSP(I+1)
00170 600 IPT(I+1) = J
00171 610
00172 620
00173 630
00174 640
00175 650
00176 660
00177 670
00201 680
00202 690
00203 700
00204 710
00206 720
00210 730
00211 740
00212 750
00213 760
00214 770
00215 780
00216 790
00220 800
00221 810
00222 820
00224 830
00225 840
00226 850
00226 860
00230 870
00231 880
00231 890
00232 900
00235 910
00236 920
00236 930
00237 940
00237 950
00241 960
00241 970
00241 980
00242 990
00243 1000
00244 1010
00245 1020
00246 1030
00247 1040
00252 1050
00253 1060

C
Z(J) = Z(J-1)+02
TMTB(J) = TMTB(J-1)+DTMET
IF (J.LT.NIPT(I)+IPT(I)) GO TO 60
J = J+1
Z(J) = ZSP(I+1)
TMTB(J) = TMTBSP(I+1)
R(J) = RSP(I+1)
IPT(I+1) = J
90 CONTINUE
J = 1
NTTM1 = NTT-1
DO 170 I=1,NTTM1
IF (I.EQ.IPT(J)) J = J+1
MATL(I) = IMAT(J,1)
IF (I.LE.(IPT(J-1)+IPT(J))/2) MATL(I) = IMAT(J-1,1)
170 CONTINUE
MATL(NTT) = IMAT(NS,1)
C
S(1) = 0.0
SP(1) = 0.
Z(1) = 0.
J=2
DO 100 I=2,NTT
Z(I) = Z(I-1)+ZSP(I)
S(I) = S(I-1)+SGR((Z(I)-Z(I-1))**2+(R(I)-R(I-1))**2)
IF (I.LT.IPT(J)) GO TO 100
SP(J) = S(I)
J=J+1
100 CONTINUE
C
NTTM1=NTT-1
ORDS(1)=1.
DO 130 I=2,NTTM1
RAT=(S(I)-S(I-1))/(S(I+1)-S(I))
ORDS(I)=(RAT**2+R(I+1)+(1.-RAT**2)*R(I)-R(I-1))/(1.+RAT)/
*(S(I)-S(I-1))
130 CONTINUE
C
ORDS(NTT)=(R(NTT)-R(NTTM1))/(S(NTT)-S(NTTM1))
C
C
NOSE RADIUS CALCULATIONS
SX = Z(1)
SX2 = Z(1)**2
SX2Z = SX2*R(1)**2
SX2X = (SX2*R(1)**2)*Z(1)
FNUM = 1.
DO 110 I=2,NTT
XY2 = Z(I)**2+R(I)**2
SX = SX+Z(I)

```

```

00254 1070 SX2 = SX2+2(1)002
00255 1080 SX2 = SX2+XY2
00256 1090 SX2X = SX2X+XY202(1)
00257 1100 FNUM = FNUM+1
00258 1110 IF (THETB(1).LT..00139) GO TO 120
00259 1120 CONTINUE
00260 1130 DENO = SX002-SX20FNUM+1.E-10
00261 1140 BSH = (SX0SX2-SX2X0FNUM)/DENO/2.
00262 1150 CSH = (SX20SX2-SX2X0SX)/DENO
00263 1160 B2MC=BSH002-CSH
00264 1170 IF(B2MC) 95,99,96
00265 1180 94 RN = 100.
00266 1190 GO TO 130
00267 1200 95 WRITE(6,98) B2MC,BSH,CSH,DENO,SX,SX2,SX2X,SX2X,FNUM
00268 1210 98 FORMAT(/6H B2MC=E12.5,2XSH BSH=E12.5,2XSM CSH=E12.5,2XSM DENO=E12.
00269 1220 5,6H SX=E12.5,2XSM SX2=E12.5,2XSM SX2X=E12.5,2XSM SX2X=F12.5,2X.
00270 1230 6H FNUM=E12.5/)
00271 1240
C
00272 1250
C
00273 1260
C
00274 1270
C
00275 1280
C
00276 1290
C
00277 1300
C
00278 1310
C
00279 1320
C
00280 1330
C
00281 1340
C
00282 1350
C
00283 1360
C
00284 1370
C
00285 1380
C
00286 1390
C
00287 1400
C
00288 1410
C
00289 1420
C
00290 1430
C
00291 1440
C
00292 1450
C
00293 1460
C
00294 1470
C
00295 1480
C
00296 1490
C
00297 1500
C
00298 1510
C
00299 1520
C
00300 1530
C
00301 1540
C
00302 1550
C
00303 1560
C
00304 1570
C
00305 1580
C
00306 1590
C
00307 1600
C
00308 1610
C
00309 1620
C
00310 1630
C
00311 1640
C
00312 1650
C
00313 1660
C
00314 1670
C
00315 1680
C
00316 1690
C
00317 1700
C
00318 1710
C
00319 1720
C
00320 1730
C
00321 1740
C
00322 1750
C
00323 1760
C
00324 1770
C
00325 1780
C
00326 1790
C
00327 1800
C
00328 1810
C
00329 1820
C
00330 1830
C
00331 1840
C
00332 1850
C
00333 1860
C
00334 1870
C
00335 1880
C
00336 1890
C
00337 1900
C
00338 1910
C
00339 1920
C
00340 1930
C
00341 1940
C
00342 1950
C
00343 1960
C
00344 1970
C
00345 1980
C
00346 1990
C
00347 2000
C
00348 2010
C
00349 2020
C
00350 2030
C
00351 2040
C
00352 2050
C
00353 2060
C
00354 2070
C
00355 2080
C
00356 2090
C
00357 2100
C
00358 2110
C
00359 2120
C
00360 2130
C
00361 2140
C
00362 2150
C
00363 2160
C
00364 2170
C
00365 2180
C
00366 2190
C
00367 2200
C
00368 2210
C
00369 2220
C
00370 2230
C
00371 2240
C
00372 2250
C
00373 2260
C
00374 2270
C
00375 2280
C
00376 2290
C
00377 2300
C
00378 2310
C
00379 2320
C
00380 2330
C
00381 2340
C
00382 2350
C
00383 2360
C
00384 2370
C
00385 2380
C
00386 2390
C
00387 2400
C
00388 2410
C
00389 2420
C
00390 2430
C
00391 2440
C
00392 2450
C
00393 2460
C
00394 2470
C
00395 2480
C
00396 2490
C
00397 2500
C
00398 2510
C
00399 2520
C
00400 2530
C
00401 2540
C
00402 2550
C
00403 2560
C
00404 2570
C
00405 2580
C
00406 2590
C
00407 2600
C
00408 2610
C
00409 2620
C
00410 2630
C
00411 2640
C
00412 2650
C
00413 2660
C
00414 2670
C
00415 2680
C
00416 2690
C
00417 2700
C
00418 2710
C
00419 2720
C
00420 2730
C
00421 2740
C
00422 2750
C
00423 2760
C
00424 2770
C
00425 2780
C
00426 2790
C
00427 2800
C
00428 2810
C
00429 2820
C
00430 2830
C
00431 2840
C
00432 2850
C
00433 2860
C
00434 2870
C
00435 2880
C
00436 2890
C
00437 2900
C
00438 2910
C
00439 2920
C
00440 2930
C
00441 2940
C
00442 2950
C
00443 2960
C
00444 2970
C
00445 2980
C
00446 2990
C
00447 3000
C
00448 3010
C
00449 3020
C
00450 3030
C
00451 3040
C
00452 3050
C
00453 3060
C
00454 3070
C
00455 3080
C
00456 3090
C
00457 3100
C
00458 3110
C
00459 3120
C
00460 3130
C
00461 3140
C
00462 3150
C
00463 3160
C
00464 3170
C
00465 3180
C
00466 3190
C
00467 3200
C
00468 3210
C
00469 3220
C
00470 3230
C
00471 3240
C
00472 3250
C
00473 3260
C
00474 3270
C
00475 3280
C
00476 3290
C
00477 3300
C
00478 3310
C
00479 3320
C
00480 3330
C
00481 3340
C
00482 3350
C
00483 3360
C
00484 3370
C
00485 3380
C
00486 3390
C
00487 3400
C
00488 3410
C
00489 3420
C
00490 3430
C
00491 3440
C
00492 3450
C
00493 3460
C
00494 3470
C
00495 3480
C
00496 3490
C
00497 3500
C
00498 3510
C
00499 3520
C
00500 3530
C
00501 3540
C
00502 3550
C
00503 3560
C
00504 3570
C
00505 3580
C
00506 3590
C
00507 3600
C
00508 3610
C
00509 3620
C
00510 3630
C
00511 3640
C
00512 3650
C
00513 3660
C
00514 3670
C
00515 3680
C
00516 3690
C
00517 3700
C
00518 3710
C
00519 3720
C
00520 3730
C
00521 3740
C
00522 3750
C
00523 3760
C
00524 3770
C
00525 3780
C
00526 3790
C
00527 3800
C
00528 3810
C
00529 3820
C
00530 3830
C
00531 3840
C
00532 3850
C
00533 3860
C
00534 3870
C
00535 3880
C
00536 3890
C
00537 3900
C
00538 3910
C
00539 3920
C
00540 3930
C
00541 3940
C
00542 3950
C
00543 3960
C
00544 3970
C
00545 3980
C
00546 3990
C
00547 4000
C
00548 4010
C
00549 4020
C
00550 4030
C
00551 4040
C
00552 4050
C
00553 4060
C
00554 4070
C
00555 4080
C
00556 4090
C
00557 4100
C
00558 4110
C
00559 4120
C
00560 4130
C
00561 4140
C
00562 4150
C
00563 4160
C
00564 4170
C
00565 4180
C
00566 4190
C
00567 4200
C
00568 4210
C
00569 4220
C
00570 4230
C
00571 4240
C
00572 4250
C
00573 4260
C
00574 4270
C
00575 4280
C
00576 4290
C
00577 4300
C
00578 4310
C
00579 4320
C
00580 4330
C
00581 4340
C
00582 4350
C
00583 4360
C
00584 4370
C
00585 4380
C
00586 4390
C
00587 4400
C
00588 4410
C
00589 4420
C
00590 4430
C
00591 4440
C
00592 4450
C
00593 4460
C
00594 4470
C
00595 4480
C
00596 4490
C
00597 4500
C
00598 4510
C
00599 4520
C
00600 4530
C
00601 4540
C
00602 4550
C
00603 4560
C
00604 4570
C
00605 4580
C
00606 4590
C
00607 4600
C
00608 4610
C
00609 4620
C
00610 4630
C
00611 4640
C
00612 4650
C
00613 4660
C
00614 4670
C
00615 4680
C
00616 4690
C
00617 4700
C
00618 4710
C
00619 4720
C
00620 4730
C
00621 4740
C
00622 4750
C
00623 4760
C
00624 4770
C
00625 4780
C
00626 4790
C
00627 4800
C
00628 4810
C
00629 4820
C
00630 4830
C
00631 4840
C
00632 4850
C
00633 4860
C
00634 4870
C
00635 4880
C
00636 4890
C
00637 4900
C
00638 4910
C
00639 4920
C
00640 4930
C
00641 4940
C
00642 4950
C
00643 4960
C
00644 4970
C
00645 4980
C
00646 4990
C
00647 5000
C
00648 5010
C
00649 5020
C
00650 5030
C
00651 5040
C
00652 5050
C
00653 5060
C
00654 5070
C
00655 5080
C
00656 5090
C
00657 5100
C
00658 5110
C
00659 5120
C
00660 5130
C
00661 5140
C
00662 5150
C
00663 5160
C
00664 5170
C
00665 5180
C
00666 5190
C
00667 5200
C
00668 5210
C
00669 5220
C
00670 5230
C
00671 5240
C
00672 5250
C
00673 5260
C
00674 5270
C
00675 5280
C
00676 5290
C
00677 5300
C
00678 5310
C
00679 5320
C
00680 5330
C
00681 5340
C
00682 5350
C
00683 5360
C
00684 5370
C
00685 5380
C
00686 5390
C
00687 5400
C
00688 5410
C
00689 5420
C
00690 5430
C
00691 5440
C
00692 5450
C
00693 5460
C
00694 5470
C
00695 5480
C
00696 5490
C
00697 5500
C
00698 5510
C
00699 5520
C
00700 5530
C
00701 5540
C
00702 5550
C
00703 5560
C
00704 5570
C
00705 5580
C
00706 5590
C
00707 5600
C
00708 5610
C
00709 5620
C
00710 5630
C
00711 5640
C
00712 5650
C
00713 5660
C
00714 5670
C
00715 5680
C
00716 5690
C
00717 5700
C
00718 5710
C
00719 5720
C
00720 5730
C
00721 5740
C
00722 5750
C
00723 5760
C
00724 5770
C
00725 5780
C
00726 5790
C
00727 5800
C
00728 5810
C
00729 5820
C
00730 5830
C
00731 5840
C
00732 5850
C
00733 5860
C
00734 5870
C
00735 5880
C
00736 5890
C
00737 5900
C
00738 5910
C
00739 5920
C
00740 5930
C
00741 5940
C
00742 5950
C
00743 5960
C
00744 5970
C
00745 5980
C
00746 5990
C
00747 6000
C
00748 6010
C
00749 6020
C
00750 6030
C
00751 6040
C
00752 6050
C
00753 6060
C
00754 6070
C
00755 6080
C
00756 6090
C
00757 6100
C
00758 6110
C
00759 6120
C
00760 6130
C
00761 6140
C
00762 6150
C
00763 6160
C
00764 6170
C
00765 6180
C
00766 6190
C
00767 6200
C
00768 6210
C
00769 6220
C
00770 6230
C
00771 6240
C
00772 6250
C
00773 6260
C
00774 6270
C
00775 6280
C
00776 6290
C
00777 6300
C
00778 6310
C
00779 6320
C
00780 6330
C
00781 6340
C
00782 6350
C
00783 6360
C
00784 6370
C
00785 6380
C
00786 6390
C
00787 6400
C
00788 6410
C
00789 6420
C
00790 6430
C
00791 6440
C
00792 6450
C
00793 6460
C
00794 6470
C
00795 6480
C
00796 6490
C
00797 6500
C
00798 6510
C
00799 6520
C
00800 6530
C
00801 6540
C
00802 6550
C
00803 6560
C
00804 6570
C
00805 6580
C
00806 6590
C
00807 6600
C
00808 6610
C
00809 6620
C
00810 6630
C
00811 6640
C
00812 6650
C
00813 6660
C
00814 6670
C
00815 6680
C
00816 6690
C
00817 6700
C
00818 6710
C
00819 6720
C
00820 6730
C
00821 6740
C
00822 6750
C
00823 6760
C
00824 6770
C
00825 6780
C
00826 6790
C
00827 6800
C
00828 6810
C
00829 6820
C
00830 6830
C
00831 6840
C
00832 6850
C
00833 6860
C
00834 6870
C
00835 6880
C
00836 6890
C
00837 6900
C
00838 6910
C
00839 6920
C
00840 6930
C
00841 6940
C
00842 6950
C
00843 6960
C
00844 6970
C
00845 6980
C
00846 6990
C
00847 7000
C
00848 7010
C
00849 7020
C
00850 7030
C
00851 7040
C
00852 7050
C
00853 7060
C
00854 7070
C
00855 7080
C
00856 7090
C
00857 7100
C
00858 7110
C
00859 7120
C
00860 7130
C
00861 7140
C
00862 7150
C
00863 7160
C
00864 7170
C
00865 7180
C
00866 7190
C
00867 7200
C
00868 7210
C
00869 7220
C
00870 7230
C
00871 7240
C
00872 7250
C
00873 7260
C
00874 7270
C
00875 7280
C
00876 7290
C
00877 7300
C
00878 7310
C
00879 7320
C
00880 7330
C
00881 7340
C
00882 7350
C
00883 7360
C
00884 7370
C
00885 7380
C
00886 7390
C
00887 7400
C
00888 7410
C
00889 7420
C
00890 7430
C
00891 7440
C
00892 7450
C
00893 7460
C
00894 7470
C
00895 7480
C
00896 7490
C
00897 7500
C
00898 7510
C
00899 7520
C
00900 7530
C
00901 7540
C
00902 7550
C
00903 7560
C
00904 7570
C
00905 7580
C
00906 7590
C
00907 7600
C
00908 7610
C
00909 7620
C
00910 7630
C
00911 7640
C
00912 7650
C
00913 7660
C
00914 7670
C
00915 7680
C
00916 7690
C
00917 7700
C
00918 7710
C
00919 7720
C
00920 7730
C
00921 7740
C
00922 7750
C
00923 7760
C
00924 7770
C
00925 7780
C
00926 7790
C
00927 7800
C
00928 7810
C
00929 7820
C
00930 7830
C
00931 7840
C
00932 7850
C
00933 7860
C
00934 7870
C
00935 7880
C
00936 7890
C
00937 7900
C
00938 7910
C
00939 7920
C
00940 7930
C
00941 7940
C
00942 7950
C
00943 7960
C
00944 7970
C
00945 7980
C
00946 7990
C
00947 8000
C
00948 8010
C
00949 8020
C
00950 8030
C
00951 8040
C
00952 8050
C
00953 8060
C
00954 8070
C
00955 8080
C
00956 8090
C
00957 8100
C
00958 8110
C
00959 8120
C
00960 8130
C
00961 8140
C
00962 8150
C
00963 8160
C
00964 8170
C
00965 8180
C
00966 8190
C
00967 8200
C
00968 8210
C
00969 8220
C
00970 8230
C
00971 8240
C
00972 8250
C
00973 8260
C
00974 8270
C
00975 8280
C
00976 8290
C
00977 8300
C
00978 8310
C
00979 8320
C
00980 8330
C
00981 8340
C
00982 8350
C
00983 8360
C
00984 8370
C
00985 8380
C
00986 8390
C
00987 8400
C
00988 8410
C
00989 8420
C
00990 8430
C
00991 8440
C
00992 8450
C
00993 8460
C
00994 8470
C
00995 8480
C
00996 8490
C
00997 8500
C
00998 8510
C
00999 8520
C
01000 8530
C

```



```

00101 10
00101 20
00101 30
00101 40
00101 50
00101 60
00101 70
00101 80
00101 90
00101 100
00101 110
00101 120
00101 130
00101 140
00101 150
00101 160
00101 170
00101 180
00101 190
00101 200
00101 210
00101 220
00101 230
00103 240
00106 250
00107 260
00110 270
00111 280
00112 290
00113 300

SUBROUTINE XSOLVE(X,Y,YGIVN,NCOUNT,XLO,YLO,XHI,YHI)
-----
C
C
C THIS ROUTINE IS USED IN ITERATION FOR X WHICH SATISFIES THE
C EQUATION Y = F(X) WHEN Y = YGIVN
C
C-----
C
C NOTE: A GOOD INITIAL GUESS IS ESSENTIAL FOR THE SOLUTION.
C
C--- INPUT ---
C X = AN ESTIMATED VALUE OF THE SOLUTION
C Y = CALCULATED FROM Y = F(X) IN THE CALLING ROUTINE
C YGIVN = THE VALUE OF Y FOR WHICH THE X VALUE IS BEING SOLVED
C NCOUNT = A COUNTER WHICH MUST BE 1 WHEN XSOLVE IS FIRST CALLED
C
C--- OUTPUT ---
C X = A VALUE OF X WHICH MORE CLOSELY SATISFIES THE EQUATION
C YGIVN = F(X)
C XLO,YLO,XHI,YHI = THE COORDINATES OF THE TWO POINTS WHICH ARE
C CONNECTED BY A STRAIGHT LINE TO SOLVE FOR X
C
C IF (NCOUNT-2) 10,20,30
10 XLO = X
YLO = Y
X = XLO+ABS(.011*XLO)
NCOUNT = 2
RETURN
20 XHI = X

```

```

000003
000005
000007
000013
000015
000021

```

```

00114 310 YMI = Y
00115 320 X = (Y6IVN-YLO)/(YMI-YLO)*(XMI-XLO)+XLO
00116 330 NCOUNT = NCOUNT+1
00117 340 RETURN
00120 350 DYLO = YLO-Y6IVN
00121 360 DYMI = YMI-Y6IVN
00122 370 IF (DYLO+DYMI) 40,40,70
00123 380 IF (Y-Y6IVN) 60,50,50
00125 390
00125 400 YLO AND YMI STRADDLE Y6IVN WITH YLO CLOSER TO Y6IVN
00125 410
00130 420 50 XMI = X
00131 430 YMI = Y
00132 440 60 TO 100
00132 450
00132 460 YLO AND YMI STRADDLE Y6IVN WITH YMI CLOSER TO Y6IVN
00133 470
00133 480 60 XLO = X
00134 490 YLO = Y
00135 500 60 TO 100
00136 510 DYLO = ABS(DYLO)
00137 520 DYMI = ABS(DYMI)
00140 530 IF (DYMI.LT.DYLO) 60 TO 90
00140 540
00140 550 YLO AND YMI ON SAME SIDE OF Y6IVN WITH YLO CLOSER TO Y6IVN
00140 560
00142 570 80 IF (ABS(Y-Y6IVN).LT.DYLO) 60 TO 85
00144 580 X = X+(XMI-X)/5.
00145 590 60 TO 200
00146 600 XMI = XLO
00147 610 YMI = YLO
00150 620 XLO = X
00151 630 YLO = Y
00152 640 60 TO 100
00152 650
00152 660 YLO AND YMI ON SAME SIDE OF Y6IVN WITH YMI CLOSER TO Y6IVN
00152 670
00153 680 90 IF (ABS(Y-Y6IVN).LT.DYMI) 80 TO 95
00155 690 X = X-(X-XLO)/5.
00156 700 60 TO 200
00157 710 95 XLO = XMI
00160 720 YLO = YMI
00161 730 XMI = X
00162 740 YMI = Y
00163 750 100 X = (Y6IVN-YLO)/(YMI-YLO+1.E-10)*(XMI-XLO)+XLO
00164 760 200 CONTINUE
00165 770 NCOUNT = NCOUNT+1
00166 780 IF (NCOUNT.LE.100) 80 TO 300
00170 790 WRITE(6,250) X,Y,Y6IVN,NCOUNT,XLO,YLO,XMI,YMI
00202 800 FORMAT(1X,10(1H:),X5OLVE X,Y,Y6IVN,NCOUNT,XLO,YLO,XMI,YMI,/11X,
00202 810 3E12.5,15,4E12.5)
00203 820 STOP
00204 830 300 CONTINUE
00205 840 RETURN
00206 850 END

```

REFERENCES

1. User's Manual, "Aerotherm Real Gas Energy Integral Boundary Layer Program ((ARGEIBL)," Aerotherm Report UM-75-69, December 1975.
2. User's Manual, "Boundary Layer Integral Matrix Procedure Version C (BLIMPC)," Aerotherm Report UM-70-20, June 22, 1970.
3. Tong, H., Suchsland, K.E., Murphy, A.J., Kwong, K.C., Lee, K., Chu, E., "Graphite Performance Prediction Program, Volume II - Applicability of Reentry Technology to Rocket Nozzle Design," AFRPL TR-77-59, November 1977.
4. Abbett, M.J., Dahm, T.J., Brink, D.F., Rafinejad, D., Wolf, C.J., "Passive Nosedip Technology (PANT II) Program, Volume II. Computer User's Manual: Abres Shape Change Code (ASCC)," Aerotherm Report 76-224, October 1976.
5. "ICRPG Turbulent Boundary Layer Nozzle Analysis Computer Program," July 1968, Pratt & Whitney Aircraft.
6. Dahm, T.J., Cooper, L., Rafinejad, D., Youngblood, S.B., Kelly, J.T., "Passive Nosedip Technology (PANT II) Program, Volume I. Inviscid Flow and Heat Transfer Modeling for Reentry Vehicle Nosedips," Aerotherm Report 76-224, October 1976.
7. Lees, L., "Convective Heat Transfer with Mass Addition and Chemical Reactions," Combustion and Propulsion, Third AGARD Colloquium, Pergamon Press, New York, March 1958.
8. Jackson, M.D. and Baker, D.L., "Surface Roughness Effects, Part I, Experimental Data," Interim Report, PANT Program, Vol. III, SAMSO TR-74-86, June 1974.
9. Headzer, J., Moffett, R., and Kays, W., "The Turbulent Boundary Layer on a Rough, Porous Plate: Experimental Heat Transfer with Uniform Blowing," Report No. HMT-18, Stanford University, May 1974.
10. Reda, D., "Compressible Turbulent Skin Friction on Rough and Rough/Wavy Walls in Adiabatic Flow," NOL Technical Report NOLTR 74-34, Naval Ordnance Laboratory, February 1974.
11. Persh, J., "A Procedure for Calculating the Boundary Layer Development in the Region of Transition from Laminar to Turbulent Flow, NAVORD Report 4438, March 1957.
12. Dahm, T.J., "Interim Modeling of Boundary Layers for Shape Change Codes," Interoffice Memorandum, Aerotherm Division/Acurex Corporation, September 4, 1975.

13. Murphy, A.J., Chu, E., Kesselring, J.P., "AFRPL Graphite Performance Prediction Program, Volume I. Recommendation for a Standardized Analytic Procedure for MX Nozzle Throat Recession Calculations," Aerotherm Report 75-143, May 1975.
14. User's Manual, "Aerotherm Chemical Equilibrium Computer Program," Aerotherm Report UM-75-68, December 1975.
15. Tong, H., Suchsland, K.E., Murphy, A.K., Kwong, K.C., Lee, K., Chu, E., "Applicability of Reentry Technology to Rocket Nozzle Design, Volume II," Aerotherm Report TR-77-59.
16. Personal Communication between Henry Tong, Kai Kwong of Aerotherm and Philip Thomlinson, Joseph Koo of ARC.